

**Refrigeration**

An industrial scale refrigeration cycle runs on *tetrafluoroethane* (thermodynamic data on attached chart and table). Instead of a throttle valve, an *adiabatic expander/turbine* is used to produce some work, which can be used to compensate some of the *adiabatic compressor's* power requirement. The *evaporator* operates at  $-40^{\circ}\text{F}$ , while the *condenser's* outlet is at  $140^{\circ}\text{F}$ .

a)

Consider the case where the compressor and expander are *reversible*. For the equipment assigned to you,

i) Describe the inlet and outlet conditions.

ii) Calculate the heat and shaft-work that it produces (in terms of Btu/lbm).

Putting the pieces together with your team, calculate the coefficient of performance of the refrigeration cycle.

b)

Back to the real world where things are often not reversible...

When you look at the cost of such a cycle, you come across this entry in the Freez'it™ catalog that matches the equipment sizes you are considering:

	<i>Cost</i>
<b>Compressor</b>	
50% efficiency	\$50,000
80% efficiency	\$85,000
<b>Expander / Turbine</b>	
50% efficiency	\$30,000
80% efficiency	\$65,000

*buy any two of these, get one condenser and one evaporator free!  
free shipping and handling; free refrigerant, piping, and accessories*

You have \$120,000 to spend on this refrigeration cycle.

Your cycle has one condenser, one evaporator, one \_\_\_\_\_% efficient expander, and one \_\_\_\_\_% compressor.

Calculate the coefficient of performance of your cycle.

For your cycle configuration, calculate the flow rate of refrigerant required for a cooling rate of 500,000 Btu/hr.

**Tetrafluoroethane**

*Italics = estimated value (reading from graph)*

**All Reversible**

In						Out					
Phase	T (F)	P (psia)	S (Btu/lb R)	H (Btu/lbm)	Phase	T (F)	P (psia)	S (Btu/lb R)	H (Btu/lbm)	W (Btu/lbm)	Q (Btu/lbm)
Condenser	Vapor	170	243.880	0.231	127	Sat liq	140	243.880	0.117	59.764	-67.236
Expander	Sat liq	140	243.880	0.117	59.764	0.504	-40	7.429	0.117	48.892	-10.872
Evaporator	0.504	-40	7.429	0.117	48.892	Sat vap	-40	7.429	0.231	97.050	48.158
Compressor	Sat vap	-40	7.429	0.231	97.050	Vapor	170	243.880	0.231	127	29.950

  

	P (psia)	Hliq	Hvap	Sliq	Svap	
-40 F	7.429	0	97.05	0	0.23125	from table
140 F	243.88	59.764	119.72	0.1165	0.21648	

  

W net	19.1 Btu/lbm					
Q cold	48.2 Btu/lbm		Q hot	67.236 Btu/lbm		For 500,000 Btu/hr
COP	2.5					10383 lbm/hr of refrigerant

**80% Compressor, 50% Expander**

In						Out					
Phase	T (F)	P (psia)	S (Btu/lb R)	H (Btu/lbm)	Phase	T (F)	P (psia)	S (Btu/lb R)	H (Btu/lbm)	W (Btu/lbm)	Q (Btu/lbm)
Condenser	Vapor	190	243.880	0.240	134	Sat liq	140	243.880	0.117	59.764	-74.724
Expander	Sat liq	140	243.880	0.117	59.764	0.560	-40	7.429	0.129	54.328	-5.436
Evaporator	0.560	-40	7.429	0.129	54.328	Sat vap	-40	7.429	0.231	97.050	42.722
Compressor	Sat vap	-40	7.429	0.231	97.050	Vapor	190	243.880	0.240	134	37.438

  

W net	32.0 Btu/lbm					
Q cold	42.7 Btu/lbm		Q hot	74.7235 Btu/lbm		For 500,000 Btu/hr
COP	1.3					11704 lbm/hr of refrigerant

**50% Compressor, 80% Expander**

In						Out					
Phase	T (F)	P (psia)	S (Btu/lb R)	H (Btu/lbm)	Phase	T (F)	P (psia)	S (Btu/lb R)	H (Btu/lbm)	W (Btu/lbm)	Q (Btu/lbm)
Condenser	Vapor	275	243.880	0.275	157	Sat liq	140	243.880	0.117	59.764	-97.186
Expander	Sat liq	140	243.880	0.117	59.764	0.526	-40	7.429	0.122	51.067	-8.697
Evaporator	0.526	-40	7.429	0.122	51.067	Sat vap	-40	7.429	0.231	97.050	45.983
Compressor	Sat vap	-40	7.429	0.231	97.050	Vapor	275	243.880	0.275	157	59.900

  

W net	51.2 Btu/lbm					
Q cold	46.0 Btu/lbm		Q hot	97.186 Btu/lbm		For 500,000 Btu/hr
COP	0.9					10873 lbm/hr of refrigerant