

13.021 - Marine Hydrodynamics Lecture 9

Vorticity Equation

Return to viscous incompressible flow.

N-S equation: $\frac{\partial \vec{v}}{\partial t} + \vec{v} \cdot \nabla \vec{v} = -\nabla \left(\frac{p}{\rho} + gy \right) + \nu \nabla^2 \vec{v}$

$$\nabla \times () \longrightarrow \frac{\partial \vec{\omega}}{\partial t} + \nabla \times (\vec{v} \cdot \nabla \vec{v}) = \nu \nabla^2 \vec{\omega} \text{ since } \nabla \times \nabla \phi = 0 \text{ for any } \phi \text{ (conservative forces)}$$

Now:

$$\begin{aligned} (\vec{v} \cdot \nabla) \vec{v} &= \frac{1}{2} \nabla (\vec{v} \cdot \vec{v}) - \vec{v} \times (\nabla \times \vec{v}) \\ &= \nabla \left(\frac{v^2}{2} \right) - \vec{v} \times \vec{\omega} \text{ where } v^2 \equiv |\vec{v}|^2 = \vec{v} \cdot \vec{v} \\ \nabla \times (\vec{v} \cdot \nabla) \vec{v} &= \nabla \times \nabla \left(\frac{v^2}{2} \right) - \nabla \times (\vec{v} \times \vec{\omega}) = \nabla \times (\vec{\omega} \times \vec{v}) \\ &= (\vec{v} \cdot \nabla) \vec{\omega} - (\vec{\omega} \cdot \nabla) \vec{v} + \underbrace{\vec{\omega} (\nabla \cdot \vec{v})}_{= 0} + \underbrace{\vec{v} (\nabla \cdot \vec{\omega})}_{= 0 \text{ since}} \\ &\qquad\qquad\qquad \text{incompressible fluid} \qquad \nabla \cdot (\nabla \times \vec{v}) = 0 \end{aligned}$$

Therefore,

$$\frac{\partial \vec{\omega}}{\partial t} + (\vec{v} \cdot \nabla) \vec{\omega} = (\vec{\omega} \cdot \nabla) \vec{v} + \nu \nabla^2 \vec{\omega}$$

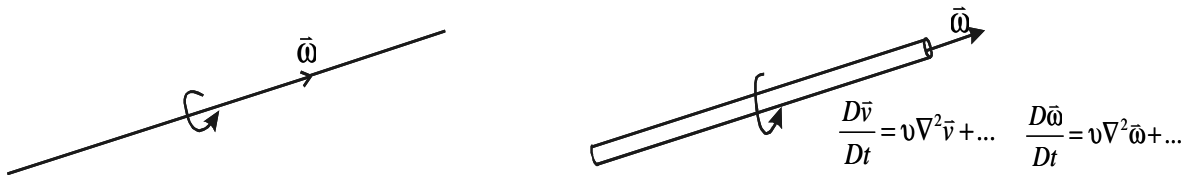
or

$$\frac{D\vec{\omega}}{Dt} = (\vec{\omega} \cdot \nabla) \vec{v} + \underbrace{\nu \nabla^2 \vec{\omega}}_{\text{diffusion}}$$

- Kelvin's Theorem revisited.

If $\nu \equiv 0$, then $\frac{D\vec{\omega}}{Dt} = (\vec{\omega} \cdot \nabla) \vec{v}$, so if $\vec{\omega} \equiv 0$ everywhere at one time, $\vec{\omega} \equiv 0$ always.

- ν can be thought of as diffusivity of (momentum) and vorticity, i.e., $\vec{\omega}$ once generated (on boundaries only) will spread/diffuse in space if ν is present.



- Diffusion of vorticity is analogous to the heat equation: $\frac{\partial T}{\partial t} = K \nabla^2 T$, where K is the heat diffusivity

Also since $\nu \sim 1$ or $2 \text{ mm}^2/\text{s}$, in 1 second, diffusion distance $\sim O(\sqrt{\nu t}) \sim O(\text{mm})$, whereas diffusion time $\sim O(L^2/\nu)$. So for a diffusion distance of $L = 1\text{cm}$, the necessary diffusion time needed is $O(10)\text{sec}$.

- For 2D, $\vec{v} = (u, v, 0)$ and $\frac{\partial}{\partial z} \equiv 0$. So, $\vec{\omega} = \nabla \times \vec{v}$ is \perp to \vec{v} (parallel to z-axis).

Then,

$$(\vec{\omega} \cdot \nabla) \vec{v} = \left(\underbrace{\omega_x}_0 \frac{\partial}{\partial x} + \underbrace{\omega_y}_0 \frac{\partial}{\partial y} + \omega_z \underbrace{\frac{\partial}{\partial z}}_0 \right) \vec{v} \equiv 0,$$

so in 2D we have

$$\frac{D\vec{\omega}}{Dt} = \nu \nabla^2 \vec{\omega}.$$

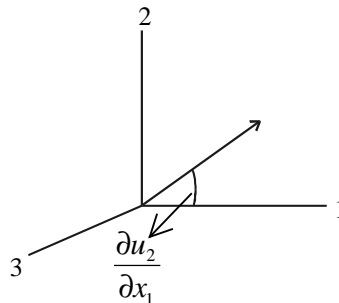
If $\nu = 0$, $\frac{D\vec{\omega}}{Dt} = 0$, i.e. in 2D, following a particle, the angular velocity is conserved. **Reason:** in 2D, the length of a vortex tube cannot change due to continuity.

- For 3D,

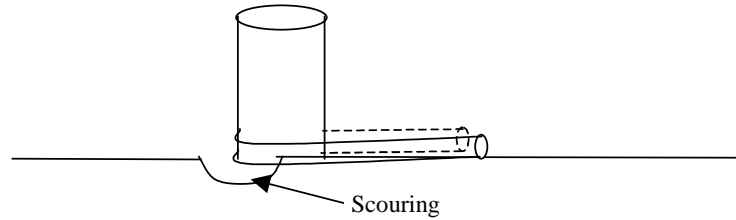
$$\frac{D\omega_i}{Dt} = \underbrace{\omega_j \frac{\partial v_i}{\partial x_j}}_{\text{vortex turning and stretching}} + \underbrace{\nu \frac{\partial^2 \omega_i}{\partial x_j \partial x_j}}_{\text{diffusion}}$$

e.g.

$$\frac{D\omega_2}{Dt} = \underbrace{\omega_1 \frac{\partial u_2}{\partial x_1}}_{\text{vortex turning}} + \underbrace{\omega_2 \frac{\partial u_2}{\partial x_2}}_{\text{vortex stretching}} + \underbrace{\omega_3 \frac{\partial u_2}{\partial x_3}}_{\text{vortex turning}} + \text{diffusion}$$



Example: Pile on a River



What really happens as length of the vortex tube L increases?

IFCF is no longer a valid assumption.

Why?

Ideal flow assumption implies that the inertia forces are much larger than the viscous effects (Reynolds number).

$$R_e \sim \frac{UL}{\nu}$$

Length increases \Rightarrow diameter becomes really small $\Rightarrow R_e$ is not that big after all.

Therefore IFCF is no longer valid.

3.3 Potential Flow - ideal (inviscid and incompressible) and irrotational flow

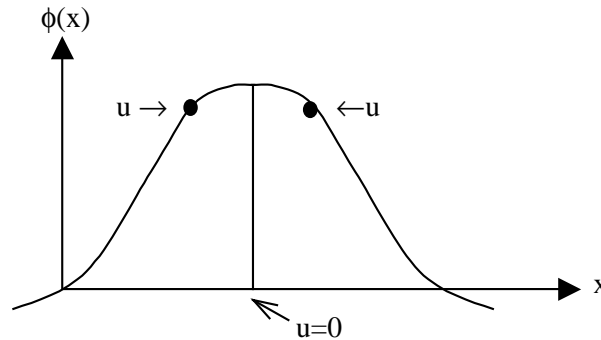
If $\vec{\omega} \equiv 0$ at some time t , then $\vec{\omega} \equiv 0$ always for ideal flow under conservative body forces by Kelvin's theorem.

Given a vector field \vec{v} for which $\vec{\omega} = \nabla \times \vec{v} \equiv 0$, then there exists a potential function (scalar) - the velocity potential - denoted as ϕ , for which

$$\vec{v} = \nabla\phi$$

Note that $\vec{\omega} = \nabla \times \vec{v} = \nabla \times \nabla\phi \equiv 0$ for any ϕ , so irrotational flow guaranteed automatically. At a point \vec{x} and time t , the velocity vector $\vec{v}(\vec{x}, t)$ in cartesian coordinates in terms of the potential function $\phi(\vec{x}, t)$ is given by

$$\vec{v}(\vec{x}, t) = \nabla\phi(\vec{x}, t) = \left(\frac{\partial\phi}{\partial x}, \frac{\partial\phi}{\partial y}, \frac{\partial\phi}{\partial z} \right)$$



The velocity vector \vec{v} is the gradient of the potential function ϕ , so it always points towards higher values of the potential function.

Governing Equations:

Continuity:

$$\nabla \cdot \vec{v} = 0 = \nabla \cdot \nabla \phi \Rightarrow \nabla^2 \phi = 0$$

Number of unknowns $\rightarrow \phi$

Number of equations $\rightarrow \nabla^2 \phi = 0$

Therefore the problem is closed. ϕ and p (pressure) are decoupled. ϕ can be solved independently first, and after it is obtained, the pressure p is evaluated.

$$p = f(\vec{v}) = f(\nabla \phi) \rightarrow \text{Solve for } \phi, \text{ then find pressure.}$$

3.4 Bernoulli equation for potential flow (steady or unsteady)

Euler eq:

$$\frac{\partial \vec{v}}{\partial t} + \nabla \left(\frac{v^2}{2} \right) - \vec{v} \times \vec{\omega} = -\nabla \left(\frac{p}{\rho} + gy \right)$$

Substitute $\vec{v} = \nabla \phi$ into the Euler's equation above, which gives:

$$\nabla \left(\frac{\partial \phi}{\partial t} \right) + \nabla \left(\frac{1}{2} |\nabla \phi|^2 \right) = -\nabla \left(\frac{p}{\rho} + gy \right)$$

or

$$\nabla \left\{ \frac{\partial \phi}{\partial t} + \frac{1}{2} |\nabla \phi|^2 + \frac{p}{\rho} + gy \right\} = 0,$$

which implies that

$$\frac{\partial \phi}{\partial t} + \frac{1}{2} |\nabla \phi|^2 + \frac{p}{\rho} + gy = f(t)$$

everywhere in the fluid for unsteady, potential flow. The equation above can be written as

$$p = -\rho \left[\frac{\partial \phi}{\partial t} + \frac{1}{2} |\nabla \phi|^2 + gy \right] + F(t)$$

which is the Bernoulli equation for unsteady or steady potential flow.

Summary: Bernoulli equation for ideal flow.

- Steady rotational or irrotational flow along streamline.

$$p = -\rho \left(\frac{1}{2} v^2 + gy \right) + C(\psi)$$

- Unsteady or steady irrotational flow everywhere in the fluid.

$$p = -\rho \left(\frac{\partial \phi}{\partial t} + \frac{1}{2} |\nabla \phi|^2 + gy \right) + F(t)$$

- For hydrostatics, $\vec{v} \equiv 0$, $\frac{\partial}{\partial t} = 0$.

$$p = -\rho gy + c \leftarrow \text{hydrostatic pressure (Archimedes' principle)}$$

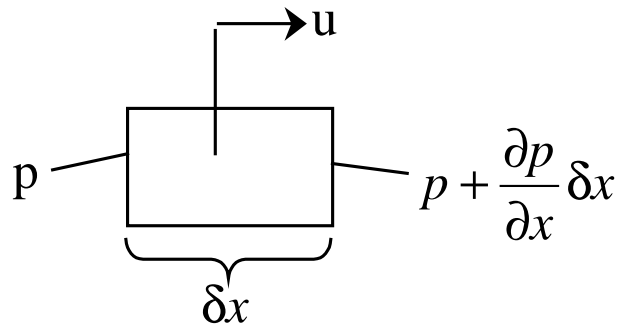
- Steady and no gravity effect ($\frac{\partial}{\partial t} = 0$, $g \equiv 0$)

$$p = -\frac{\rho v^2}{2} + c = -\frac{\rho}{2} |\nabla \phi|^2 + c \leftarrow \text{Venturi pressure (created by velocity)}$$

- Inertial, acceleration effect

$$p \sim -\rho \frac{\partial \phi}{\partial t} + \dots$$

$$\nabla p \sim -\rho \frac{\partial}{\partial t} \vec{v} + \dots$$



3.5 - Boundary Conditions

- KBC on an impervious boundary

$$\underbrace{\vec{v} \cdot \hat{n}}_{\hat{n} \cdot \nabla \phi} = \underbrace{\vec{u} \cdot \hat{n}}_{U_n \text{ given}} \quad \text{no flux across boundary} \Rightarrow \frac{\partial \phi}{\partial n} = U_n \text{ given}$$

- DBC: specify pressure at the boundary, i.e.,

$$-\rho \left(\frac{\partial \phi}{\partial t} + \frac{1}{2} |\nabla \phi|^2 + gy \right) = \text{given}$$

Note: On a free-surface $p = p_{atm}$.

3.6 - Stream function

- continuity: $\nabla \cdot \vec{v} = 0$; irrotationality: $\nabla \times \vec{v} = \vec{\omega} = 0$
- velocity potential: $\vec{v} = \nabla \phi$, then $\nabla \times \vec{v} = \nabla \times (\nabla \phi) \equiv 0$ for any ϕ , i.e. irrotationality is satisfied automatically. Required for continuity:

$$\nabla \cdot \vec{v} = \nabla^2 \phi = 0$$

- Stream function $\vec{\psi}$ defined by

$$\vec{v} = \nabla \times \vec{\psi}$$

Then $\nabla \cdot \vec{v} = \nabla \cdot (\nabla \times \vec{\psi}) \equiv 0$ for any $\vec{\psi}$, i.e. satisfies continuity automatically.

Required for irrotationality:

$$\nabla \times \vec{v} = 0 \Rightarrow \nabla \times (\nabla \times \vec{\psi}) = \underbrace{\nabla (\nabla \cdot \vec{\psi}) - \nabla^2 \vec{\psi}}_{\text{still 3 unknowns}} = 0 \quad (1)$$

$\vec{v} \longleftrightarrow \vec{\psi}$

- For 2D and axisymmetric flows, $\vec{\psi}$ is a scalar ψ (so stream functions are more useful for 2D and axisymmetric flows).

For 2D flow: $\vec{v} = (u, v, 0)$ and $\frac{\partial}{\partial z} \equiv 0$.

$$\vec{v} = \nabla \times \vec{\psi} = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ \psi_x & \psi_y & \psi_z \end{vmatrix} = \left(\frac{\partial}{\partial y} \psi_z \right) \hat{i} + \left(-\frac{\partial}{\partial x} \psi_z \right) \hat{j} + \left(\frac{\partial}{\partial x} \psi_y - \frac{\partial}{\partial y} \psi_x \right) \hat{k}$$

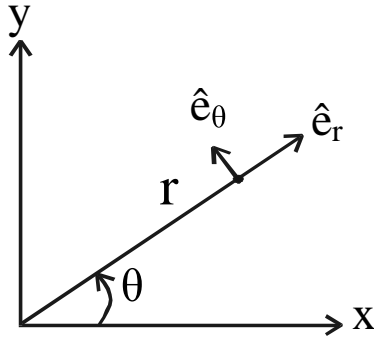
Set $\psi_x = \psi_y \equiv 0$ and $\psi_z = \psi$, then $u = \frac{\partial \psi}{\partial y}$; $v = -\frac{\partial \psi}{\partial x}$

So, for 2D:

$$\nabla \cdot \vec{\psi} = \frac{\partial}{\partial x} \psi_x + \frac{\partial}{\partial y} \psi_y + \frac{\partial}{\partial z} \psi_z \equiv 0$$

Then, from the irrotationality (see (1)) $\Rightarrow \nabla^2 \psi = 0$ and ψ satisfies Laplace's equation.

- 2D polar coordinates: $\vec{v} = (v_r, v_\theta)$ and $\frac{\partial}{\partial z} \equiv 0$.



$$\vec{v} = \nabla \times \vec{\psi} = \frac{1}{r} \begin{vmatrix} \hat{e}_r & r\hat{e}_\theta & \hat{e}_z \\ \frac{\partial}{\partial r} & \frac{\partial}{\partial \theta} & \frac{\partial}{\partial z} \\ \psi_r & \psi_\theta & \psi_z \end{vmatrix} = \overbrace{\frac{1}{r} \frac{\partial \psi_z}{\partial \theta}}^{v_r} \hat{e}_r - \overbrace{\frac{\partial \psi_z}{\partial r}}^{v_\theta} \hat{e}_\theta + \overbrace{\frac{1}{r} \left(\frac{\partial}{\partial r} r \psi_\theta - \frac{\partial}{\partial \theta} \psi_r \right)}^{v_z} \hat{e}_z$$

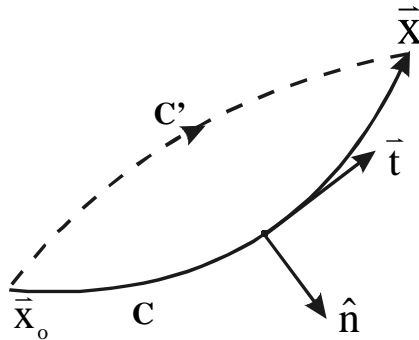
Again let $\psi_r = \psi_\theta \equiv 0$ and $\psi_z = \psi$, then $v_r = \frac{1}{r} \frac{\partial \psi}{\partial \theta}$ and $v_\theta = -\frac{\partial \psi}{\partial r}$.

- For 3D but axisymmetric flows, $\vec{\psi}$ also reduces to ψ (read JNN 4.6 for details).
- Physical Meaning of ψ .

In 2D: $u = \frac{\partial \psi}{\partial y}$ and $v = -\frac{\partial \psi}{\partial x}$.

We define

$$\psi(\vec{x}, t) = \psi(\vec{x}_0, t) + \underbrace{\int_{\vec{x}_0}^{\vec{x}} \vec{v} \cdot \hat{n} dl}_{\substack{\text{total volume flux} \\ \text{from left to right} \\ \text{across a curve C} \\ \text{between } \vec{x} \text{ and } \vec{x}_0}} = \psi(\vec{x}_0, t) + \int_{\vec{x}_0}^{\vec{x}} (u dy - v dx)$$

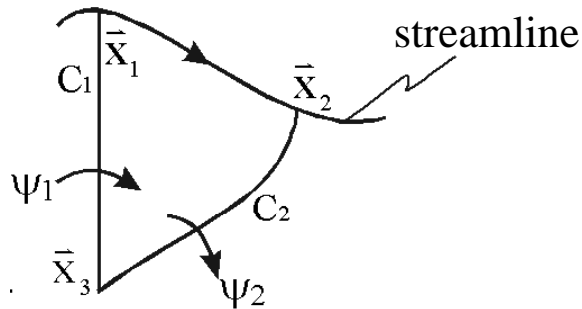


For ψ to be single-valued, \int must be path independent.

$$\int_C = \int_{C'} \text{ or } \int_C - \int_{C'} = 0 \longrightarrow \oint_{C-C'} \vec{v} \cdot \hat{n} dl = \iint_S \underbrace{\nabla \cdot \vec{v}}_{\text{continuity}} ds = 0$$

Therefore, ψ is unique because of continuity.

Let \vec{x}_1, \vec{x}_2 be two points on a given streamline ($\vec{v} \cdot \hat{n} = 0$ on streamline)

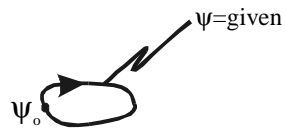
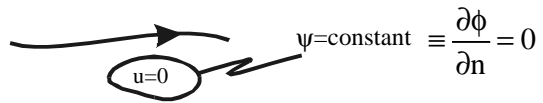


$$\underbrace{\psi(\vec{x}_2)}_{\psi_2} = \underbrace{\psi(\vec{x}_1)}_{\psi_1} + \int_{\vec{x}_1}^{\vec{x}_2} \underbrace{\vec{v} \cdot \hat{n}}_{=0} dl$$

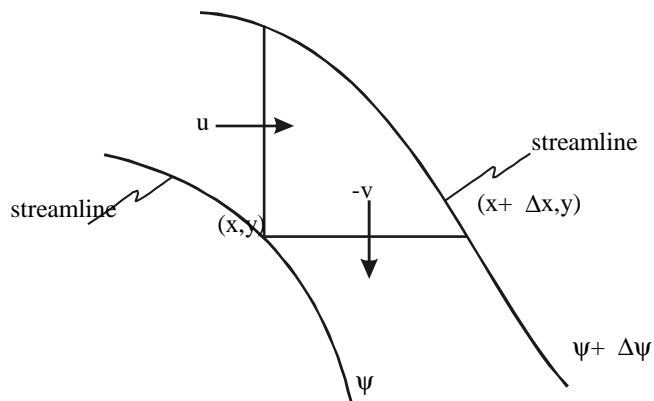
along
streamline

Therefore, $\psi_1 = \psi_2$, i.e., ψ is a constant along any streamline. For example, on an impervious stationary body $\vec{v} \cdot \hat{n} = 0$, so $\psi = \text{constant}$ on the body is the appropriate boundary condition. If the body is moving $\vec{v} \cdot \hat{n} = U_n$

$$\psi = \psi_0 + \int \underbrace{U_n}_{\text{given}} dl \quad \text{on the body}$$



Flux $\Delta\psi = -v\Delta x = u\Delta y$. Therefore, $u = \frac{\partial\psi}{\partial y}$ and $v = -\frac{\partial\psi}{\partial x}$



Summary: Potential formulation vs. Stream-function formulation for ideal flows

	potential	stream-function
definition	$\vec{v} = \nabla\phi$	$\vec{v} = \nabla \times \vec{\psi}$
continuity $\nabla \cdot \vec{v} = 0$	$\nabla^2\phi = 0$	automatically satisfied
irrotationality $\nabla \times \vec{v} = 0$	automatically satisfied	$\nabla \times (\nabla \times \vec{\psi}) = \nabla (\nabla \cdot \vec{\psi}) - \nabla^2\vec{\psi} = 0$
In 2D : $w = 0, \frac{\partial}{\partial z} = 0$		
	$\nabla^2\phi = 0$ for continuity	$\psi \equiv \psi_z : \nabla^2\vec{\psi} = 0$ for irrotationality
Cauchy-Riemann equations for $(\phi, \psi) = (\text{real, imaginary})$ part of an analytic complex function of $z = x + iy$		
Cartesian (x, y)	$u = \frac{\partial\phi}{\partial x}$ $v = \frac{\partial\phi}{\partial y}$	$u = \frac{\partial\psi}{\partial y}$ $v = -\frac{\partial\psi}{\partial x}$
Polar (r, θ)	$v_r = \frac{\partial\phi}{\partial r}$ $v_\theta = \frac{1}{r} \frac{\partial\phi}{\partial\theta}$	$v_r = \frac{1}{r} \frac{\partial\psi}{\partial\theta}$ $v_\theta = -\frac{\partial\psi}{\partial r}$

For irrotational flow	use	ϕ
For incompressible flow	use	ψ
For both flows	use	ϕ or ψ

Given ϕ or ψ for 2D flow, use Cauchy-Riemann equations to find the other:

e.g. $\phi = xy$ $\psi = ?$

$$\left. \begin{aligned} \frac{\partial\phi}{\partial x} = y = \frac{\partial\psi}{\partial y} &\longrightarrow \psi = \frac{1}{2}y^2 + f_1(x) \\ \frac{\partial\phi}{\partial y} = x = -\frac{\partial\psi}{\partial x} &\longrightarrow \psi = -\frac{1}{2}x^2 + f_2(y) \end{aligned} \right\} \psi = \frac{1}{2}(y^2 - x^2) + const$$