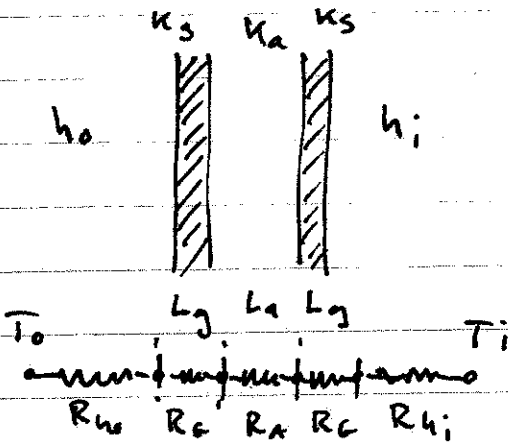
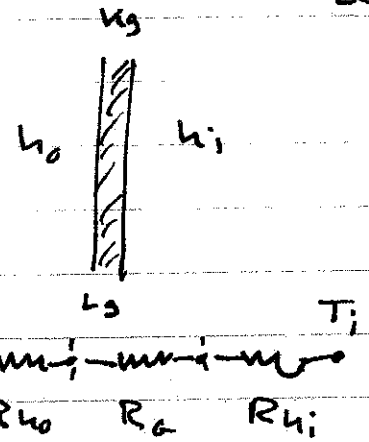


T18

16. unifid sp09
25



double glazed
vs. single
glazed window



$$h_o = 12 \text{ W/m}^2\text{-K}$$

$$h_i = 6 \text{ W/m}^2\text{-K}$$

$$k_g = 0.78 \text{ W/m-K}$$

$$k_a = 0.026 \text{ W/m-K}$$

(see tables)

$$\dot{Q}_D = \frac{\Delta T}{R_D}; \quad R_D = \frac{1}{h_o} + \frac{2L_g}{k_s} + \frac{1}{h_i} + \frac{L_a}{k_a} \text{ (per unit area)}$$

$$\dot{Q}_S = \frac{\Delta T}{R_S}; \quad R_S = \frac{1}{h_o} + \frac{L_g}{k_g} + \frac{1}{h_i} \quad \text{same } \Delta T = T_i - T_o$$

Reduction in heat transfer: $\frac{\dot{Q}_S - \dot{Q}_D}{\dot{Q}_S} = \frac{\frac{1}{R_S} - \frac{1}{R_D}}{\frac{1}{R_S}} = \Delta$

$$\Delta = 1 - \frac{\frac{1}{h_o} + L_g/k_g + 1/h_i}{\frac{1}{h_o} + 2L_g/k_s + L_a/k_a + 1/h_i}$$

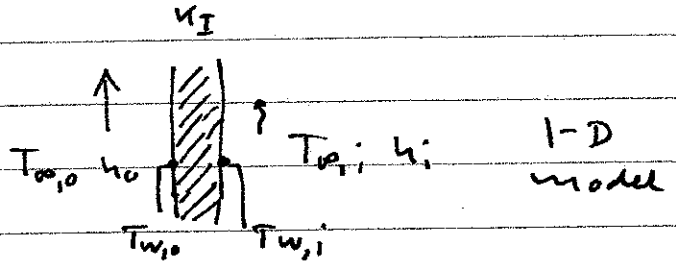
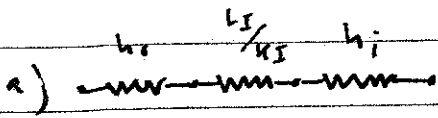
$$L_a = 0.005 \text{ m}$$

$$L_g = 0.004 \text{ m}$$

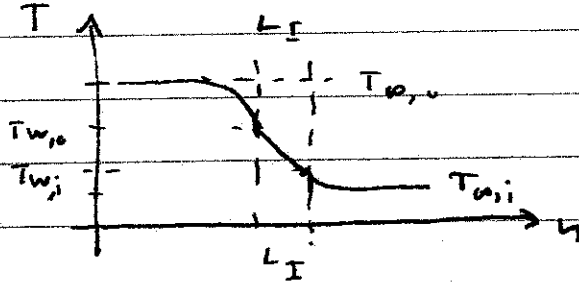
find $\Delta = 0.564$

So heat transfer is reduced by 56.4% due to significantly higher resistance of air film

Cooled turbine blade no TBC



$T_{\infty,0}$ $T_{w,0}$ $T_{w,i}$ $T_{\infty,i}$



b) Fourier: $q = -k \frac{dT}{dx}$

Newton: $q_c = h(T_a - T_w)$

c) highest temp in blade: $T_{w,0}$, $\dot{Q} = \frac{T_{\infty,0} - T_{\infty,i}}{R_{tot}}$, 1st law: $\dot{Q} = \text{const}$

$$R_{tot} = \frac{1}{h_0} + \frac{L_I}{k_I} + \frac{1}{h_i} = 0.0033 \text{ K/W} \cdot \text{m}^2$$

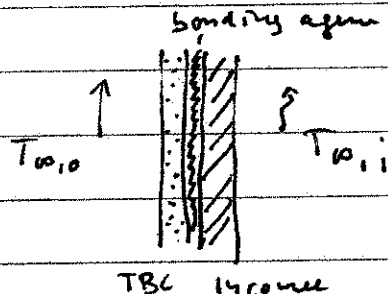
$$\dot{Q} = \frac{T_{\infty,0} - T_{w,0}}{R_0}$$

$$T_{w,0} = T_{\infty,0} - \frac{T_{\infty,0} - T_{\infty,i}}{R_{tot}} \cdot \frac{1}{h_0}, \text{ find } T_{w,0} = 1306 \text{ K} > 1250 \text{ K!}$$

blade will melt!

d)

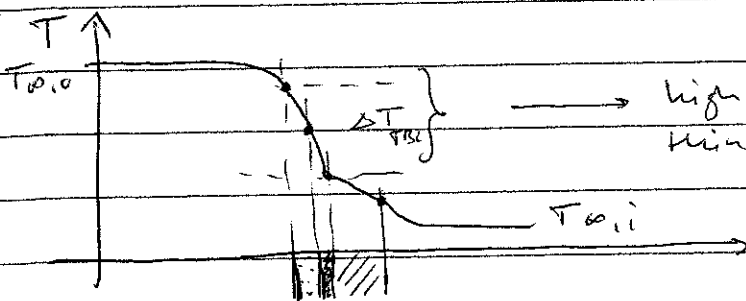
$$\frac{1}{h_0} + \frac{L_{TBC}}{k_{TBC}} + \frac{L_B}{k_B} + \frac{L_I}{k_I} + \frac{1}{h_i} = R_{tot}^{TBC}$$



$$T_{w,0}^{TBC} = T_{\infty,0} - \frac{T_{\infty,0} - T_{\infty,i}}{R_{tot}^{TBC}} \left(\frac{1}{h_0} + \frac{L_{TBC}}{k_{TBC}} + \frac{L_B}{k_B} \right)$$

$$\Rightarrow R_{tot} = 0.00373 \frac{\text{K}}{\text{W}}$$

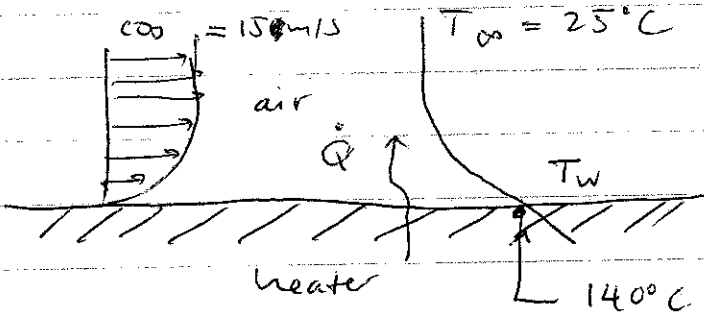
$$T_{w,0}^{TBC} = 1,183 \text{ K} < 1250 \text{ K} \text{ blade is protected and will not melt}$$



high resistance in TBC and thin bonding agent yields significant temperature drop

T20

16. Unified Sp 09 25



$$D = 0.25 \text{ m}$$

$$A = 0.25 \text{ m}^2$$

concept: Reynolds analogy, convective heat x-fc

Re-analogy: $St = \frac{cf}{2}$, $D = \frac{1}{2} cf A g_{\infty} C_{\infty}^2$

$$St = \frac{h}{g_{\infty} C_p} \quad \text{so} \quad \frac{h}{g_{\infty} C_p} = \frac{D}{A g_{\infty} C_{\infty}^2}, \quad h = \frac{D C_p}{A C_{\infty}}$$

find $h = 66.9 \text{ W/m}^2\text{K}$

Newton's law of cooling: $\dot{Q} = Ah(T_w - T_{\infty}) = \dot{Q}_{el}$

find $\dot{Q}_{el} = 2,093 \text{ W}$ of electrical power required to maintain surface temperature