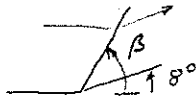


UE Fluids Problem 17+18 Solution

S 07

a) Usual oblique-shock case, $\theta = 8^\circ$, $M_1 = 1.5 \rightarrow \beta = 52.5^\circ$ from chart



$M_{n1} = M_1 \sin \beta = 1.19$, plug into normal-shock functions: $\frac{P_2}{P_1} = 1.486$, $M_{n2} = 0.8486$

$$\boxed{\frac{P_a}{P_\infty} = \frac{P_2}{P_1} = 1.486}, \quad \boxed{M_a = \frac{M_{n2}}{\sin(\beta - \theta)} = 1.211}, \quad \boxed{\frac{P_{0a}}{P_\infty} = \frac{P_a}{P_\infty} \left[1 + \frac{\gamma-1}{2} M_a^2\right]^{-\frac{\gamma}{\gamma-1}} = 3.656}$$

b) Usual expansion fan case, $\theta = 16^\circ$, $M_1 = M_a = 1.211$



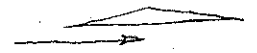
$\nu(M_1) = 3.83^\circ$, $\nu(M_2) = \nu(M_1) + \theta = 19.83^\circ \rightarrow M_2 = M_b = 1.769$ from P-M table

Since fan is isentropic, $P_{0b} = P_{0a} = 3.656 P_\infty$, and $P_b = P_{0b} \left[1 + \frac{\gamma-1}{2} M_b^2\right]^{-\frac{\gamma}{\gamma-1}}$

$$\boxed{\frac{P_b}{P_\infty} = \frac{P_{0b}}{P_\infty} \left[1 + \frac{\gamma-1}{2} M_b^2\right]^{-\frac{\gamma}{\gamma-1}} = 0.667}$$

c) There is no shock on bottom ($\theta = 0^\circ$), so

$$\boxed{\frac{P_c}{P_\infty} = 1}$$



$$d) L' = \int_0^c (P_{lower} - P_{upper}) dx = \int_0^{c/2} (P_c - P_a) dx + \int_{c/2}^c (P_c - P_b) dx = P_\infty \frac{c}{2} \left[\frac{P_c}{P_\infty} - \frac{P_a}{P_\infty} + \frac{P_c}{P_\infty} - \frac{P_b}{P_\infty} \right]$$

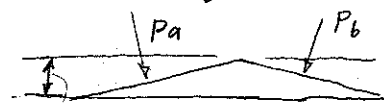
$$\boxed{L' = P_\infty \frac{c}{2} [1 - 1.486 + 1 - 0.667] = -P_\infty c \cdot 0.0765}$$



$$D' = \int_0^c \left(P \frac{dy}{dx} \right)_{upper} - \left(P \frac{dy}{dx} \right)_{lower} dx, \quad \frac{dy}{dx} \Big|_{lower} = 0, \quad \frac{dy}{dx} \Big|_a = \tan 8^\circ = 0.1405, \quad \frac{dy}{dx} \Big|_b = -0.1405$$

$$D' = P_a \cdot \tan(8^\circ) \frac{c}{2} - P_b \tan(8^\circ) \frac{c}{2} - P_c \cdot 0$$

$$\boxed{D' = (P_a - P_b) \tan 8^\circ \cdot \frac{c}{2} = P_\infty c \cdot 0.0576}$$

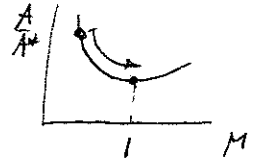


$\frac{e}{2} \cdot \frac{dy}{dx} =$ projected area on which $P_a - P_b$ act

$$\boxed{C_e = \frac{L'}{\frac{1}{2} \rho_\infty V_\infty^2 c} = \frac{L'}{\frac{\gamma}{2} \rho_\infty M_\infty^2 c} = \frac{-0.0765 P_\infty c}{\frac{\gamma}{2} M_\infty^2 P_\infty c} = -0.0485}$$

$$\boxed{C_d = \frac{D'}{\frac{1}{2} \rho_\infty V_\infty^2 c} = \frac{D'}{\frac{\gamma}{2} \rho_\infty M_\infty^2 c} = \frac{0.0576 P_\infty c}{\frac{\gamma}{2} M_\infty^2 P_\infty c} = 0.0365}$$

a) The sonic ($M=1$) condition can only occur at a throat, or area minimum. This can be seen from the A/A^* versus M plot. Since the flow starts at $M \ll 1$ in the bottle, and A monotonically decreases, then M must monotonically increase up to $M=1$ at the nozzle.



b) Stagnation conditions in the bottle, which is in effect a reservoir:



$$P_0 = 4 \times 10^5 \text{ Pa (given)}, T_0 = 300 \text{ K (given)}, \rho_0 = \frac{P_0}{RT_0} = 4.65 \text{ kg/m}^3$$

At the throat, where $M=1$, we have

$$P = P^* = P_0 \left[1 + \frac{\gamma-1}{2} \right]^{-\frac{\gamma}{\gamma-1}} = 2.11 \times 10^5 \text{ Pa}$$

$$T = T^* = T_0 \left[1 + \frac{\gamma-1}{2} \right]^{-1} = 250 \text{ K}$$

$$\rho = \rho^* = \rho_0 \left[1 + \frac{\gamma-1}{2} \right]^{-\frac{1}{\gamma-1}} = 2.95 \text{ kg/m}^3$$

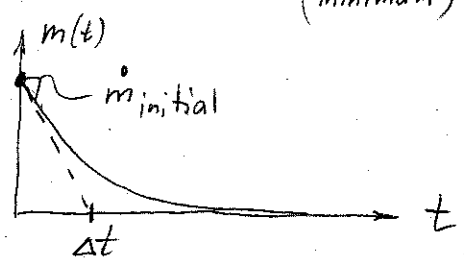
$$u = a^* = \sqrt{\gamma RT^*} = 316.9 \text{ m/s}$$

c) Initial $\dot{m} = \rho u A = 2.95 \text{ kg/m}^3 \cdot 316.9 \text{ m/s} \cdot 0.0004 \text{ m}^2 = 0.374 \text{ kg/s}$

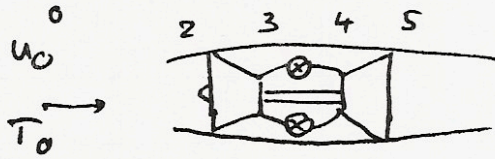
Initial mass in bottle: $m = \rho_0 V = 3.318 \text{ kg/m}^3 \cdot 2 \text{ l} \frac{1}{1000 \text{ l/m}^3} = 0.0093 \text{ kg}$

If the initial \dot{m} is sustained, the mass will flow out in $\Delta t \approx \frac{m}{\dot{m}} \approx 0.025 \text{ s}$ (minimum)

In reality, \dot{m} will decrease as the bottle empties so the actual time will be longer.

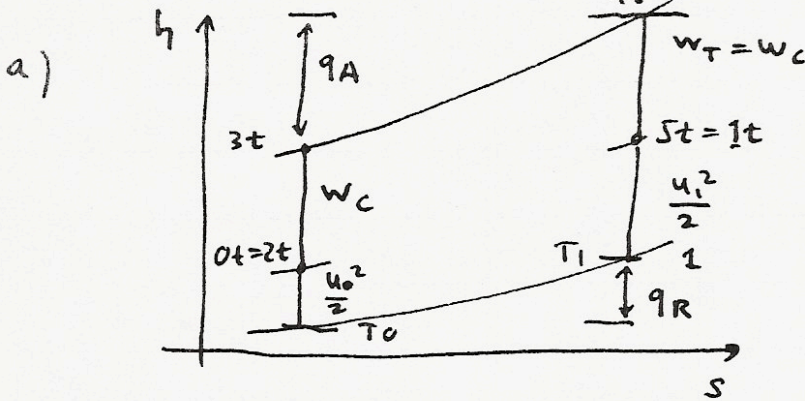


Problem T12



spring out, out

assume ideal cycle



shaft power balance

$$w_C = w_T$$

$$w_{net} = w_{mech} = \frac{1}{2}(u_1^2 - u_0^2)$$

q_A : heat absorbed

q_R : heat rejected

b) ideal cycle, heat rejection at $p = \text{const}$: $T ds = dh - \frac{1}{s} dp = dq$

$$\underline{q_R = c_p(T_1 - T_0)}$$

net heat input: $q_A - q_R = \frac{1}{2}(u_1^2 - u_0^2)$

c) 1st law: $w_{net} = q_A - q_R$, $q_A = q_R + w_{mech} \rightarrow \underline{q_A = c_p(T_1 - T_0) + \frac{1}{2}(u_1^2 - u_0^2)}$

d)

$$\eta_{th} = \frac{w_{net}}{q_A} = \frac{\frac{1}{2}(u_1^2 - u_0^2)}{\frac{1}{2}(u_1^2 - u_0^2) + c_p(T_1 - T_0)} = \frac{1}{1 + \frac{T_1 - T_0}{\frac{u_1^2 - u_0^2}{2c_p}}}$$

e) $\eta_{overall} = \eta_{th} - \eta_{prop}$

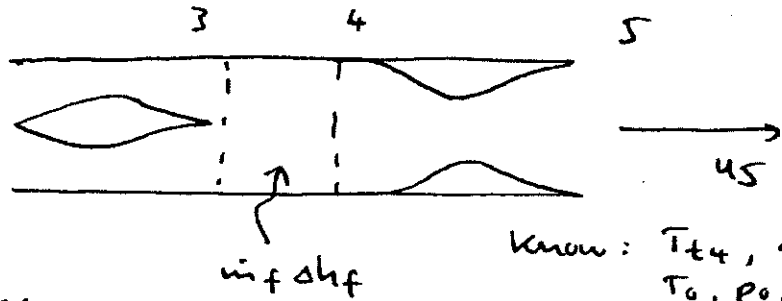
$$\eta_{overall} = \frac{\dot{W}_{u0}}{\dot{m} \dot{s} h} = \frac{\dot{W}_{u0}}{\dot{m} q_A} = \frac{(u_1 - u_0) u_0}{q_A}$$

$$\eta_{overall} = \frac{u_0}{\frac{1}{2}(u_1 + u_0) + c_p \frac{T_1 - T_0}{u_1 - u_0}} = \frac{2}{1 + \frac{u_1}{u_0} + \frac{2c_p}{u_0} \frac{T_1 - T_0}{u_1 - u_0}}$$

Problem T13

$$P_0 \quad \longrightarrow$$

$$T_0 \quad u_0$$



Known: T_{t4} , Δh_f
 T_0 , P_0 , u_0
 $P_5 = P_0$
 $P = \dot{F} u_0$

Assume: no losses, no shocks

a) $T_{t0} = T_{t3}$, $T_{t0} = T_0 + \frac{u_0^2}{2c_p}$ (st. law)

isentropic compression $P_{t0} = P \left(1 + \frac{\gamma-1}{2} M_0^2\right)^{\frac{\gamma}{\gamma-1}} = P_{t3}$

$M_0 = \frac{u_0}{\sqrt{\gamma R T_0}}$, $M_0 = 3.06$, $T_{t3} = 638 \text{ K}$, $P_t = 8.04 \text{ bar}$

b) $M_0 = M_5$ (same PR \rightarrow same TR, hence same M)

$T_5 = T_{t4} \left(1 + \frac{\gamma-1}{2} M_5^2\right)^{-1}$ $u_5 = M_5 \sqrt{\gamma R T_5}$ $u_5 = 1736.7 \text{ m/s}$

c) $F = \dot{m} (u_5 - u_0)$, $P = \dot{F} u_0$ so $\dot{F} = 8.2 \text{ kN}$

$\dot{m} = \frac{P}{u_0 (u_5 - u_0)}$ $\dot{m} = 9.97 \text{ kg/s}$

d) $w_{\text{net}} = w_{\text{mech}} = \frac{1}{2} (u_5^2 - u_0^2)$ $w_{\text{net}} = 1.09 \text{ MJ/kg}$

e) $\dot{Q}_A = \dot{m} c_p (T_{t4} - T_{t3}) = \dot{m} f \Delta h_f$ $f = \frac{c_p (T_{t4} - T_{t3})}{\Delta h_f}$

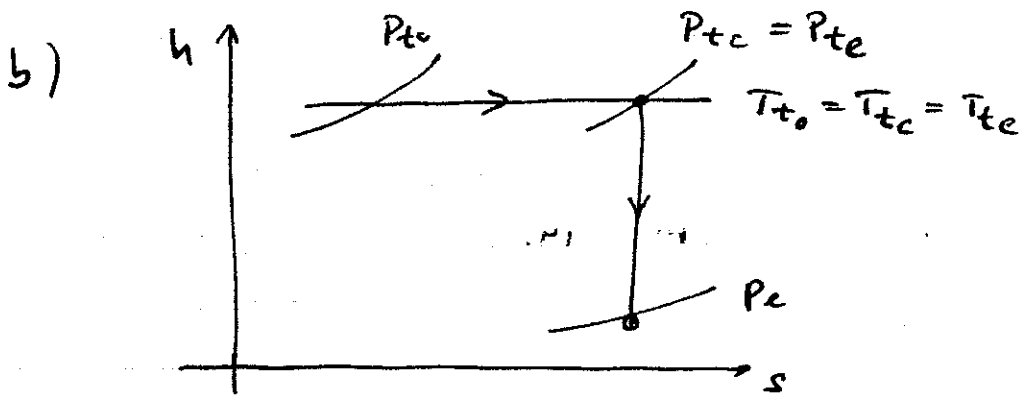
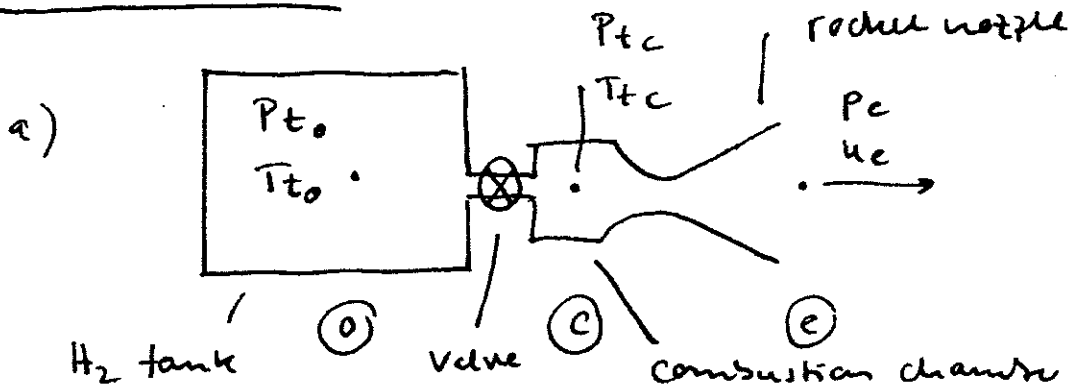
$f = 0.0388$ $\dot{m} f = f \cdot \dot{m} \rightarrow \dot{m} f = 0.387 \text{ kg/s}$

f) $\eta_{\text{prop}} = \frac{2}{1 + \frac{u_5}{u_0}} \rightarrow \eta_{\text{prop}} = 0.69$

g) $\eta_{\text{overall}} = \eta_{\text{th}} \times \eta_{\text{prop}}$ $\eta_{\text{th}} = \frac{w_{\text{net}}}{f \Delta h_f} = 0.65$

$\eta_{\text{overall}} = 0.45$

Problem T14



$H_2: c_p = \frac{7}{2} \frac{R}{M} = 14.5 \frac{kJ}{kg \cdot K}$
 $R = \frac{R}{M} = 4155 J/kg \cdot K$

c) $I_{sp} = \frac{F}{\dot{m}_f g} = \frac{\dot{m}_e u_e}{\dot{m}_f g} = \frac{u_e}{g}$

1st law: $h_t = const \rightarrow T_{t0} = T_{t_c} = T_e + \frac{u_e^2}{2c_p}$

$u_e = \sqrt{2c_p(T_{t0} - T_e)}$ $T_e = T_{t0} \left(\frac{P_e}{P_{t0}} \right)^{\frac{\gamma-1}{\gamma}}$

$I_{sp} = \frac{u_e}{g} \wedge u_e = \sqrt{2c_p T_{t0} \left(1 - \left(\frac{P_e}{P_{t0}} \right)^{\frac{\gamma-1}{\gamma}} \right)} = 2237 \text{ m/s} \quad \underline{I_{sp} = 228 \text{ s}}$

d) $\dot{m}_f = \frac{F}{I_{sp} g}$ $\dot{m}_f = \dot{m}_i \rightarrow \underline{\dot{m}_i = 0.089 \text{ kg/s}}$

e) thrusting requirement: $F_{at} = \dot{m}_e u_e \Delta t = \rho_0 V_0 u_e \Delta t$

$\underline{V_0 = \frac{F_{at}}{\rho_0 u_e} = \frac{F_{at} R T_{t0}}{P_{t0} u_e} = 0.139 \text{ m}^3}$

(equivalent to sphere of 0.32m radius)