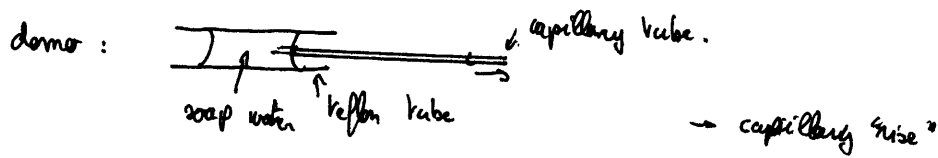


⑤ Interfacial hydrodynamics



Navier & Stokes eq:

$$\rho \frac{\partial \vec{v}}{\partial t} + \rho (\vec{v} \cdot \nabla) \vec{v} = \rho \vec{f} - \nabla p + \mu \nabla^2 \vec{v}$$

$\downarrow$  body force       $\downarrow$  pressure       $\downarrow$

orders of magnitude       $\rho \frac{V^2}{L}$        $\mu \frac{V}{L^2}$

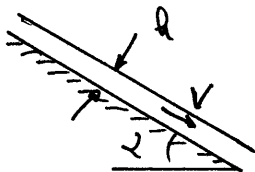
$$Re = \frac{\text{inertia}}{\text{viscous}} = \frac{\rho V L}{\mu}$$

$$Re = \frac{\rho V L}{\mu}$$

$Re \gg 1 \rightarrow$  inertia (Bernoulli ...)

$Re \ll 1 \rightarrow$  viscous (Stokes flow)

examples scaling laws:  $\rightarrow$  N-S difficult to solve  $\rightarrow$  scalings.



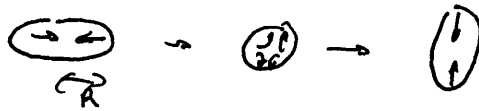
$\rightarrow$  if viscous flow. ( $\frac{\rho V h}{\mu} \ll 1$ )

$$\mu \frac{V}{h^2} \sim \rho g \sin \alpha$$

$$\Rightarrow \boxed{V \sim \frac{\rho g h^2}{\mu} \sin \alpha} \rightarrow \text{Darcy law.}$$

Oscillations of a droplet:

→ slide: many modes.



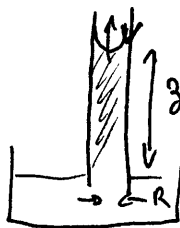
driving: surface tension / inertia / surface tension ...

$$\rho V^2 \sim \frac{\sigma}{R}$$

$$V \sim \frac{R}{\tau_{osc}} \Rightarrow \rho \frac{R^2}{\tau_{osc}^2} \sim \frac{\sigma}{R} \rightarrow \boxed{\tau_{osc} \sim \left(\frac{\rho R^3}{\sigma}\right)^{1/2}}$$

## 5.1 Spontaneous wetting

### 5.1.1 Capillary rise



$$\mu \frac{V}{R^2} \sim \frac{2\sigma \cos \theta}{Rg} - \rho g.$$

$$\mu \frac{V}{R^2} \sim \frac{\sigma \cos \theta}{Rg} \left(1 - \frac{z}{h_{eq}}\right).$$

if  $z \ll h_{eq}$  ( $h_{eq} \rightarrow \infty$ : ~~long~~ horizontal tube).

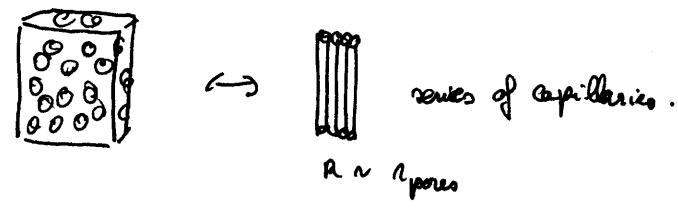
$$V \sim \frac{R \sigma \cos \theta}{\mu g} \rightarrow g \frac{dz}{dt} \sim R \frac{\sigma}{\mu} \cos \theta.$$

$$\boxed{z \sim \left(R \frac{\sigma \cos \theta}{\mu} t\right)^{1/2}} \quad \text{Washburn law.}$$

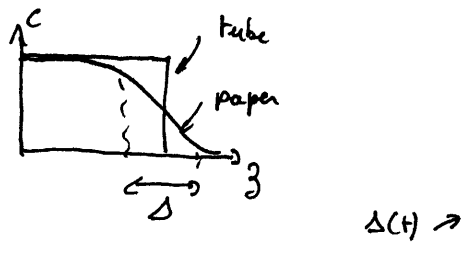
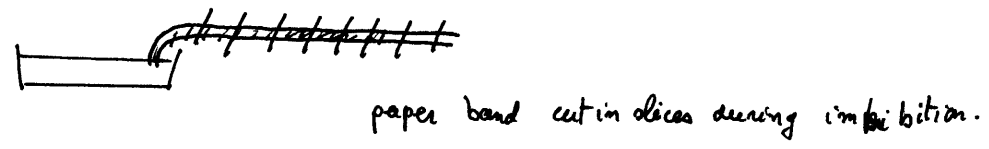
$V^* = \frac{\sigma}{\mu}$  characteristic capillary speed.

→ may have some inertia at the beginning.

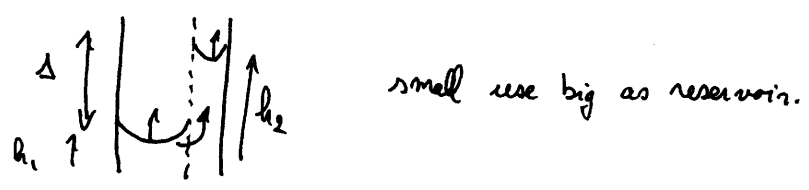
→ imbibition of a porous media:



↳ delamination of the front.



↳ effect of the pores polydispersity:



Capillary rise in trees?

→ slide: sequoia.

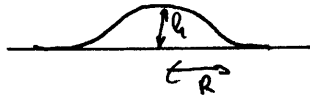
$$R \sim 10 \mu \quad \mu \sim 10^{-3} \text{ Pa}\cdot\text{s} \quad h \sim 30 \text{ m} \quad \sigma \sim 70 \text{ mN/m}$$

$$z \sim \frac{h^2 \mu}{R \sigma} \sim \text{many months!}$$

best situation  
 of neglected

→ surface tension just holds the sap

driving force: evaporation.

5.1.1 Spreading

$$\text{Laplace pressure: } \frac{1}{r} = \frac{\ddot{\theta}}{(1+\dot{\theta}^2)^{3/2}}$$

$\sim$  scaling for smooth surface

$$\frac{1}{r} \sim \frac{h}{R^2}$$

$$\Rightarrow \Delta p_c \sim \frac{\sigma h}{R^2} \quad \nabla p \sim \frac{\sigma h}{R^3}$$

capillary driven spreading:

$$\mu \frac{V}{R^2} \sim \frac{\sigma h}{R^3}$$

$$\Rightarrow V \sim \frac{\sigma}{\mu} \left(\frac{h}{R}\right)^3$$

$$\Omega \sim R^2 h \Rightarrow h \sim \frac{\Omega}{R^2}$$

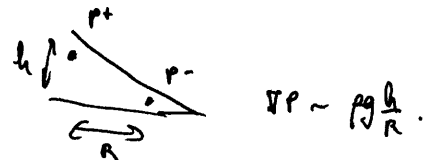
$$\frac{dR}{dt} \sim \frac{\sigma}{\mu} \left(\frac{\Omega}{R^3}\right)^3 \rightarrow R^9 \frac{dR}{dt} \sim \frac{\sigma}{\mu} \Omega^3$$

$$R^{10} \sim \Omega^3 V^* t \quad \boxed{R \sim (\Omega^3 V^* t)^{1/10}}$$

$\hookrightarrow$  delicate point: integration  $\#$  in the edge  $\Rightarrow$  An term and cut-off.

$\rightarrow$  slide: A.N. Cazabat.  $\rightarrow$  2<sup>nd</sup> regime  $\#$   $1/8$ .

gravity driven:  
(if time enough)  $\mu \frac{V}{R^2} \sim \rho g \frac{h}{R}$



$$V \sim \frac{\rho g}{\mu} \frac{h^3}{R}$$

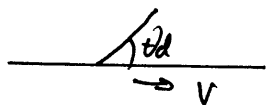
$$V \sim \frac{\rho g}{\mu} \frac{\Omega^3}{R^2}$$

$$R^2 \frac{dR}{dt} \sim \frac{\rho g}{\mu} \Omega^3 \rightarrow R \sim \left(\frac{\rho g}{\mu} \Omega^3 t\right)^{1/8}$$

cross over:  $\rho g \frac{h}{R} \sim \frac{\sigma h}{R^3} \rightarrow R \sim \ell_c$

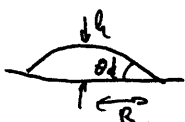
5.2 Forced wetting:

5.2.1 Dynamic contact angle:



capillarity wants  $\theta \rightarrow 0$   
viscosity - liquid follows the plate.

→ analogue spreading



$h/R \sim \theta_d \Rightarrow V \sim \frac{\sigma}{\mu} \theta_d^3$

$\theta_d \sim \left(\frac{\mu V}{\sigma}\right)^{1/3}$

Tanner's law.

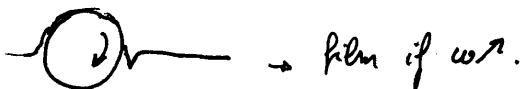
$Ca = \frac{\mu V}{\sigma}$

capillary number

→ slide.  $\theta_d$  from Hoffman.

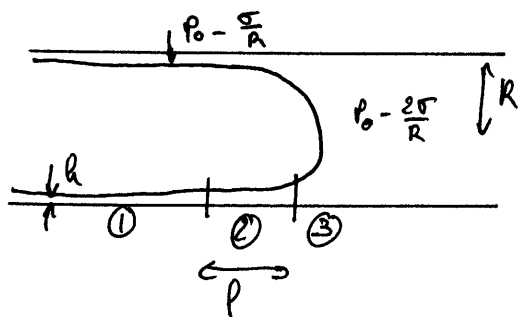
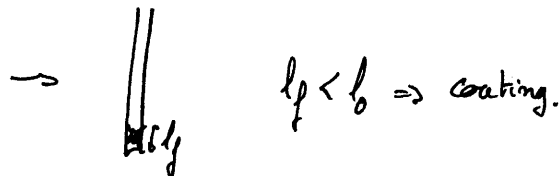
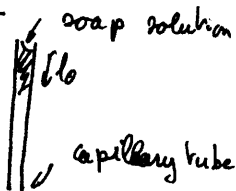
as application → limit to coating process:  $Ca$  too big  $\Rightarrow \theta_d \sim 180^\circ \Rightarrow$  air entrapment.

slide: cusp near a rotating cylinder ~~curvature~~



5.2.2 Coating

demo:



{ viscosity  $\Rightarrow$  film thick.  
surface tension  $\Rightarrow$  sucks the film.

- ① static film
- ② dynamic meniscus
- ③ static meniscus

→ dynamic meniscus:  $\frac{\mu V}{h^2} \sim \frac{\sigma}{Rl}$

connection static & dynamic: same ~~eff~~ curvatures:

$$\frac{l}{R} \sim \frac{h}{\rho l} \left( \frac{\ddot{z}}{(1+\dot{z}^2)^{3/2}} \right)$$

$$\Rightarrow \underline{l \sim (Rh)^{1/2}}$$

$$\frac{\mu V}{h^2} \sim \frac{\sigma}{R(Rh)^{1/2}}$$

$$\Rightarrow \boxed{h \sim R \left( \frac{\mu V}{\sigma} \right)^{2/3}}$$

{ Landau-Levich  
Bridgman

is works for  $Ca \ll 1$  ( $h \ll R$  for a tube).

same for a plate  $l \leftrightarrow R$ :



$$\boxed{h \sim l Ca^{2/3}}$$

effect of gravity?

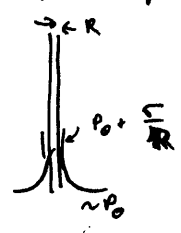
$$\rho g \sim \frac{\sigma}{l^2} \rightarrow l \sim l_c. (\Rightarrow Ca \sim 1)$$



→  $Ca \gg 1$

$$h \sim \left( \frac{\mu V}{\rho g} \right)^{1/2} \rightarrow \underline{h \sim l_c Ca^{1/2}}$$

same for a fiber:



$$\rightarrow \underline{h \sim R Ca^{2/3}}$$