# CO<sub>2</sub> Hydrate: Synthesis, Composition, Structure, Dissociation Behavior, and a Comparison to Structure I CH<sub>4</sub> Hydrate

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Structure I (sI) carbon dioxide (CO<sub>2</sub>) hydrate exhibits markedly different dissociation behavior from sI methane (CH<sub>4</sub>) hydrate in experiments in which equilibrated samples at 0.1 MPa are heated isobarically at 13 K/h from 210 K through the H<sub>2</sub>O melting point (273.15 K). The CO<sub>2</sub> hydrate samples release only about 3% of their gas content up to temperatures of 240 K, which is 22 K above the hydrate phase boundary. Up to 20% is released by 270 K, and the remaining  $CO_2$  is released at 271.0  $\pm$  0.5 K, where the sample temperature is buffered until hydrate dissociation ceases. This reproducible buffering temperature for the dissociation reaction  $CO_2 \cdot nH_2O = CO_2(g) + nH_2O(l \text{ to s})$  is measurably distinct from the pure  $H_2O$  melting point at 273.15 K, which is reached as gas evolution ceases. In contrast, when sI CH<sub>4</sub> hydrate is heated at the same rate at 0.1 MPa, >95% of the gas is released within 25 K of the equilibrium temperature (193 K at 0.1 MPa). In conjunction with the dissociation study, a method for efficient and reproducible synthesis of pure polycrystalline CO<sub>2</sub> hydrate with suitable characteristics for material properties testing was developed, and the material was characterized. CO<sub>2</sub> hydrate was synthesized from CO<sub>2</sub> liquid and H<sub>2</sub>O solid and liquid reactants at pressures between 5 and 25 MPa and temperatures between 250 and 281 K. Scanning electron microscopy (SEM) examination indicates that the samples consist of dense crystalline hydrate and 50-300 µm diameter pores that are lined with euhedral cubic hydrate crystals. Deuterated hydrate samples made by this same procedure were analyzed by neutron diffraction at temperatures between 4 and 215 K; results confirm that complete conversion of water to hydrate has occurred and that the measured unit cell parameter and thermal expansion are consistent with previously reported values. On the basis of measured weight gain after synthesis and gas yields from the dissociation experiments, approximately all cages in the hydrate structure are filled such that  $n \approx 5.75$ .

### Introduction

Carbon dioxide hydrate,  $CO_2 \cdot nH_2O$  ( $n \ge 5.75$ ), belongs to a family of nonstoichiometric compounds in which hydrogenbonded water molecules are arranged in an icelike framework, forming polyhedral cavities occupied by "guest" molecules with an appropriate size range. CO2 hydrate crystallizes in one of the two cubic hydrate structures (structure I), in which the unit cell consists of 46 H<sub>2</sub>O (or D<sub>2</sub>O) molecules and up to 8 CO<sub>2</sub> molecules occupying both small (pentagonal dodecahedral) and large (tetrakaidecahedral) cavities in a ratio of 1:3. CO<sub>2</sub> hydrate is stable over a range of elevated pressure and low-temperature conditions (see Sloan<sup>1</sup> for a summary of the published phase equilibria data). The formation of CO<sub>2</sub> hydrate from H<sub>2</sub>O ice has been observed optically,<sup>2,3</sup> and synthetic CO<sub>2</sub> hydrate has been studied by a number of techniques, including NMR spectroscopy,<sup>4,5</sup> IR spectroscopy,<sup>6</sup> X-ray diffraction,<sup>7,8</sup> and neutron diffraction. 9-11 These studies indicate that CO<sub>2</sub> occupies both cavities in the sI hydrate structure, having approximately full occupancy of the larger cavities and variable occupancy of the small cavities, dependent on the synthesis conditions. In naturally occurring gas hydrates,  $CH_4$  typically is the principal "guest" molecule with a variety of condensed alkanes and inorganic gases such as  $N_2$ ,  $H_2S$ , and  $CO_2$  present as additional constituents.

Concerns about the effect of greenhouse gases, such as atmospheric CO<sub>2</sub> produced by fossil fuel combustion, on global warming have intensified in the past decade. Sequestering large amounts of liquid CO2 in deep ocean settings has been proposed. Numerous researchers have observed the interaction between CO<sub>2</sub> liquid and seawater in the laboratory (e.g., ref 12) and in a natural setting, where researchers observed the direct release of gaseous and liquid CO<sub>2</sub> at a range of depths in the ocean.<sup>13</sup> Investigations of CO<sub>2</sub> hydrate properties and reaction kinetics, in the laboratory as well as in marine settings, are relevant to the possible large-scale disposal of liquid CO<sub>2</sub> in deep ocean environments, where CO<sub>2</sub> hydrate readily forms at the CO<sub>2</sub> liquid-seawater interface. With this purpose in mind, we have built on preliminary work in the CO<sub>2</sub>-H<sub>2</sub>O system<sup>2,3</sup> to (1) find a reliable, reproducible, and efficient method for CO<sub>2</sub> hydrate synthesis, (2) characterize the texture, structure, and composition of this material, (3) investigate the dissociation behavior of CO<sub>2</sub> hydrate in a CO<sub>2</sub> gas atmosphere at 0.1 MPa, including comparison with sI CH<sub>4</sub> hydrate studied under similar condi-

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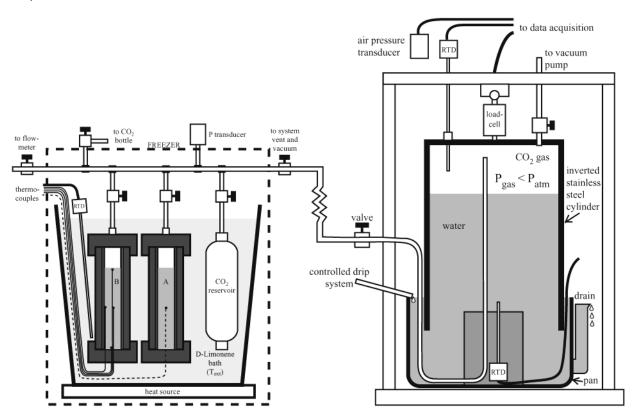


Figure 1. Schematic drawing (not to scale) of the synthesis apparatus showing the pressure vessels with internal thermocouple configurations, the  $CO_2$  reservoir (150 cm<sup>3</sup>), and their immersion in a bath of D-limonene. The apparatus is located in a commercial freezer, and the bath is heated from below to raise the temperature above the ambient freezer temperature (about  $252 \pm 3$  K). Bath temperature ( $T_{ext}$ ) is monitored with a resistance temperature detector (RTD). When an internal thermocouple is used in Sample A, it is located along the cylinder axis at the sample middle (height is 4.7 cm). In Sample B, three thermocouples are located along the cylinder axis at the top (8.9 cm from sample bottom), middle (4.7 cm), and bottom (0.6 cm) of the sample. A side thermocouple (4.8 cm) measures temperature a few millimeters in from the sample surface. The vessel interior is packed with granular  $H_2O(s)$  (shown as the gray-shaded space), and the free space is filled with  $CO_2$  liquid (metal disks, not shown, are placed on the sample top to decrease the fluid volume). The thermocouples, RTD, and pressure transducer are interfaced with a data acquisition system. The apparatus is connected to a flow meter (modified from Figure 1 in Circone et al.<sup>20</sup>), which monitors  $CO_2$  evolution during hydrate dissociation. As gas is released during hydrate dissociation, it is collected in the inverted, close-ended cylinder of the flow meter, which is suspended from a load cell. The evolved gas displaces the water in the column, and the corresponding weight change is measured over time and converted into moles of gas, from which the amount and rate of gas release is calculated. Refer to Circone et al.<sup>20</sup> for further details. The flow meter and controlled drip system are enclosed in  $CO_2$  gas-filled bags (not shown) to keep the system saturated in  $CO_2$ .

tions, <sup>14</sup> and (4) provide well-characterized samples for a collaborative research project to determine the dissolution rates of CH<sub>4</sub> and CO<sub>2</sub> hydrates in a deep ocean setting. <sup>15</sup>

# **Experimental Methods**

Synthesis Setup. Structure I CO<sub>2</sub> hydrate was synthesized starting from liquid CO<sub>2</sub> and solid H<sub>2</sub>O using the methodology for synthesizing pure CH<sub>4</sub> hydrate<sup>16</sup> and also following a twostage synthesis process for CO2 hydrate used by Henning et al.<sup>11</sup> The synthesis apparatus and seed ice preparation have been described previously.<sup>16</sup> We synthesize two 2.54 cm diameter by 12 cm long cylinders of CO<sub>2</sub> hydrate at a time (Figure 1). There are two pressure vessels: vessel A had either no thermocouples or one centered internal thermocouple, and vessel B had four internal thermocouples (Figure 1). The pressure vessels were first packed at temperatures near 250 K with  $\sim$ 26 g of H<sub>2</sub>O seed ice with a grain size of 180–250  $\mu$ m and a nominal intergranular porosity of 52%. Deuterated samples were made from 29 g of D<sub>2</sub>O seed ice and the same size fraction packed to a nominal intergranular porosity of 56%. The vessels are then suspended in a fluid bath housed in a conventional freezer. After evacuating the vessels for 1.5 min to remove air, they were first filled with cold CO<sub>2</sub> gas from the CO<sub>2</sub> reservoir and then slowly pressurized with room-temperature CO<sub>2</sub> liquid from a large bottle. Because the internal vessel temperature

increased as warm  $CO_2$  was introduced, the flow rate of  $CO_2$  liquid was controlled to maintain the temperature below 260 K as the vessels were filled with  $CO_2$  liquid to a pressure near 6 MPa, taking up to 0.5 h. The vessel interiors attained thermal equilibrium with the surrounding bath before we started the synthesis cycle, during which some hydrate formation occurred, as evidenced by a slow and steady decrease in  $CO_2$  liquid pressure.

**Synthesis Procedure.** Initially, we synthesized CO<sub>2</sub> hydrate using a two-stage, two-cycle heating method. Samples were first heated to 267.5 K, 17  $\pm$  2 MPa and held isothermal for approximately 20 h. Once all of the CO2 gas in the system had condensed (by 255 K and 6.0 MPa), the pressure climbed rapidly during heating because of the low compressibility of the CO<sub>2</sub> liquid. Samples were then heated through the H<sub>2</sub>O solidus to  $280 \pm 1$  K,  $23 \pm 2$  MPa and again held isothermal for approximately 20 h before cooling to ambient freezer temperatures near 250 K (cycle 1, Figure 2a). We checked for the presence of unreacted H<sub>2</sub>O in the samples by looking for temperature or pressure increases during cooling through the H<sub>2</sub>O ice point due, respectively, to heat release and to a volume increase upon H<sub>2</sub>O freezing. This can be detected in samples containing a few percent unreacted H<sub>2</sub>O, and these samples were heated again to 281 K, 20  $\pm$  2 MPa and held isothermal for approximately 20 h before cooling to ambient freezer temperCO<sub>2</sub> Hydrate J. Phys. Chem. B C

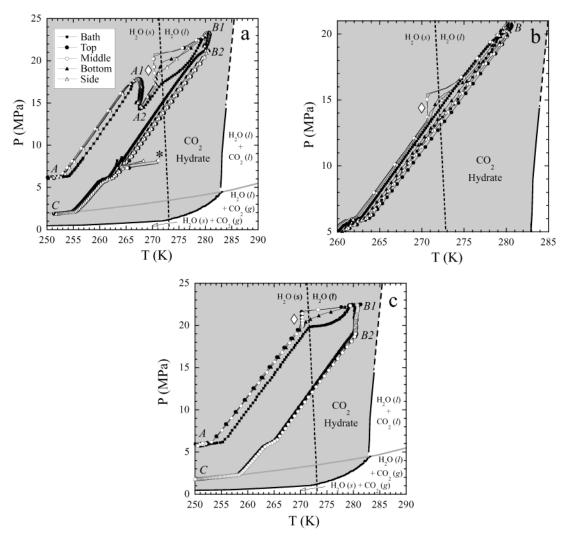


Figure 2. Pressure—temperature history during CO<sub>2</sub> hydrate synthesis by either a two-stage, two-cycle heating method (a, b) or a single-stage, one-cycle method (c). Phase boundaries for the CO<sub>2</sub>-H<sub>2</sub>O system (CO<sub>2</sub> hydrate = shaded area) and for the CO<sub>2</sub> gas/liquid boundary (gray line) are from the phase equilibria data summarized in Sloan; the H<sub>2</sub>O solid/liquid boundary is also shown (dashed line). Every fourth data point for internal sample temperatures is plotted, and all data for external bath temperature are plotted. In panel a, CO<sub>2</sub> pressure as a function of bath and sample temperatures is shown. Two-stage heating in the first cycle involves heating at a rate of 13 K/h to 267.5 K (A to A1) for a 20-hour isothermal hold (A1 to A2) and then heating to 281 K (A2 to B1) for a 20-hour isothermal hold (B1 to B2), followed by cooling back to ambient freezer temperature (B2 to C). The internal sample temperatures are displaced 1-2 K from the bath temperature ( $T_{\rm ext}$ ) during heating and cooling because of the delay in heat transfer through the pressure-vessel walls. This effect is more pronounced, especially during heating, in the sample interior (middle, top) than along the sample surfaces (bottom, side). The internal sample temperatures buffer near 270 K ( $\Diamond$ ) for up to 60 min and lag the external bath temperature by up to 8 K before eventually equilibrating with the bath. Note that data points at a given pressure are isotemporal such that at the diamond the temperature distribution in the bath and the sample interior were as follows: bath > side > bottom > top and middle of the samples. During cooling, the sharp CO<sub>2</sub> pressure increases near 264 K and 8 MPa coincide with the anomalous temperature increase (\*) observed in sample B (sample A did not contain internal thermocouples). The P, T slope flattens near 6 MPa during heating and cooling as the CO2 gas condenses in the sections of tubing outside of the freezer (see Figure 1). By the end of cycle 1, the CO<sub>2</sub> pressure has dropped significantly because of hydrate formation, and the CO<sub>2</sub> liquidus is intersected near 256 K. Panel b shows CO<sub>2</sub> pressure as a function of bath and sample temperatures during cycle 2, which involves direct heating from near 250 to 281 K, followed by a 16 h isothermal hold at 281 K (B) before cooling to 250 K. The thermal lag near 270 K (\$\dightarrow\$) is again observed during heating; however, there is no anomalous pressure or temperature increase during cooling, and the pressure offset due to hydrate formation is greatly reduced in this cycle. Panel c shows CO<sub>2</sub> pressure as a function of bath temperature and internal sample temperatures during single-stage, single-cycle synthesis of CO<sub>2</sub> hydrate by direct heating to 281 K (A to B1), followed by a 50 h isothermal hold at 281 K (B1 to B2) before cooling (B2 to C). Again, a thermal lag near 270 K (⋄) is observed, and upon cooling no anomalous increase in pressure or temperature is detectable. See text for a discussion of the significance of the thermal lags and anomalous changes in pressure and temperature.

ature (cycle 2, Figure 2b), at which point conversion of all H<sub>2</sub>O to hydrate was complete. The two-stage heating process was used to make the deuterated sample analyzed by neutron diffraction (see below). In subsequent syntheses of CO<sub>2</sub> hydrate, a single heating stage from 252 to 282 K, followed by an isothermal hold for 30–50 h, resulted in complete conversion of the reactants to hydrate (Figure 2c). After synthesis, samples were either dissociated or recovered for further study (see below).

**Sample Recovery.** In earlier experiments in this laboratory,  $CO_2$  hydrate was synthesized successfully both in bulk and microscopically in an optical cell apparatus using  $H_2O$  seed ice and  $CO_2$  gas or liquid. The absence of pressure anomalies in the synthesis record of samples made at the highest pressures (up to 16 MPa) indicates that the conversion to hydrate was complete. However, recovered bulk samples were plagued by the presence of large amounts of solid  $CO_2$  after quenching in liquid nitrogen, and further analysis of these samples using other

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techniques (such as measuring the CO<sub>2</sub> content of the hydrate by weighing) was not possible.

More recently, we have been able to expel excess CO<sub>2</sub> by flushing with CH<sub>4</sub> gas. Henning et al. 11 were able to recover CO<sub>2</sub> hydrate samples free of excess CO<sub>2</sub> and without appreciable dissociation by flushing the samples with He. We tried flushing the samples with CH<sub>4</sub> because of a separate research interest in temporarily holding CH<sub>4</sub> and CO<sub>2</sub> hydrate samples together in the same vessel without partial dissociation or exchange.<sup>15</sup> Following synthesis, samples equilibrated near 252 K and 2.0 MPa (point C, Figure 2) such that CO<sub>2</sub> liquid filled the sample pore space. We released CO<sub>2</sub> from the system in several pulses over 1-1.5 h, until the pressure stabilized near 252 K at 1.0 MPa in the CO<sub>2</sub> gas-only phase field (Figure 2). Then samples were pressurized with CH<sub>4</sub> gas to 1.9 MPa and vented to 1.0 MPa, and this flushing cycle was repeated four to six times over the next 0.5 h to dilute the free CO<sub>2</sub>. The sample vessels were isolated at pressure and removed from the synthesis apparatus, stored at 252 K and 1.0 MPa gas pressure for less than 0.5 h or for 48 h, and then plunged into liquid nitrogen while the gas pressure was dropped to 0.1 MPa. The CH<sub>4</sub> flushing did not remove all of the CO<sub>2</sub> gas but diluted it to the extent that, after depressurization to 0.1 MPa, no residual CO<sub>2</sub> solid was detected by powder X-ray diffraction or neutron diffraction analysis.

Some of the  $CH_4$ -flushed samples were dissociated and then analyzed by gas chromatography to determine whether there was any appreciable  $CO_2$ — $CH_4$  exchange. One sample, quenched in liquid  $N_2$  within minutes after flushing, contained trace  $N_2$  but no detectable  $CH_4$ . Another sample, stored for 48 h, showed the gas content to be nearly pure  $CO_2$  with only 163 ppm of  $CH_4$  and trace amounts of  $N_2$ . Given the very low levels of  $CH_4$  incorporated in the gas released during hydrate dissociation, we judged this procedure for removal of pore  $CO_2$  with no dissociation of the hydrate (see below) to be a success.

Scanning Electron Microscopy. Images were obtained with a LEO 982 field emission scanning electron microscope equipped with a cryochamber for sample preparation and a cryostage in the microscope (Gatan Alto 2100 cryosystem). Samples were loaded onto a holder then transferred from liquid nitrogen to the preparation chamber at 93 K. A fresh surface free from condensation of atmospheric water was made by fracturing the sample with a scalpel in the preparation chamber, and then this surface was cold sputter-coated with gold—palladium before transferring to the microscope stage. Images were obtained at 2.0 keV and 45  $\mu$ A, while the sample temperature was maintained between 113 and 123 K.

Powder Diffraction Analysis. Several samples were analyzed by powder X-ray diffraction near 77 K. The diffraction data was collected usually on a middle cross section of the sample cylinder, while liquid nitrogen was dripped onto the sample to maintain low temperature. Samples were scanned from 15° to  $48^{\circ}$   $2\theta$  at  $0.5^{\circ}$ /min using Cu K $\alpha$  radiation (1.5418 Å). Hydrogenous CO<sub>2</sub> hydrate and deuterated CO<sub>2</sub> hydrate were examined by neutron diffraction at the high-resolution powder diffraction beam lines HRPD (Japan Atomic Energy Research Institute, JAERI) and BT-1 (National Institute of Standards and Technology, NIST), respectively. Data from JAERI were collected from 5° to 165°  $2\theta$  in 0.05° steps using a monochromatic neutron beam with wavelength 1.163 Å; data were collected between 8 and 215 K at ambient pressures. Data from NIST were collected from  $4^{\circ}$  to  $160^{\circ}$   $2\theta$  in  $0.05^{\circ}$  steps using a monochromatic neutron beam with wavelength 1.540 Å; data were collected at 4.2, 50, 75, and 100 K at ambient pressure.

Crystal structure parameters were refined by the Rietveld method using the GSAS software package.<sup>17</sup> More detailed description of the refinement methods are given in Chakoumakos et al.<sup>18</sup> and in a similar study of propane hydrate.<sup>19</sup>

Measurement of CO<sub>2</sub> Gas. Our custom-built, water-based flow meter<sup>20</sup> (see Figure 1) has been used successfully to measure CH<sub>4</sub> gas evolution from dissociating CH<sub>4</sub> hydrate samples. 14,21 To measure CO<sub>2</sub>, which is 28 times more soluble than CH<sub>4</sub> in water, several modifications to the apparatus were made: (1) both the water reservoir for the controlled drip system and the flow meter itself were enclosed in CO2 gas-filled glovebags and the water reservoir was agitated to promote CO<sub>2</sub> dissolution; (2) the gas inlet inside the flow meter cylinder was raised so that the CO<sub>2</sub> gas did not mix the water column as it entered; (3) the flow meter was primed with CO<sub>2</sub> gas several times for a few days prior to the dissociation experiment to promote CO<sub>2</sub> saturation of the water within the cylinder; (4) baseline drifts of 0.1 to 0.3 mV/h in the load-cell output (due to continued solution of CO<sub>2</sub> in the water column during periods of no gas flow) were incorporated into the data analysis. With these modifications, we were able to minimize changes due to CO<sub>2</sub> dissolution during the dissociation measurements. Nonetheless, slow dissolution produced a steady positive baseline drift in the load-cell output data. Because the starting and ending baseline drifts were not equal and the intervening interval was dominated by large changes in load-cell output due to gas flow, there is uncertainty in the baseline correction in this region. We assumed that the baseline drift lies between the starting and ending values, and depending on which baseline correction is applied, we obtained yields of 100% with uncertainties on the order of  $\pm 3\%$  in the measurements of hydrate stoichiometry (see below), which are higher than the calculated uncertainty for CH<sub>4</sub> ( $\pm 1\%$ ).<sup>20</sup>

Hydrate Dissociation Experiments. Two types of experiments, both utilized previously to study the dissociation behavior of CH<sub>4</sub> hydrate, 14,22 were performed at 0.1 MPa on CO<sub>2</sub> hydrate: (1) temperature ramping at fixed pressure and (2) pressure release at fixed temperature. In temperature ramping, the CO<sub>2</sub> hydrate sample was first depressurized to conditions in the CO<sub>2</sub> gas stability field (1.0 MPa near 250 K) and then cooled slowly while maintaining  $P_{\text{CO}_2}$  below the  $\text{CO}_2$ liquidus, before equilibrating at 208–210 K at 0.1 MPa for up to 20 min (P, T conditions in the CO<sub>2</sub> hydrate stability field). Then the sample was warmed at an average rate of 13 K/h to 282 K, while both sample and bath temperatures were monitored and while released CO2 gas was collected in the flow meter. In pressure-release experiments, the CO<sub>2</sub> hydrate sample was equilibrated at some constant temperature between 238 and 277 K, then pressure was lowered to a pressure still in the hydrate and CO<sub>2</sub> gas stability fields. To start the experiment, pressure was rapidly decreased to 0.1 MPa within 20 s, and then internal sample temperature(s) and released CO2 were monitored continuously, while the external bath temperature was held isothermal. In experiments performed at temperatures below 273 K, the experiments were concluded by warming the samples to 282 K to release the remaining CO<sub>2</sub>.

# Synthesis and Sample Characterization—Results and Discussion

CO<sub>2</sub> hydrate has been successfully synthesized in bulk from fine-grained seed ice and CO<sub>2</sub> liquid, resulting in complete conversion to hydrate with excess CO<sub>2</sub> liquid remaining. In the two-stage, two-cycle synthesis procedure, the pressure dropped monotonically during the isothermal hold at 267.5 K

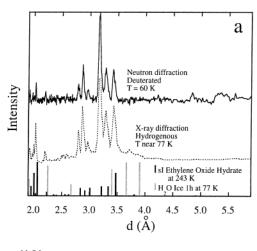
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(Figure 2a, A1 to A2), as  $CO_2$  reacted with  $H_2O(s)$  to form hydrate. The evolution of the  $CO_2$  pressure over time is consistent with the results of Henning et al.<sup>11</sup> on  $D_2O$  ice +  $CO_2$  liquid. They determined that about 70%  $\pm$  5% of the  $D_2O$  converted to  $CO_2$  hydrate after 15 h at 263 K and similar pressures and that the amount of conversion to hydrate after a fixed time interval increased with increasing temperature from 230 to 263 K. Therefore, we surmise that, in our experiments, after 20 h at 267.5 K a significant amount of  $CO_2$  hydrate formation had occurred but that unreacted  $H_2O$  still remained.

When the bath was heated to 281 K (Figure 2a, A2 to B1), the internal sample temperature held steady between 270 and 271 K (diamond) as the bath temperature rose continuously and the pressure climbed from 17 to 21 MPa. This thermal buffering does not correspond to any phase boundaries in the CO<sub>2</sub>-H<sub>2</sub>O system that involve hydrate but parallels the  $H_2O(s) = H_2O(1)$ reaction that lies approximately 1.5 K higher at these pressures. We infer that significant melting of the unreacted H<sub>2</sub>O occurred (Figure 2a, diamond) and that the melting point was depressed by the solution of CO<sub>2</sub> in H<sub>2</sub>O(l). Once the remaining free H<sub>2</sub>O(s) melted, temperatures in the sample quickly attained thermal equilibrium with their surroundings. As the samples were held at 281 K (Figure 2a, B1 to B2), the liquid CO2 pressure continued to drop as the CO<sub>2</sub> hydrate formation reaction proceeded. After 20 h at 281 K, the sample was cooled to ambient freezer temperature (Figure 2a, B2 to C). The temperature and pressure decreased smoothly with time until the temperature neared 265 K, at which point the pressure and the sample temperature abruptly increased because of the freezing of unreacted H<sub>2</sub>O(l), which occurs at a depressed temperature in part because of the solution of CO<sub>2</sub> in the H<sub>2</sub>O(l).

A second heating cycle over 24 h is required to react the remaining free  $\rm H_2O$  (Figure 2b). During heating, the temperatures at the sample top and middle again buffer at 270–271 K for several minutes (diamond), although this thermal signal persists for a shorter time (25 vs 55 min in cycle 1). After another isothermal hold at 281 K for  $\sim$ 18 h, the samples are cooled to freezer temperature, and no  $\rm H_2O$  freezing anomalies appear in the pressure or temperature record. We conclude at this point that the reaction has gone to completion. In an attempt to avoid heating the samples through a second cycle to 281 K, in one experiment the samples were held for >48 h at 281 K during the first two-stage cycle (not shown). When the sample was cooled, the freezing anomaly was much less pronounced in size and duration, but still present, requiring the additional heating cycle for complete conversion to hydrate.

In the single-stage synthesis process for CO<sub>2</sub> hydrate (Figure 2c), the results are similar to those described above for the twostage, two-cycle process. The buffering between 270 and 271 K (diamond) is again observed and lasts almost an hour. At the isothermal hold temperature of 281 K, the pressure decreases monotonically (Figure 2c, B1 to B2) with an increasingly shallow slope with time (not shown) as hydrate forms. We also observed a distinct overstep of the sample temperature over the external bath temperature by 1-2 K once isothermal conditions were reached at 281 K (Figure 2c, near B1). We believe that this sample temperature increase is due to sufficiently rapid formation of CO<sub>2</sub> hydrate such that heat generated from the exothermic hydrate formation reaction is not exchanged quickly enough with the surroundings to maintain thermal equilibrium. There is no other heat source for raising the vessel temperatures above that of the surrounding bath. Similar temperature oversteps have been observed during the synthesis of larger diameter (3.18 cm) samples of CH<sub>4</sub> hydrate (unpub-



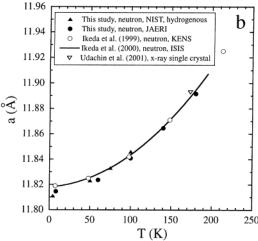


Figure 3. Powder X-ray diffraction pattern (a) of hydrogenous CO<sub>2</sub> hydrate, a portion of the powder neutron diffraction pattern of deuterated CO<sub>2</sub> hydrate, and peak positions and intensities for sI hydrate<sup>23</sup> and H<sub>2</sub>O ice. The peak positions obtained for our synthetic CO<sub>2</sub> hydrate samples correspond well to the published positions for sI hydrate (allowing for the systematic offset due to the difference in data collection temperature), although the relative peak intensities do not. The appearance of possible low-intensity ice peaks in the X-ray diffraction patterns of the hydrogenous and deuterated (not shown) CO<sub>2</sub> hydrate samples are not confirmed in the more sensitive neutron diffraction pattern, which probes grain interiors, as well as the surfaces. The likely source of these ice peaks is the unavoidable formation of H<sub>2</sub>O ice condensate on the sample surface during data collection. Panel b shows lattice parameter vs temperature for hydrogenous (▲) and deuterated (●) CO<sub>2</sub> hydrate synthesized using our method. Our results are in close agreement with those obtained by Ikeda et al.<sup>10</sup> (O), Udachin et al.8 (\nabla), and Ikeda et al.24 (polynomial fit to data collected between 5 and 195 K at intervals of 10 K) on deuterated samples synthesized at lower pressures.

lished data). After 30-50 h at 281 K, no anomalous pressure or temperature increases are observed upon cooling, indicating that complete conversion of  $H_2O$  to hydrate with one heating cycle and in less total time (50-70 h versus 85 h) has resulted. Thus, the single-stage procedure initially used for  $CO_2$  hydrate synthesis<sup>2,3</sup> is deemed the more efficient method.

Samples were characterized in several ways: physical appearance (both macroscopic and by scanning electron microscopy (SEM)), powder X-ray and neutron diffraction analysis, direct measurement of  $CO_2$  uptake by sample weighing, and measurement of the amount of  $CO_2$  released during dissociation. The  $CO_2$  hydrate samples are fine-grained, cohesive, and radially and axially homogeneous. Although the internal thermocouples record a significant  $H_2O$  melting event when the samples are

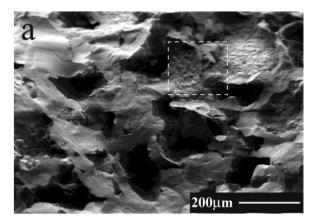
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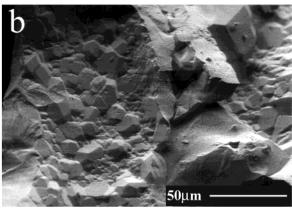
TABLE 1: Rietveld Crystal Structure Refinement Results for CO<sub>2</sub> Deuterate<sup>a</sup>

	T(K)	8	60	100	140	180
	a (Å)	11.8143(7)	11.8241(9)	11.840(1)	11.864(1)	11.891(2)
$ ho_{ m cal}$	$_{c}$ (g/cm <sup>3</sup> )	1.282	1.279	1.274	1.266	1.257
	$R_{\rm p}$	0.063	0.062	0.061	0.062	0.061
	$\chi^2$	1.248	1.187	1.145	1.156	1.097
V	ariables			34		
			Host Ato	oms		
$O_k$	X			0		
	y	0.309(1)	0.308(1)	0.306(1)	0.306(2)	0.306(2)
	Z o -	0.119(1)	0.116(1)	0.118(1)	0.114(1)	0.118(2)
	$U_{\rm iso}({\rm \AA}^2)$	0.008(1)	0.012(1)	0.015(1)	0.021(3)	0.025(3)
$O_i$	x = y = z		0.184(1)	0.187(1)	0.184(1)	0.185(2)
_	$U_{\rm iso}({\rm \AA}^2)$	0.008(1)	0.012(1)	0.015(1)	0.021(3)	0.025(3)
$O_c$	x			0		
	y z					
	$U_{\rm iso}$ (Å <sup>2</sup> )	0.008(1)	0.012(1)	0.015(1)	0.021(3)	0.025(3)
$D_{ik}$	x	0.125(2)	0.133(3)	0.118(2)	0.120(3)	0.127(3)
	y	0.226(2)	0.239(3)	0.221(2)	0.227(3)	0.222(3)
	Z	0.185(3)	0.184(4)	0.186(3)	0.195(3)	0.188(4)
	$U_{\rm iso}$ (Å <sup>2</sup> )	0.040(4)	0.057(6)	0.040(4)	0.041(5)	0.037(5)
$O_{ki}$	X	0.073(3)	0.078(3)	0.080(2)	0.078(3)	0.074(3)
n.t	y	0.257(2)	0.252(3)	0.264(2)	0.253(3)	0.258(3)
	Z	0.142(2)	0.151(3)	0.142(3)	0.140(3)	0.141(3)
	$U_{\rm iso}$ (Å <sup>2</sup> )	0.040(4)	0.057(6)	0.040(4)	0.041(5)	0.037(5)
$O_{kk}$	X			0		
na.	y	0.314(4)	0.313(4)	0.311(4)	0.319(4)	0.316(5)
	Z	-0.041(3)	-0.039(3)	-0.051(3)	-0.045(3)	-0.052(3)
	$U_{\rm iso}({\rm \AA}^2)$	0.040(4)	0.057(6)	0.040(4)	0.041(5)	0.037(5)
$O_{kc}$	x	. ,	. ,	0	. ,	. ,
	y	0.380(4)	0.381(4)	0.366(4)	0.366(4)	0.366(4)
	z	0.130(4)	0.136(4)	0.137(3)	0.142(4)	0.139(4)
	$U_{\rm iso}({\rm \AA}^2)$	0.040(4)	0.057(6)	0.040(4)	0.041(5)	0.037(5)
$O_{ck}$	X			0		
	y	0.428(3)	0.436(4)	0.437(3)	0.440(3)	0.433(4)
	z _	0.183(3)	0.172(3)	0.182(3)	0.185(3)	0.185(4)
	$U_{\rm iso}({\rm \AA}^2)$	0.040(4)	0.057(6)	0.040(4)	0.041(5)	0.037(5)
$O_{ii}$	x = y = z	0.230(2)	0.232(3)	0.229(2)	0.229(2)	0.231(3)
	$U_{\rm iso}({\rm \AA}^2)$	0.040(4)	0.057(6)	0.040(4)	0.041(5)	0.037(5)
			Guest At	oms		
$c_{s}$	x = y = z	0	0	0	0	0
	$U_{\rm iso}({\rm \AA}^2)$	0.014(9)	0.013(8)	0.004(7)	0.02(1)	0.01(1)
$)_{S}$	X			-0.0842		
	y			0.0343		
	z			0.0343		
	$U_{\rm iso}({\rm \AA}^2)$	0.014(9)	0.013(9)	0.004(7)	0.02(1)	0.01(1)
	n			1/12		
$C_{\rm L}$	X			0		
	y					
	Z ° 2					
	$U_{\rm iso}({\rm \AA}^2)$	0.08(1)	0.09(1)	0.06(1)	0.07(1)	0.07(2)
$O_{L1}$	X			-0.0268		
	y			0.3161		
	Z ° °			0.5661		
	$U_{\rm iso}({\rm \AA}^2)$	0.08(1)	0.09(1)	0.06(1)	0.07(1)	0.07(2)
	n			1/8		
$O_{L2}$	X			0.0268		
	у			0.1839		
	Z o -			0.4339		
	$U_{\rm iso}({\rm \AA}^2)$	0.08(1)	0.09(1)	0.06(1)	0.07(1)	0.07(2)
	n			1/8		

 $^a$  Space group Pm3n. Atomic site labels follow that of Ikeda et al.,  $^{24}$  and rigid body constraints are used to describe the guest molecule positions. Occupancies of the deuterium sites were fixed at 0.5. Isotropic displacement parameters for like atoms were constrained to be the same.

warmed through the  $H_2O$  ice point (described above), there is no textural evidence that unreacted  $H_2O$  coalesced or pooled in the samples. After synthesis is complete, as determined by the absence of anomalous pressure or temperature increases upon cooling through the  $H_2O$  ice point, we have pure synthetic  $CO_2$ 





**Figure 4.** Representative SEM images of deuterated CO<sub>2</sub> hydrate: (a) fractured surface of hydrate, exhibiting densely crystallized regions of CO<sub>2</sub> hydrate with  $50-300~\mu m$  pore spaces distributed throughout the material. The texture suggests that the original intergranular seed ice porosity persisted during hydrate synthesis but that H<sub>2</sub>O mobility on a localized scale has eliminated the original seed ice grain texture. Panel b shows a magnified view  $(5\times)$  of the area outlined in panel a, showing that the pore cavities are lined with euhedral  $1-20~\mu m$  grains of hydrate. SEM images of hydrogenous CO<sub>2</sub> hydrate (not shown) exhibit features similar in scale and texture.

hydrate that is free of unreacted  $H_2O$  (see below). The samples typically contain 37 g of hydrate with a calculated porosity of  $44\% \pm 1\%$ .

X-ray and Neutron Diffraction. The powder X-ray and neutron diffraction patterns of both hydrogenous and deuterated CO<sub>2</sub> hydrate samples exhibit well-defined peaks for sI hydrate and no peaks attributable to solid CO2 (Figure 3a). The trace ice peaks in X-ray powder patterns of both hydrogenous and deuterated (not shown) CO<sub>2</sub> hydrates were probably due to H<sub>2</sub>O condensation from the atmosphere during data collection; no ice was detected by neutron diffraction, confirming that complete conversion of the starting material to deuterate was achieved. Rietveld refinements of the neutron diffraction data yielded thermal expansion for CO<sub>2</sub> hydrate that is consistent with earlier measurements (Figure 3b). Table 1 summarizes the Rietveld structure refinements results for the deuterated CO<sub>2</sub> hydrate. The refinement results are not as precise as those reported by Ikeda et al.;<sup>24</sup> however, we do largely corroborate the temperature-dependent behavior of the mean-square displacements of the guest molecules. One difference in our results is that the isotropic displacements increase in the order host  $O = CO_2$  in small cage < host D < CO<sub>2</sub> in large cage whereas the results of Ikeda et al.<sup>24</sup> are host O < host D < CO<sub>2</sub> in small cage < CO<sub>2</sub> in large cage. The large and nearly temperature-independent displacements of the guest molecules, particularly in the large CO<sub>2</sub> Hydrate J. Phys. Chem. B G

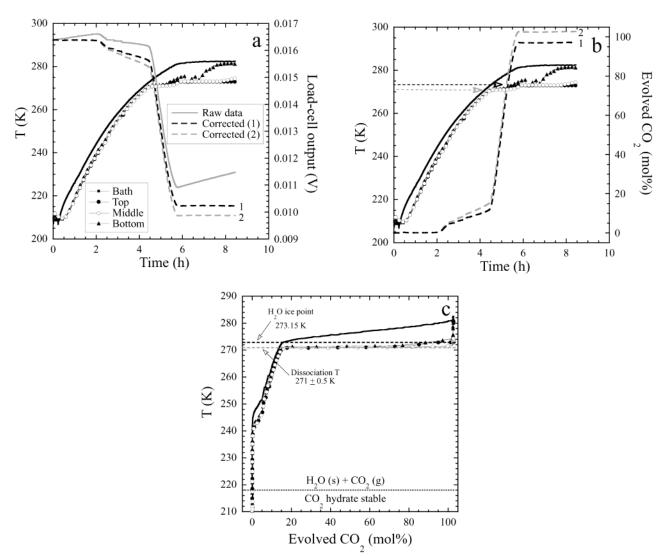


Figure 5. Results from a temperature-ramping experiment at 0.1 MPa on  $CO_2$  hydrate, in which the sample is slowly warmed from 210 to 282 K, resulting in complete dissociation of the hydrate to form  $H_2O(1 \text{ and s})$  and  $CO_2$  gas. In panel a external bath temperature and internal sample temperatures (every tenth data point plotted), as well as the load-cell output from the flow meter (gray line = raw data, gray and black dotted lines = baseline-corrected data), are continuously monitored as the hydrate dissociates and gas is released and collected in the flow meter. The initial baseline drift of the flow meter (0.119 mV/h between 0.5 and 1.8 h) and the final baseline drift (0.257 mV/h between 5.8 and 8.4 h) were collected over the intervals when no gas was evolving from the sample (on the basis of the linearity of the load-cell data and the sample temperature conditions). The baseline-corrected data (curves labeled 1 and 2) represent the range in which the actual corrected load-cell data may fall (see text). Panel b shows the external bath and internal sample temperatures (as in panel a) and the amount of  $CO_2$  gas evolved from the sample during dissociation. Internal sample temperatures are buffered at 271 K for over an hour (gray arrow), during which most of the gas is released from the hydrate, and also at 273 K for several hours (black arrow), during which no gas release occurs (see text for discussion). The buffering at 273 K is less pronounced at the sample bottom where ice melted first and liquid water coalesced. Evolved  $CO_2$  curves 1 and 2 represent the data range after baseline corrections are applied, resulting in an uncertainty of  $\pm 3\%$  in the measured total amount of evolved  $CO_2$ . Panel c shows the evolution of  $CO_2$  (only curve 2 results shown) vs external bath and internal sample temperatures of  $CO_2$  hydrate (symbols as in panel a). Maximum gas evolution rates of  $CO_2$  mol/h) occur at 271 K.

cage, imply a significant amount of positional disorder about the cage center, that is, movement of the  $CO_2$  molecule off from the cage center position. Earlier diffraction studies yielded stoichiometries for deuterated  $CO_2$  hydrate of  $6.20 \pm 0.15$ ,  $^86.1$  to 6.7,  $^{11}$  and 6.3 to 6.9 (depending on synthesis pressures of 6 to 1.5 MPa $^9$ ). It was not possible to extract cage occupancy information from the refinements of the diffraction data; however, we have been able to determine the  $CO_2$  gas contents of the samples by other means (see below).

Mass Uptake Measurements. The mass uptake results are in excellent agreement with the measured gas yields obtained from hydrate dissociation (see below). The mass uptake was measured on two samples that had been flushed with CH<sub>4</sub> gas before quenching in liquid nitrogen. The samples, encased in

an indium jacket with a bottom disk used for synthesis, were weighed on a Denver Instruments XP-300 balance (maximum capacity is 300 g with  $\pm 0.01$  g precision) that is routinely kept in a commercial freezer near 250 K. One sample, synthesized from 25.95 g of seed ice, gained 11.11 g after synthesis, yielding a composition of  $CO_2 \cdot 5.71H_2O$  if all weight gain is attributed to  $CO_2$  occupying hydrate sites. Another sample, synthesized from 25.98 g of seed ice, gained 11.25 g after synthesis, yielding a composition of  $CO_2 \cdot 5.64H_2O$ . Both measurements indicate that the water/carbon dioxide ratio is within 2% of the minimum value of n = 5.75 for fully occupied sI hydrate. The systematically high weight gains in part are due to observed  $H_2O$  condensation on the indium jacket during weighing; we cannot rule out the possibility that some free  $CO_2$  solidified during the

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quenching procedure, although no evidence for solid CO<sub>2</sub> was observed in the diffraction patterns.

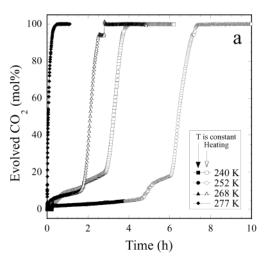
**SEM Imaging.** The CO<sub>2</sub> hydrate samples were imaged using scanning electron microscopy (SEM). A deuterated sample is shown in Figure 4. The dense crystalline hydrate contains large (typically  $50-300~\mu m$ ), irregularly shaped pore structures that are lined with euhedrally faceted hydrate crystals. This porosity is a relic of the starting intergranular seed ice porosity; however, the original ice grain boundaries have been fundamentally altered by hydrate crystallization. We infer a grain size in the hydrate from etching that develops on cleaved surfaces as the sample sits under vacuum in the SEM. This inferred grain size distribution (not shown in Figure 4) is comparable to that of the faceted pore-lining crystals (a few microns to a few tens of microns) and not that of the starting seed ice material (180–250  $\mu$ m).

#### Dissociation-Results and Discussion

**Dissociation Behavior.** The temperature-ramping experiments on  $CO_2$  hydrate yielded consistent results on hydrate gas content and gas release as a function of temperature (Figure 5) but exhibited unexpected dissociation behavior: at most only 20% of the observed  $CO_2$  gas content was released by 270 K, even though phase equilibria data<sup>1</sup> indicate that  $CO_2$  hydrate is stable only below 218 K at 0.1 MPa. The initial gas release occurred between 240 and 250 K in one or two pulses, sometimes sharply defined and accompanied by drops in the sample interior temperature, followed by a slow, steady release between 250 and 270 K. The remaining 80+% of the gas was released above 270 K in a sharply defined event (Figure 5b,c) in which the internal sample temperature was buffered at 271  $\pm$  0.5 K. Once gas evolution ceased, the internal sample temperature climbed to 273.2 K, the melting point of pure H<sub>2</sub>O.

Isothermal pressure-release experiments also were performed between 240 and 277 K (Figure 6). In the experiments performed below 273 K, slow, steady CO2 loss was observed during the isothermal portions of the experiments. Samples released up to 10% of their gas content during the isothermal holds, which lasted 0.3-3.8 h (Figure 6a). The average rate of dissociation (amount of gas released divided by the isothermal hold time) does not correlate simply with increasing temperature (240 K, 10.0 mol %/h; 252 K, 1.2 mol %/h; 268 K, 7.2 mol %/h); however, the facts that the 252 K experiment was on a deuterated sample and that the data set is limited make it impossible to describe the relationship between temperature and dissociation rate in any detail. As samples were heated to 282 K, the observed dissociation behavior was comparable to that observed in the temperature-ramping experiments in that by 270 K (273 K for D<sub>2</sub>O sample) up to 20% of the observed CO<sub>2</sub> loss had occurred, although the small, sudden gas releases and accompanying temperature decreases occurred at slightly warmer temperatures (255-265 K). The remaining 80% of the gas was released at 271  $\pm$  0.5 K. In the experiment on the deuterated sample, the buffering temperature of dissociation is displaced +3 K, which is slightly smaller than the difference in melting temperature of  $D_2O$ , +3.8 K.

In pressure-release experiments above 273 K (274 and 277 K), dissociation proceeded to completion as the external bath temperature was held isothermal. The internal sample temperatures dropped several degrees following the pressure release. In the 274 K experiment (not shown), the buffering temperature in the sample interior was  $271 \pm 0.5$  K, the same temperature interval observed during dissociation of  $CO_2$  hydrate under nonisothermal conditions (see above). In the 277 K



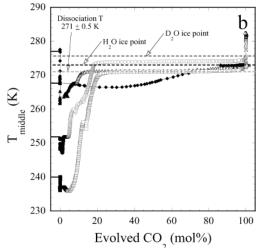


Figure 6. Evolution of CO2 gas after rapid depressurization of the hydrate sample to 0.1 MPa. A constant external temperature was maintained for some time interval (closed symbols) before heating the sample to 282 K (open symbols); transition from closed to open symbols indicates time at which heating of the external bath began. Temperatures and isothermal hold times are as follows: 240 K, 0.4 h (T settled at 238 K for most of isothermal hold); 252 K, 3.8 h (deuterated sample); 268 K, 1.2 h; 277 K, 1.2 h. Panel a shows the evolution of CO2 from hydrate sample over time. Sample held isothermally at 277 K dissociated completely and did not require further heating. CO<sub>2</sub> gas yields were normalized to 100%; however, actual yields were 90% (240 K), 73% (252 K), 78% (268 K), and 70% (277 K). See text for discussion of low yields. Panel b shows evolution of CO2 (only curve 2 results shown) vs temperatures of the external bath and sample middle (symbols as in panel a). During the rapid depressurization event, the internal sample temperature drops several degrees due to rapid expansion of the gas but rebounds by the end of the isothermal hold. In experiments performed below 273 K, the sample temperature reequilibrates with the external bath temperature within minutes, while above 273 K sample temperatures remain depressed as rapid dissociation of the hydrate occurs to completion.

experiment (Figure 6b), the sample interior was depressed below 268 K for more than 50% of the dissociation event and eventually reached 271 K after 75% of the sample dissociated. We suspect that the high rate of dissociation in this experiment may have produced the larger temperature depression.

**Hydrate Stoichiometry.** The gas content of the synthetic  $CO_2$  hydrate has been determined from the results of the temperature-ramping experiments, as we did previously for  $CH_4$  hydrate.<sup>20</sup> In three different temperature-ramping experiments, we obtained the following  $CO_2$  yields (with uncertainties of  $\pm 3\%$ , as described above): 103%, 102%, and 100%, based on the

CO<sub>2</sub> Hydrate J. Phys. Chem. B I

TABLE 2: Reported Compositions for Synthetic CO<sub>2</sub> Hydrate

reference	$T^a$	P <sub>equil</sub>	$P^b$ (MPa)		mathad
reference	(K)	(MPa)	(MPa)	n	method
Kuhs et al.9	273	1.2	1.5 - 6.0	6.9 - 6.3	neutron diffraction
Henning et al.11	278	2.2	6.2	$6.4 \pm 0.3$	neutron diffraction
Udachin et al.8	276	1.7	3.8	$6.20\pm0.15$	X-ray diffraction
this study	280	2.8	20.3	5.7	mass uptake
	280	2.8	18.3	5.6	mass uptake
	280.5	3.0	20.1	$5.59^{c}$	dissociation
	280.5	3.0	20.1	$5.64^{c}$	dissociation
	280.5	3.0	17.4	$5.74^{c}$	dissociation

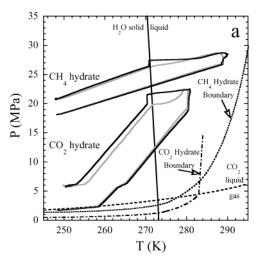
 $^a$  Kuhs et al. and Udachin et al. synthesized hydrate under isothermal conditions, whereas Henning et al. and this study synthesized hydrate at 263–278 K and 250–281 K, respectively. Maximum synthesis temperatures are shown in table.  $^bP$  for this study and for Henning et al. is the final pressure reached at the end of synthesis; in this study, initial pressures at 281 K were slightly higher (by up to 3 MPa) and decreased as synthesis reached completion.  $^c$  Uncertainty of  $\pm 3$  mol % corresponds to an uncertainty in n of  $\pm 0.15$  (see text).

assumption of full occupancy of all cages (i.e., n=5.75). The last experiment, which had a slightly lower gas yield, was annealed near 1.0 MPa and 252 K for 6 days before the temperature-ramping experiment because there was some concern that condensed  $\rm CO_2$  liquid was remaining in the sample after dropping pressure below the  $\rm CO_2$  gas/liquid boundary (this was a significant problem in synthetic propane hydrate samples made from propane liquid, unpublished data). The measured gas yields indicate that approximately all cages in the  $\rm CO_2$  hydrate are filled, which is consistent with the measured mass uptake of these samples (see above, Table 2). Unfortunately, we cannot extract cage occupancy information from the refinement of the neutron diffraction data in this study to corroborate this result.

Partial occupancy of small cages and nearly complete occupancy of large cages in CO2 hydrate has been determined for previous synthetic CO<sub>2</sub> hydrate samples, which had values of n of 6.2 or higher (Table 2). These samples were synthesized at maximum temperatures between 273 and 278 K and at pressures up to 6.0 MPa. In this study, using the methods described above, measured gas contents of CO<sub>2</sub> hydrate have values of n near 5.75, suggesting that both small and large cages are approximately filled. Two independent techniques have yielded a consistent hydrate number for samples made under our synthesis conditions, although we acknowledge that the techniques that we have utilized to determine n do have significant uncertainties. Kuhs et al. have shown that higher synthesis pressures yield higher cage occupancies (n = 6.9 at 1.5 MPa and n = 6.3 at 6.0 MPa, both at 273 K), while Udachin et al.<sup>8</sup> suggest that the overstep of the synthesis pressure above the hydrate equilibrium pressure (expressed as a ratio  $P/P_0$ ) is a relative indicator of the resulting cage occupancies. Since the samples in this study were synthesized at much higher CO2 liquid pressures  $(P/P_0 \text{ of } 6-7)$  than those in the earlier studies  $(P/P_0$  between 1 and 5), it is plausible that all cages could be approximately filled.

## Comparison with Structure I CH4 Hydrate

**Synthesis.** Using the technique developed by Stern et al., <sup>16</sup> complete conversion of the starting seed ice to sI hydrate is achieved at CH<sub>4</sub> gas or CO<sub>2</sub> gas/liquid pressures well above the equilibrium hydrate phase boundaries and at a range of temperatures that span the H<sub>2</sub>O solid/liquid-phase boundary (Figure 7a). The maximum synthesis temperature for CO<sub>2</sub> hydrate is about 10 K lower than that for CH<sub>4</sub> hydrate because



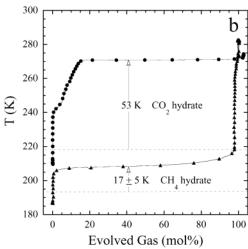


Figure 7. Comparison of sI CO<sub>2</sub> and CH<sub>4</sub> hydrate synthesis and dissociation, illustrating the relationship to their respective hydrate stability boundaries. Panel a shows typical pressure-temperature pathways for CO<sub>2</sub> and CH<sub>4</sub> hydrate synthesis. Bath temperatures (gray curves) and internal sample temperatures (black curves; only the temperature measured at the sample middle is shown, see text) are plotted. Pressure is for either CH<sub>4</sub> gas or CO<sub>2</sub> gas/liquid (see Figure 2). The following phase boundaries are indicated: CH<sub>4</sub> hydrate =  $CH_4(g) + H_2O(l \text{ or } s)$  (···);  $CO_2$  hydrate =  $CO_2(g \text{ or } l) + H_2O(l \text{ or } s)$  $(-\cdot -)$ ; CO<sub>2</sub> g = 1 (- - -); H<sub>2</sub>O s = 1 (-). The single-stage, singlecycle curve is shown for CO2 hydrate synthesis. Note that the temperature range over which the CO<sub>2</sub> hydrate sample temperature lags the external bath temperature (near 270 K) is displaced more than a degree below that in the CH<sub>4</sub> hydrate system (see text). Panel b shows the dissociation of CO<sub>2</sub> and CH<sub>4</sub> hydrate in temperature-ramping experiments. Samples were equilibrated at a starting temperature approximately 8 K below the equilibrium hydrate boundary at 0.1 MPa (---) and then heated isobarically at a rate of  $\sim$ 13 K/h. Internal sample temperatures (at sample middle) are shown, and every tenth data point is plotted (data collected at 60 s intervals). Vertical arrows indicate temperature offset between the equilibrium boundary and the dissociation temperature under dynamic heating conditions.

of the steepness of the hydrate phase boundary above the CO<sub>2</sub> liquidus, and the range of CO<sub>2</sub> pressure is controlled by the initial bottle pressure of the CO<sub>2</sub> source. Upon pressurization with hydrate-forming gas (either CH<sub>4</sub> or CO<sub>2</sub>) at temperatures below the H<sub>2</sub>O melting point, the ice surface converts to hydrate at an observable rate.<sup>2,3</sup> Hydrate growth proceeds at a rate that decreases with time after an initial period of rapid nucleation and growth.<sup>1,25</sup> From their isothermal neutron diffraction experiments below the D<sub>2</sub>O ice point, Henning et al.<sup>11</sup> and Wang et al.<sup>26</sup> showed that the rate of conversion increased with increasing

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TABLE 3: Comparison of Dissociation Behaviors of CO<sub>2</sub> and CH<sub>4</sub> Hydrates at 0.1 MPa<sup>a</sup>

1	2 7 0	
temperature interval	CO <sub>2</sub> hydrate	CH <sub>4</sub> hydrate
T <sub>eq</sub> at 0.1 MPa	218 K	193 K
	Temperature-Ramping (from Below $T_{eq}$ to 28)	2 K)
$T_{\rm eq}$ to $T_{\rm eq} + 25$ K	<10% of CO <sub>2</sub> is released	≥95% of CH <sub>4</sub> is released
$T_{\rm eq} + 25$ K to 270 K	>80% of the CO <sub>2</sub> remains	<3% of the CH <sub>4</sub> remains
near $T_{\text{melting}}$ of $H_2O$	remaining gas released (271.0 $\pm$ 0.5 K)	remaining gas released (272.5 $\pm$ 0.6 K)
	Rapid Depressurization (Experiments at Vario	us T)
$T_{\text{isothermal}} \leq T_{\text{eq}} + 46 \text{ K}$	$<$ 20% of $CO_2$ is released <sup>b</sup>	$\geq$ 90% of CH <sub>4</sub> is released <sup>c</sup>
$T_{\text{isothermal}} = 242 - 271 \text{ K}$		anomalous preservation <sup>d</sup>
$T_{\rm isothermal}$ to 282 K	remaining gas released (271.0 $\pm$ 0.5 K)	remaining gas released (272.5 $\pm$ 0.6 K)
$T_{\text{isothermal}} \ge 273 \text{ K}$	gas released while T buffered at 271.0 $\pm$ 0.5 K	gas released while T buffered at 272.5 $\pm$ 0.6 K

<sup>a</sup> Note that in all temperature-ramping experiments samples were heated at approximately 13 K/h (see Figures 5 and 7b). In rapid depressurization experiments at  $T_{\text{isothermal}} \leq T_{\text{eq}} + 46$  K and at  $T_{\text{isothermal}} \geq 273$  K, the isothermal portions of the experiments were performed over similar time intervals of up to a few hours (see Figure 6, refs 14 and 21). <sup>b</sup> Isothermal temperatures for individual experiments were 240, 252, and 268 K (268 K is actually +50 K above  $T_{\text{eq}}$ ). <sup>c</sup> Isothermal temperatures ranged from 204 to 239 K at approximately 5 K intervals. <sup>14</sup> <sup>d</sup> Dissociation rates are dramatically depressed relative to measured rates at isothermal temperatures below 239 K and above 272 K. For example, the average rate at 268 K (based on the time required to lose 50% of the sample's gas content) is less than 10<sup>-4</sup>%/s, whereas at 239 K the rate is 0.8%/s, a difference of 4 orders of magnitude. The rates in this temperature interval vary nonsystematically with increasing temperature. <sup>14</sup>

temperature, which was successfully modeled wherein the rate of reaction depends on a diffusion constant, the ice grain size (assuming spherical grain shapes with a controlled grain size distribution), and determination of the point at which the hydrate growth becomes dominated by diffusion of CO<sub>2</sub> and CH<sub>4</sub> through the external hydrate layer to the unreacted free water core. In an in situ X-ray diffraction study of CO<sub>2</sub> hydrate growth, Takeya et al.<sup>7</sup> also conclude that CO<sub>2</sub> diffusion is the rate-limiting step in hydrate growth below the H<sub>2</sub>O melting point.

Complete conversion of the free H<sub>2</sub>O to CH<sub>4</sub> or CO<sub>2</sub> hydrate occurs on an efficient time scale of a few days only when the temperature is increased above the H<sub>2</sub>O solidus and held at high temperature near the hydrate stability boundary for several hours. 11,16,26 As the temperature nears 273 K, the internal sample temperature is buffered at nearly constant temperature for as much as 1 h while the bath temperature continues to increase at a constant rate, and the buffering temperature decreases slightly as pressure increases (Figure 7a). In the CH<sub>4</sub> system, the buffering temperature is slightly depressed (~0.3 K) below that of the H<sub>2</sub>O solidus, while the depression is 1.2 K in the CO<sub>2</sub> system. We attribute the observed thermal buffering to the melting of ice (H<sub>2</sub>O or D<sub>2</sub>O, as described above), the temperature offsets from the pure H2O phase boundary to freezingpoint depression due to the solubility of CH<sub>4</sub> or CO<sub>2</sub> in the liquid water phase, and the greater offset in the CO<sub>2</sub> system to the greater solubility of CO2 in water.

The formation of a free water phase during hydrate synthesis can alter the sample texture and obscure the individual ice grain morphology under certain conditions. In optical cell experiments, Stern et al.<sup>2,3</sup> observed that particle morphology of individual grains of loosely packed ice starting material can be maintained as hydrate growth proceeds from the surface inward at temperatures that spanned the H2O melting point (under optimum synthesis conditions of high pressure above 25 MPa from finegrained seed ice of  $\leq 250 \,\mu\text{m}$ ; in experiments that did not meet these conditions, a discrete melt phase was observed). Moudrakovski et al.<sup>27</sup> also showed that, when hydrate-encapsulated ice (100-200 µm) was warmed above the H<sub>2</sub>O ice point under moderate CH<sub>4</sub> pressures (6-12 MPa), liquid water formed and remained discretely contained within the hydrate shells. In contrast, SEM micrographs of CO<sub>2</sub> hydrate (Figure 4) and CH<sub>4</sub> hydrates<sup>22</sup> clearly show that a substantial change in texture does occur during hydrate growth in the bulk samples that start with an intergranular ice porosity of nominally 40-50%. The discrete ice grain morphology is no longer evident, and the hydrate

crystallizes on a finer scale (typically grains are less than  $10-20~\mu m$  across) than the starting ice material ( $200~\mu m$ ), although some intergranular porosity persists. The observed textures indicate that free  $H_2O$  is locally mobile and not confined to the interiors of hydrate-bounded grains, and this may explain the rapid and complete conversion of remaining free  $H_2O$  to hydrate at temperatures above the  $H_2O$  solidus. These observed textural changes in the closely packed samples suggest that models of inward-diffusion of  $CO_2$  or  $CH_4$  through the outer hydrate layer of a spherical grain may be incomplete for describing nonisothermal hydrate growth at temperatures that span the  $H_2O$  ice point. The grain—grain contacts in closely packed ice starting material may spoil the spherical symmetry of the reaction by limiting appreciable gas diffusion at these points of contact.

**Dissociation.** The dissociation behavior of CO<sub>2</sub> hydrate is in marked contrast to the behavior of hydrocarbon gas hydrates. First, in temperature-ramping experiments at least 80% of the CO<sub>2</sub> hydrate persisted for several hours at temperatures reaching more than 50 K above its equilibrium phase boundary, while sI CH<sub>4</sub> hydrate<sup>14</sup> (Figure 7b, Table 3), sII methane-ethane hydrate,<sup>22</sup> and sII propane hydrate (unpublished data) released >95% of their gas contents within 25 K of their equilibrium boundaries. Second, although the CO<sub>2</sub> hydrate data set is limited, there is no evidence for the complex temperature-dependent dissociation behavior observed in pressure-release experiments on CH<sub>4</sub> hydrate. 14,22 The dissociation rate of CH<sub>4</sub> hydrate increases with increasing temperature up to 239 K (+46 K above  $T_{\rm eq}$ , the equilibrium temperature at 0.1 MPa), is significantly depressed between 242 and 272 K (+49 to 79 K above  $T_{eq}$ ), and then increases with increasing temperature above 272 K (see Table 3). The slowest rates are observed at 268 K ( $T_{eq}$  + 75 K). Conversely, the dissociation rate of CO<sub>2</sub> hydrate does not vary considerably with temperature between  $T_{\rm eq}$  and 268 K (+50 K). For example, in comparing experiments at +21 K above T<sub>eq</sub>, CH<sub>4</sub> hydrate released 97% of its gas content in 1.3 h, whereas CO<sub>2</sub> hydrate released less than 10% of its gas content in 0.5 h (or, extrapolating the data, at most 16% in 1.3 h). Third, the pressure-release experiments on CO<sub>2</sub> hydrate at temperatures below 273 K are wholly consistent with the dissociation behavior observed in the temperature-ramping experiments. Again this is in contrast to the behavior of CH<sub>4</sub> hydrate, in which amounts and rates of dissociation in both types of experiments are consistent below 240 K but not between 242 and 272 K. Furthermore, our observations are entirely consistent with the ability of Henning et al.<sup>11</sup> to vent the excess

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CO<sub>2</sub> at 263 K and repressurize with a different gas (in their case, He) without appreciable CO<sub>2</sub> hydrate dissociation.

However, in pressure-release experiments above 273 K, the observed dissociation behavior of  $CO_2$  hydrate is similar to that observed for  $CH_4$  hydrate<sup>21</sup> in that regardless of the starting temperature the internal sample temperatures plunge below the  $H_2O$  melting point following the pressure release and are buffered in a distinct temperature interval (272.5  $\pm$  0.5 K for  $CH_4$  hydrate) until dissociation nears completion and then climb to the  $H_2O$  melting point (Table 3). In the 277 K experiments, we note that in the  $CO_2$  system (1) the temperature depression due to adiabatic cooling from rapid release of gas pressure and the onset of hydrate dissociation is more pronounced (265 vs 271 K) and (2) the time to complete dissociation is less (0.5 vs 1.5 h for  $CH_4$ ).

In summary, the dissociation behavior of sI CO<sub>2</sub> hydrate is governed by one dominant characteristic: regardless of the pressure—temperature pathway the sample follows to conditions outside the hydrate stability field (i.e., by increasing temperature or by decreasing pressure), on a time scale of at least several hours the bulk of hydrate can persist metastably at 0.1 MPa until the temperature reaches 271 K, at which point all of the remaining CO<sub>2</sub> gas is released. This is in marked contrast to the highly temperature- and path-dependent behavior exhibited by sI CH<sub>4</sub> hydrate below 273 K. However, as temperatures near the H<sub>2</sub>O melting point, all of the remaining gas is released from the hydrate, regardless of the identity of the hydrate-forming gas, and the dissociation occurs in well-defined temperature intervals. In pressure-release experiments above 273 K, the dissociation behavior of CO2 hydrate is closely comparable to that of CH<sub>4</sub> hydrate.

# Conclusion

Applying the technique of Stern et al.16 for making CH<sub>4</sub> hydrate, we have synthesized bulk samples of CO2 hydrate from H<sub>2</sub>O or D<sub>2</sub>O ice/liquid and CO<sub>2</sub> liquid. Using a variety of techniques, we characterized the material's composition, microstructure, crystal structure, and dissociation behavior following various P, T pathways. CO<sub>2</sub> hydrate persists metastably at 0.1 MPa until temperatures near the H<sub>2</sub>O solid/liquid phase boundary are reached. This may suggest that for CO2 hydrate the dissociation to gas + ice is impeded and the formation of liquid water is the key to permitting rapid and complete breakdown of the hydrate. This phenomenon is not unique to CO<sub>2</sub> hydrate in that the final gas release from partially to almost completely dissociated CH<sub>4</sub> hydrate samples also occurs at temperatures just below the H2O ice point. However, the similarity ends there because the dissociation behavior of hydrate at temperatures below 273 K is as varied as the gas guest molecules themselves.

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#### References and Notes

- (1) Sloan, E. D. Clathrate Hydrates of Natural Gases, 2nd ed; Marcel Dekker: New York, 1998.
- (2) Stern, L. A.; Hogenboom, D. L.; Durham, W. B.; Kirby, S. H.; Chou, I.-M. J. Phys. Chem. B 1998, 102, 2627.
- (3) Stern, L. A.; Kirby, S. H.; Durham, W. B. Energy Fuels 1998, 12, 201.
  - (4) Ratcliffe, C. I.; Ripmeester, J. A. J. Phys. Chem. 1986, 90, 1259.
  - (5) Ripmeester, J. A.; Ratcliffe, C. I. Energy Fuels 1998, 12, 197.
  - (6) Fleyfel, F.; Devlin, J. P. J. Phys. Chem. 1988, 92, 631.
- (7) Takeya, S.; Hondoh, T.; Uchida, T. In *Gas Hydrates: Challenges for the Future*; Holder, G., Bishnoi, P., Eds.; New York Academy of Sciences: New York, 2000; pp 973–982.
- (8) Udachin, K. A.; Ratcliffe, C. I.; Ripmeester, J. A. J. Phys. Chem. B 2001, 105, 4200.
- (9) Kuhs, W. F.; Chazallon, B.; Klapproth, A.; Pauer, F. Rev. High-Pressure Sci. Technol. 1998, 7, 1147.
- (10) Ikeda, T.; Yamamuro, O.; Matsuo, T.; Mori, K.; Torii, S.; Kamiyama, T.; Izumi, F.; Ikeda, S.; Mae, S. *J. Phys. Chem. Solids* **1999**, *60*, 1527.
- (11) Henning, R. W.; Schultz, A. J.; Thieu, V.; Halpern, Y. J. Phys. Chem. A 2000, 104, 5066.
  - (12) Aya, I.; Yamane, K.; Nariai, H. Energy 1997, 22, 263.
- (13) Brewer, P. G.; Friederich, G.; Peltzer, E. T.; Orr, F. M. Science 1999, 284, 943.
- (14) Stern, L. A.; Circone, S.; Kirby, S. H.; Durham, W. B. J. Phys. Chem. B **2001**, 105, 1756.
- (15) Rehder, G.; Kirby, S. H.; Durham, W. B.; Brewer, P. G.; Stern, L. A.; Peltzer, E. T. *Geochim. Cosmochim. Acta*, submitted for publication, Fall 2002.
- (16) Stern, L. A.; Kirby, S. H.; Durham, W. B. Science 1996, 273, 1843.
   (17) Larson, A. C.; Von Dreele, R. B. General Structure Analysis System;
   Report LAUR 86-748; Los Alamos National Laboratory: Los Alamos, NM,
- (18) Chakoumakos, B. C.; Rawn, C. J.; Rondinone, A. J.; Marshall, S. L.; Stern, L. A.; Circone, S.; Kirby, S. H.; Jones, C. Y.; Toby, B. H.; Ishii, Y. *Proceedings of the Fourth International Conference on Gas Hydrates*, Yokohama, Japan; 2002; Vol. 2, pp 655–658.
- (19) Rawn, C. J.; Rondinone, A. J.; Chakoumakos, B. C.; Circone, S.; Stern, L. A.; Kirby, S. H.; Ishii, Y. Can. J. Phys., 2003, 81, 431.
- (20) Circone, S.; Kirby, S. H.; Pinkston, J. C.; Stern, L. A. Rev. Sci. Instrum. 2001, 72, 2709.
- (21) Circone, S.; Stern, L. A.; Kirby, S. H.; Pinkston, J. C.; Durham, W. B. In *Gas Hydrates: Challenges for the Future*; Holder, G., Bishnoi, P., Eds.; New York Academy of Sciences: New York, 2000; pp 544–555.
- (22) Stern, L. A.; Circone, S.; Kirby, S. H.; Durham, W. B. Can. J. Phys. **2003**, 81, 271.
- (23) McMullan, R. K.; Jeffrey, G. A. *J. Chem. Phys.* **1965**, *42*, 2725. (24) Ikeda, T.; Mae, S.; Yamamuro, O.; Matsuo, T.; Ikeda, S.; Ibberson, R. M. *J. Phys. Chem. A* **2000**, *104*, 10623.
- (25) Hwang, M. J.; Wright, D. A.; Kapur, A.; Holder, G. D. J. Inclusion Phenom. Mol. Recognit. Chem. 1990, 8, 103.
- (26) Wang, X.; Schultz, A. J.; Halpern, Y. J. Phys. Chem. A 2002, 106, 7304
- (27) Moudrakovski, I. L.; Ratcliffe, C. I.; McLaurin, G. E.; Simard, B.; Ripmeester, J. A. *J. Phys. Chem. A* **1999**, *103*, 4969.