

Calculate the volume occupied by 50 kg of propane at 35 bar and 50 °C, using the following:

(a) The ideal gas model

$$PV = NRT = \frac{M}{MW}RT \quad (1 \text{ point for correct equation})$$

$$V = \frac{MRT}{P(MW)}$$

$$V = \frac{(50 \cdot 10^3 \text{ g})(0.08314 \frac{\text{Lbar}}{\text{molK}})(323\text{K})}{(35\text{bar})(44.10 \frac{\text{g}}{\text{mol}})}$$

$$V = 869.9 \text{ L}$$

(1 point)

(b) The Redlich-Kwong equation of state

$$P = \frac{RT}{v-b} - \frac{a}{T^{1/2}v(v+b)}$$

Where $a = \frac{0.42748R^2T_c^{2.5}}{P_c}$ and $b = \frac{0.08664RT_c}{P_c}$

From Appendix A,

$P_c = 42.44 \text{ bar}$, $T_c = 370.0\text{K}$

Calculating

$$a = \frac{0.42748(0.08314 \frac{L^2 \text{bar}}{\text{molK}})^2 (370.0\text{K})^{2.5}}{42.44 \text{bar}} = 183.34 \frac{L^2 \text{barK}^{1/2}}{\text{mol}^2}$$

$$b = \frac{0.08664(0.08314 \frac{L \text{bar}}{\text{molK}})(370.0\text{K})}{42.44 \text{bar}} = 0.0628 \frac{L}{\text{mol}}$$

Substitute values into RK EOS,

$$P = \frac{RT}{v-b} - \frac{a}{T^{1/2}v(v+b)}$$

$$35 \text{bar} = \frac{(0.08314 \text{bar})(323\text{K})}{v - 0.0628 \frac{L}{\text{mol}}} - \frac{183}{(323\text{K})^{1/2} v(v + 0.0628 \frac{L}{\text{mol}})}$$

Solving for v numerically,

$$v = 0.1093 \frac{L}{\text{mol}}$$

$$V = \frac{M}{MW} v$$

$$V = \frac{50000g}{44.10 \frac{g}{mol}} 0.1093 \frac{L}{mol}$$

$$V \Rightarrow 123.9L$$

(2 points)

The Peng-Robinson equation of state

$$P = \frac{RT}{v-b} - \frac{a\alpha(T)}{v(v+b)+b(v-b)}$$

Where $a = 0.45724 \frac{R^2 T_c^2}{P_c}$, $b = 0.07780 \frac{RT_c}{P_c}$

$$\alpha(T) = [1 + \kappa(1 - \sqrt{T_r})]^2, \quad \kappa = 0.37464 + 1.54226\omega - 0.26992\omega^2$$

From Appendix A,

$$P_c = 42.44 \text{ bar}, \quad T_c = 370.0\text{K}, \quad \omega = 0.152$$

Calculating

$$a = 0.45724 \frac{(0.08314 \frac{\text{Lbar}}{\text{molK}})^2 (370.0\text{K})^2}{42.44\text{bar}} = 10.195$$

$$b = 0.07780 \frac{(0.08314 \frac{\text{Lbar}}{\text{molK}})(370.0\text{K})}{42.44\text{bar}} = 0.0564$$

$$\kappa = 0.37464 + 1.54226(0.152) - 0.26992(0.152)^2 = 0.603$$

$$\alpha(T) = [1 + (0.603)(1 - \sqrt{\frac{323\text{K}}{370\text{K}}})]^2 = 1.081$$

Substitute values into PR EOS,

$$P = \frac{RT}{v-b} - \frac{a\alpha(T)}{v(v+b)+b(v-b)}$$

$$35\text{bar} = \frac{(0.08314 \frac{\text{Lbar}}{\text{molK}})(323\text{K})}{v - 0.0564 \frac{\text{L}}{\text{mol}}} - \frac{(10.195)(1.081)}{v(v + 0.0564 \frac{\text{L}}{\text{mol}}) + 0.0564 \frac{\text{L}}{\text{mol}}(v - 0.0564 \frac{\text{L}}{\text{mol}})}$$

Solving for v numerically,

$$v = 0.0942 \frac{L}{mol}$$

$$V = \frac{M}{MW} v$$

$$V = \frac{50000g}{44.10 \frac{g}{mol}} 0.0942 \frac{L}{mol}$$

$V = 106.8L$

(2 points)

(c) The compressibility charts

$$P_r = \frac{P}{P_c} = \frac{35 \text{ bar}}{42.44 \text{ bar}} = 0.825$$

$$T_r = \frac{T}{T_c} = \frac{323 \text{ K}}{370.0 \text{ K}} = 0.873$$

Using Tables C.1 and C.2 (by interpolation)

$$z^{(0)} = 0.1349$$

$$z^{(1)} = -0.0520$$

$$z = z^{(0)} + \omega z^{(1)}$$

$$z = 0.1349 + 0.152(-0.0520)$$

$$z = 0.127$$

(1 point)

$$V = nv = \left(\frac{M}{MW}\right)\left(\frac{zRT}{P}\right)$$

$$V = \left(\frac{50000 \text{ g}}{44.10 \frac{\text{g}}{\text{mol}}}\right)\left(\frac{0.127(0.08314 \frac{\text{Lbar}}{\text{molK}})(323 \text{ K})}{35 \text{ bar}}\right)$$

$$V \rightleftharpoons 10.5L$$

(1 point)

The textbook software, ThermoSolver: www.wiley.com/college/koretsky

Using Peng-Robinson Equation of State,

$$v = 0.0942 \frac{L}{mol}$$

$$V = \frac{50000g}{44.10 \frac{g}{mol}} 0.0942 \frac{L}{mol}$$

$$V \Rightarrow 406.8L$$

(1 point)

Using Compressibility Chart,

$$v = 0.0971 \frac{L}{mol}$$

$$V = \frac{50000g}{44.10 \frac{g}{mol}} 0.0971 \frac{L}{mol}$$

$$V \Rightarrow 410.1L$$

(1 point)