

Lawrence Livermore National Laboratory

Rate Constant Estimation for Large Chemical Kinetic Models  
and Application to Biofuels

ICCK 2001, MIT

July 28, 2011



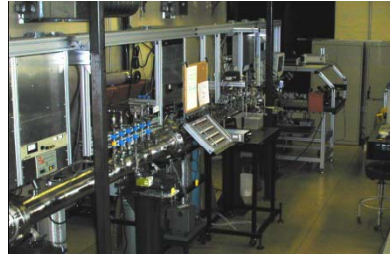
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Sarathy and Taku Tsujimura**  
**Lawrence Livermore National Laboratory**

Lawrence Livermore National Laboratory, P. O. Box 808, Livermore, CA 94551

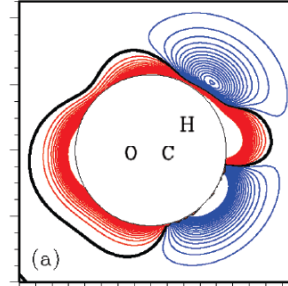
This work performed under the auspices of the U.S. Department of Energy by  
Lawrence Livermore National Laboratory under Contract DE-AC52-07NA27344

LLNL-PRES-490531

# Development of chemical kinetic models for fuels



Fundamental experimental measurements

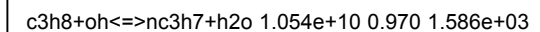


Ab initio calculations

oh	7/13/ 0	rucich	1o	1	0	0g	300.000	5000.000	1710.000	01
	2.85376040e+00	1.02994334e-03	-2.32666477e-07	1.93750704e-11	-3.15759847e-16					2
	3.69949720e+03	5.78756825e+00	3.41896226e+00	3.19255801e-04	-3.08292717e-07					3
	3.64407494e-10	-1.00195479e-13	3.45264448e+03	2.54433372e+00						4

C1C2 base chemistry

Thermodynamic database



Reaction rate constants

Detailed chemical kinetic model for practical fuels

Reaction rate rules

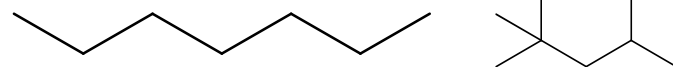
reactions
<chem>h+o2&lt;=&gt;o+oh</chem> 9.65E+14 -0.262 1.62E+04
<chem>o+h2&lt;=&gt;h+oh</chem> 5.080e+04 2.670 6.292e+03
<chem>oh+h2&lt;=&gt;h+h2o</chem> 2.160e+08 1.510 3.430e+03
<chem>o+h2o&lt;=&gt;oh+oh</chem> 2.970e+06 2.020 1.340e+04
<chem>h2+m&lt;=&gt;h+h+m</chem> 4.577e+19 -1.400 1.044e+05
h2/ 2.5/ h2o/ 12/ co/ 1.9/ co2/ 3.8/
<chem>o+o+m&lt;=&gt;o2+m</chem> 6.165e+15 -0.500 0.000e+00
h2/ 2.5/ h2o/ 12/ ar/ .83/ co/ 1.9/ co2/ 3.8/ ch4/ 2/ c2h6/ 3/ he/ .83/
<chem>o+h+m&lt;=&gt;oh+m</chem> 4.714e+18 -1.000 0.000e+00
h2/ 2.5/ h2o/ 12/ ar/ .75/ co/ 1.5/ co2/ 2/ ch4/ 2/ c2h6/ 3/ he/ .75/

- High temperature mechanism*
- Reaction class 1: Unimolecular fuel decomposition
  - Reaction class 2: H atom abstractions from fuel
  - Reaction class 3: Alkyl radical decomposition
  - Reaction class 4: Alkyl radical + O<sub>2</sub> = olefin + HO<sub>2</sub>
  - Reaction class 5: Alkyl radical isomerization
  - Reaction class 6: H atom abstraction from olefins
  - Reaction class 7: Addition of radical species to olefins
  - Reaction class 8: Alkenyl radical decomposition
  - Reaction class 9: Olefin decomposition

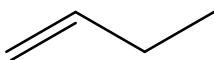


# Need reaction rate rules for many chemical classes of fuels

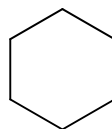
■ Alkanes



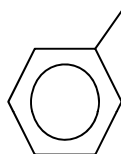
■ Alkenes



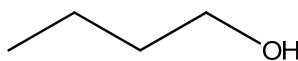
■ Cycloalkanes



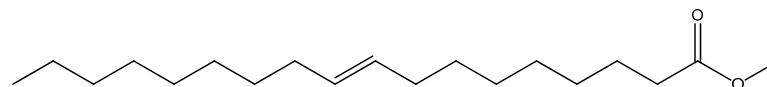
■ Aromatics



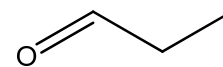
■ Alcohols



■ Methyl esters (biodiesel compounds)

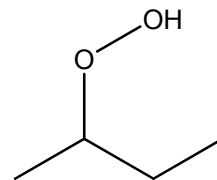


■ Carbenes (aldehydes, ketenes)

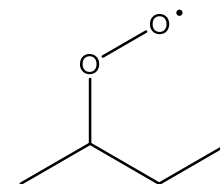


■ Special structures in intermediate species:

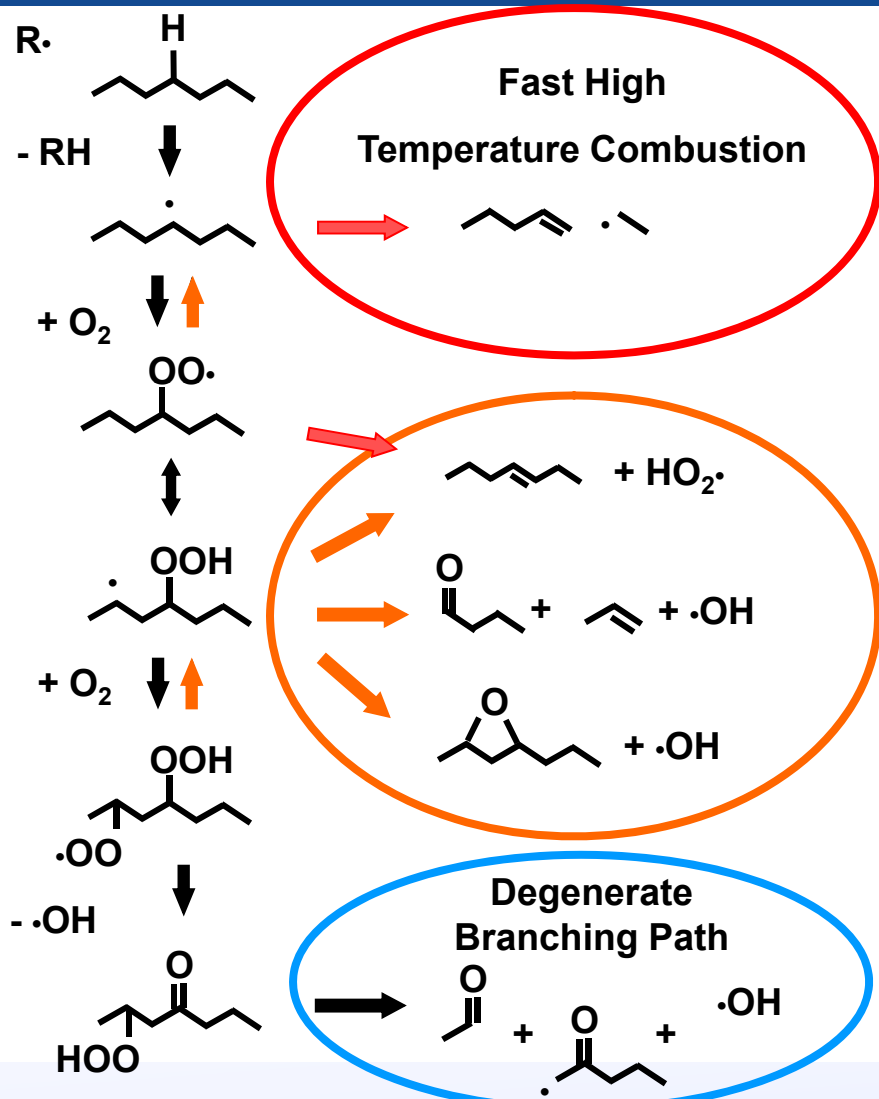
• Alkylhydroperoxides



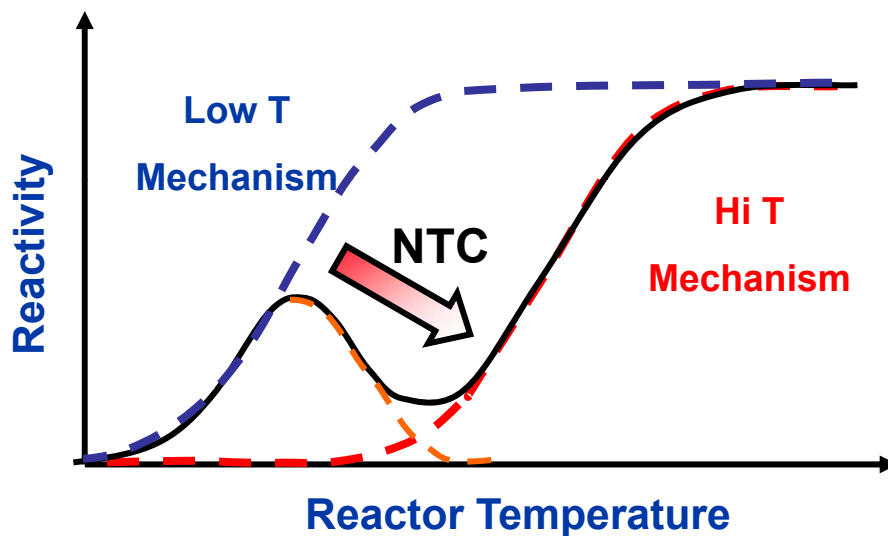
• Alkylperoxy



# Need reaction rate rules for many types of reaction steps



## Long Chain Alkanes



# Assign reaction rate rules by reaction classes

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## High temperature mechanism

Reaction class 1: Unimolecular fuel decomposition

Reaction class 2: H atom abstractions from fuel

Reaction class 3: Alkyl radical decomposition

Reaction class 4: Alkyl radical + O<sub>2</sub> = olefin + HO<sub>2</sub>

Reaction class 5: Alkyl radical isomerization

Reaction class 6: H atom abstraction from olefins

Reaction class 7: Addition of radical species to olefins

Reaction class 8: Alkenyl radical decomposition

Reaction class 9: Olefin decomposition



# Reaction classes for low temperature reactions

## Low temperature mechanism

Reaction class 10: Alkyl radical addition to  $O_2$  ( $R + O_2$ )

Reaction class 11:  $R + R'O_2 = RO + R'O$

Reaction class 12: Alkylperoxy radical isomerization

Reaction class 13:  $RO_2 + HO_2 = ROOH + O_2$

Reaction class 14:  $RO_2 + H_2O_2 = ROOH + HO_2$

Reaction class 15:  $RO_2 + CH_3O_2 = RO + CH_3O + O_2$

Reaction class 16:  $RO_2 + R'O_2 = RO + R'O + O_2$

Reaction class 17:  $ROOH = RO + OH$

Reaction class 18: RO Decomposition

Reaction class 19:  $QOOH = \text{Cyclic Ether} + OH$

Reaction class 20:  $QOOH = \text{Olefin} + HO_2$

Reaction class 21:  $QOOH = \text{Olefin} + \text{Aldehyde or Carbonyl} + OH$

Reaction class 22: Addition of  $QOOH$  to molecular oxygen  $O_2$

Reaction class 23:  $O_2QOOH$  isomerization to carbonylhydroperoxide + OH

Reaction class 24: Carbonylhydroperoxide decomposition

Reaction class 25: Reactions of cyclic ethers with OH and  $HO_2$



# Reaction rate rules make the assignment of reaction rate constants manageable

Class 2



H- atom abstraction rate rules for alkanes

	C-H type	A (cm <sup>3</sup> mol <sup>-1</sup> s <sup>-1</sup> )	n	E <sub>A</sub> (cal)
H	1°	2.22E+05	2.54	6,756
	2°	6.50E+05	2.40	4,471
	3°	6.02E+05	2.40	2,583
OH	1°	1.76E+09	0.97	1,586
	2°	2.34E+07	1.61	-35
	3°	5.73E+10	0.51	63
CH <sub>3</sub>	1°	1.51E-01	3.65	7,154
	2°	7.55E-01	3.46	5,481
	3°	6.01E-10	6.36	893
HO <sub>2</sub>	1°	6.80E+00	3.59	17,160
	2°	3.16E+01	3.37	13,720
	3°	6.50E+02	3.01	12,090



# Reaction rate rule issues: fuel decomposition reactions

## Alkanes

- Set by reverse reaction
  - Exothermic direction
  - C-C bond breaking most important
  - Some variations in forward rate constants, even though you think they should be all the same



	Fwd				Rate at T	rev		
	A fwd	n fwd	AT <sup>n</sup>	EA fwd	1300 K	A rev	n rev	EA rev
	cm <sup>3</sup> -mol-s units			cal/mole		cm <sup>3</sup> -mol-s units		cal/mole
C3H8=C2H5+CH3	1.77E+23	-1.889	2.32E+17	9.04E+04	145	1.00E+13	0	0.0
C4H10=CH3+NC3H7	1.59E+23	-1.848	2.80E+17	9.03E+04	184	1.00E+13	0	0.0
c4h10=c2h5+c2h5	6.73E+24	-2.297	4.73E+17	8.93E+04	456	8.00E+12	0	0.0
NC10H22=C7H15-1+NC3H7	4.78E+24	-2.206	6.47E+17	8.89E+04	745	8.00E+12	0	0.0
NC10H22=C6H13-1+PC4H9	7.54E+24	-2.3	5.18E+17	8.88E+04	613	8.00E+12	0	0.0
NC10H22=C5H11-1+C5H11-1	9.81E+23	-2.023	4.92E+17	8.86E+04	622	8.00E+12	0	0.0





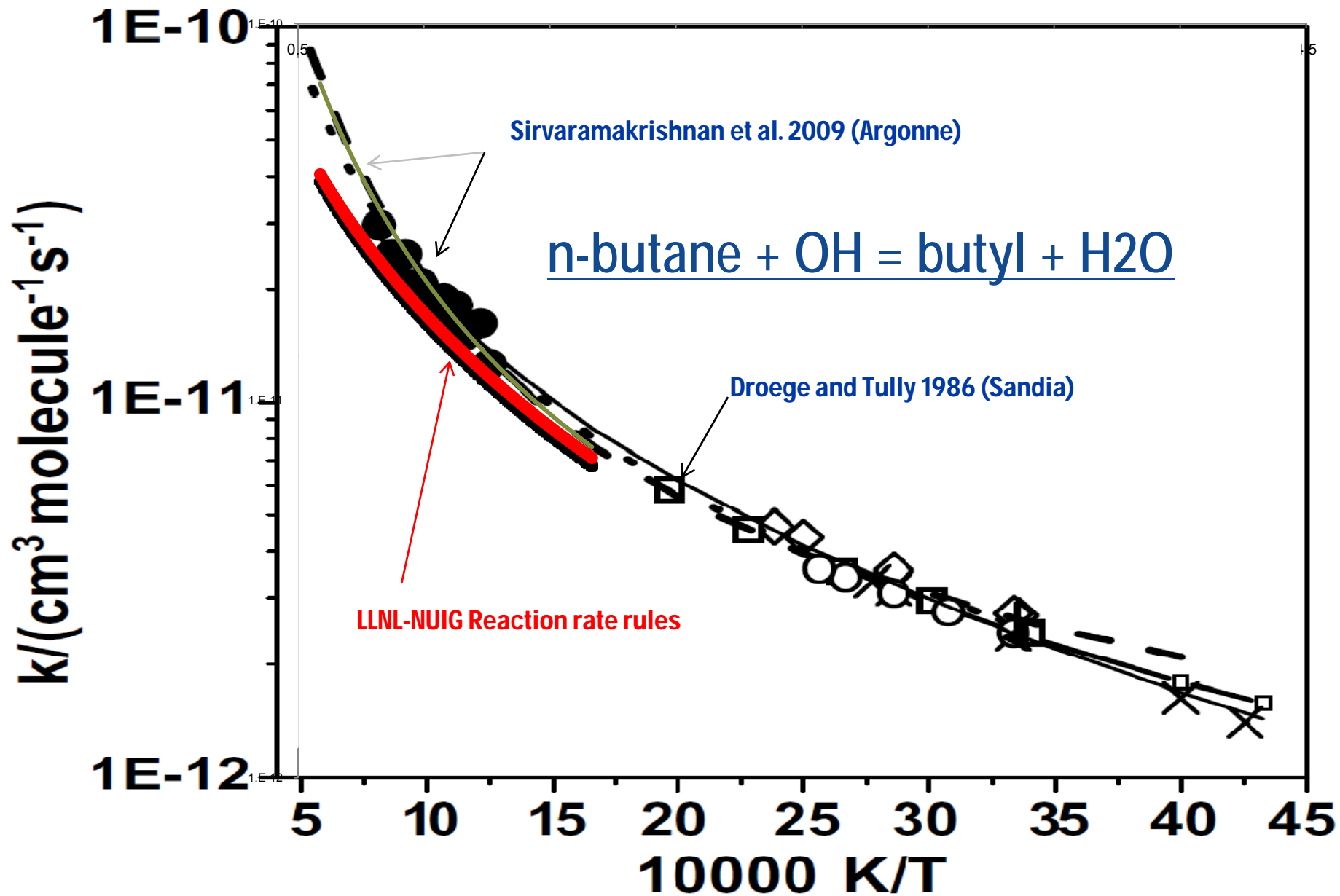
# Reaction rate rules for H-atom abstraction from alkanes



	C-H type	A (cm <sup>3</sup> mol <sup>-1</sup> s <sup>-1</sup> )	n	E <sub>A</sub> (cal)
H	1°	2.22E+05	2.54	6,756
	2°	6.50e+05	2.40	4,471
	3°	6.02E+05	2.40	2,583
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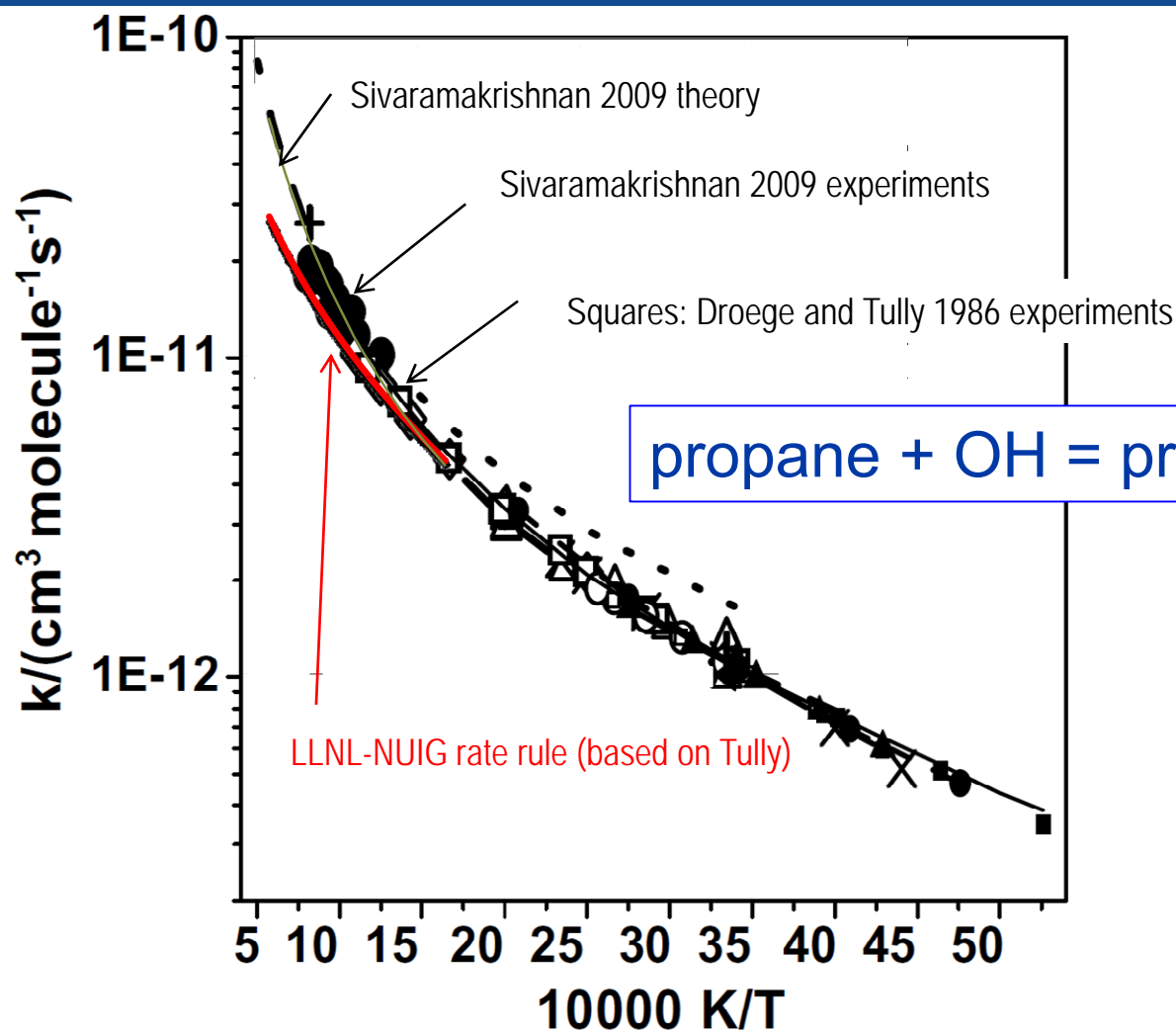


# New Argonne data for OH + alkanes

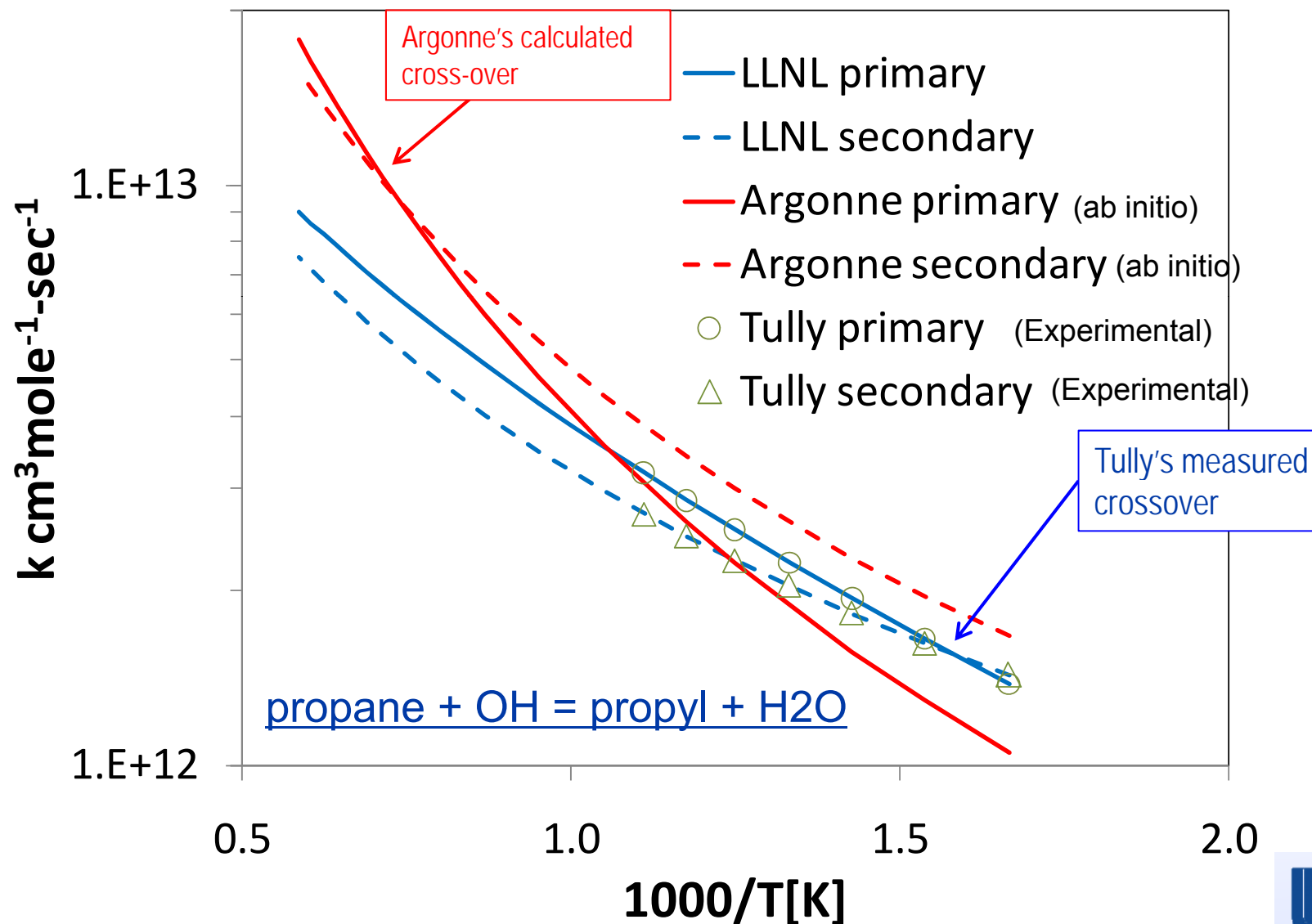


# New measured and calculated rate constants for OH + alkanes are higher at $T > 900\text{K}$

Class 2



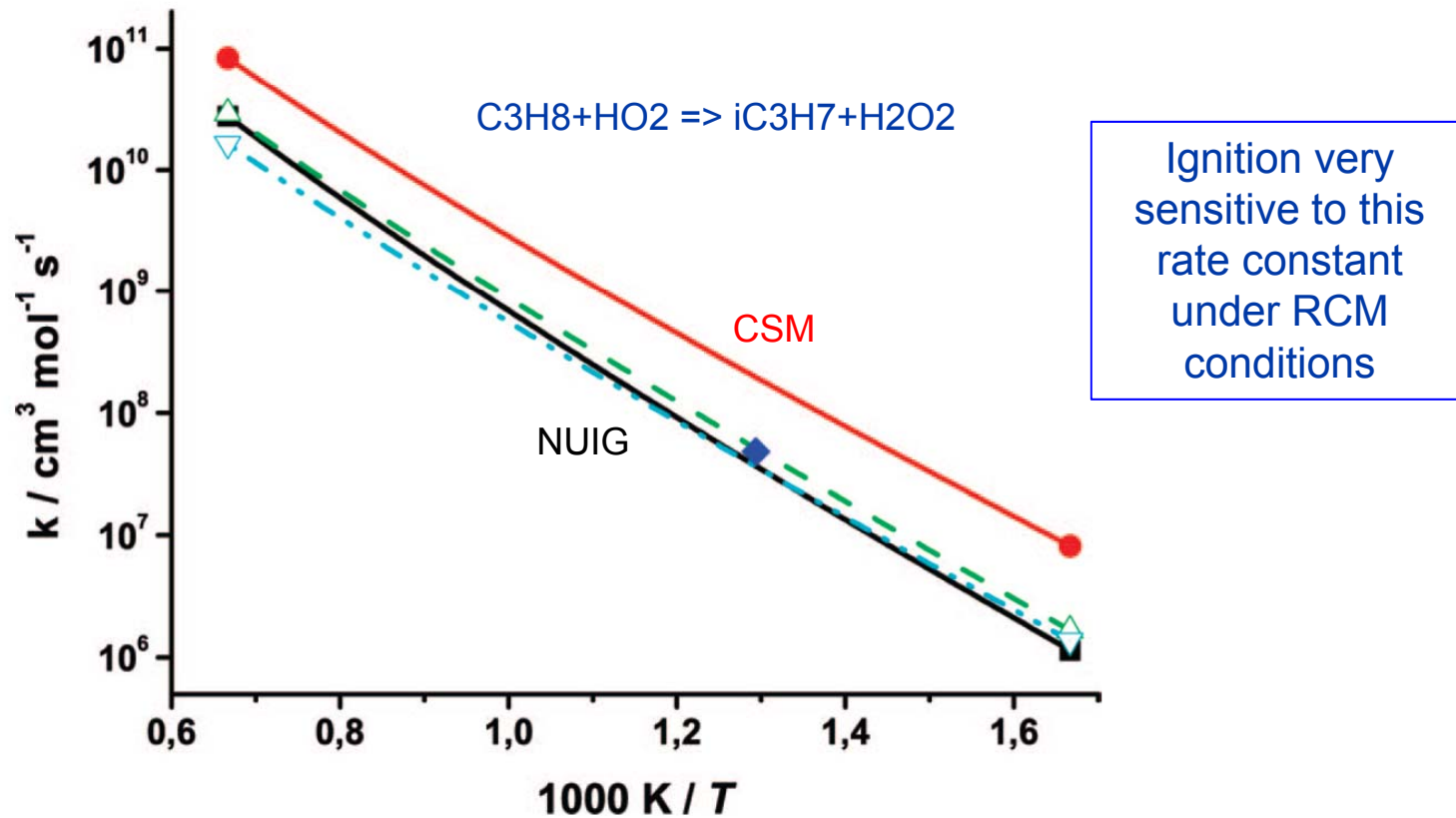
# Ab initio calculations show higher rates due to higher primary rate



# H-atom abstraction from the fuel: HO<sub>2</sub> + alkanes

## Uncertainty in rate of a factor of 3 - 6

Class 2

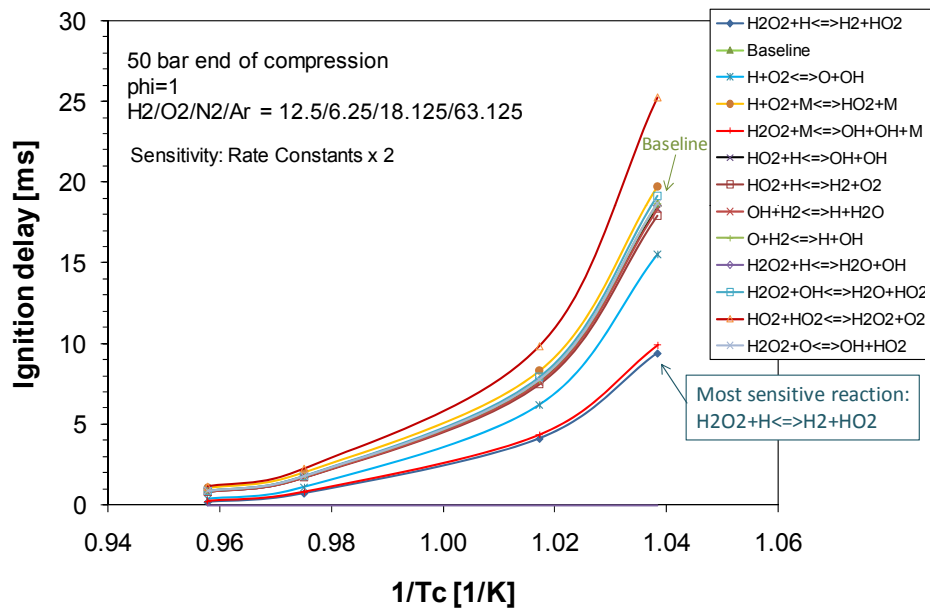


**Figure 6.**  $k(\text{C}_3\text{H}_8 + \text{HO}_2 \rightarrow i\text{-C}_3\text{H}_7 + \text{H}_2\text{O}_2)$ . This work (—■—), Carstensen<sup>18</sup> (—●—), Scott<sup>8</sup> (--Δ--), Orme<sup>14</sup> (-••▽-••), Baldwin<sup>11</sup> (◆).

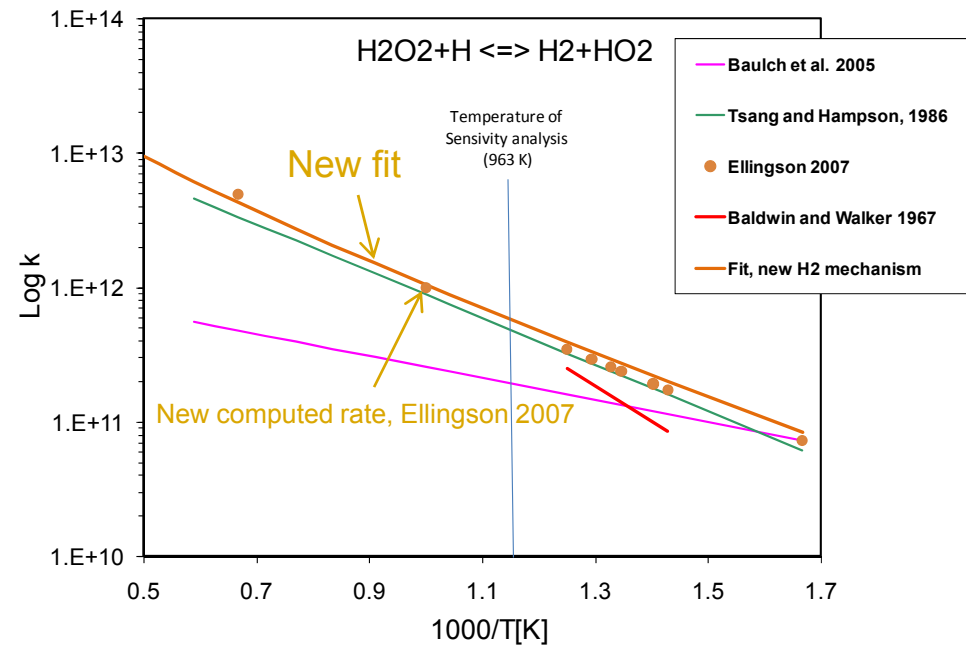


# Fuel + HO<sub>2</sub> shows high sensitivity when the fuel is hydrogen

Sensitivity results under conditions in rapid compression machine:



New rate constant fit:

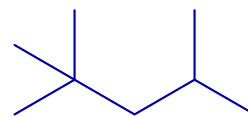


Important branching sequence at high pressure:  
 $\text{H}_2 + \text{HO}_2 \Rightarrow \text{H} + \text{H}_2\text{O}_2$   
 $\text{H}_2\text{O}_2 \Rightarrow \text{OH} + \text{OH}$   
 Retarding reaction:  
 $\text{HO}_2 + \text{HO}_2 \Rightarrow \text{H}_2\text{O}_2 + \text{O}_2$

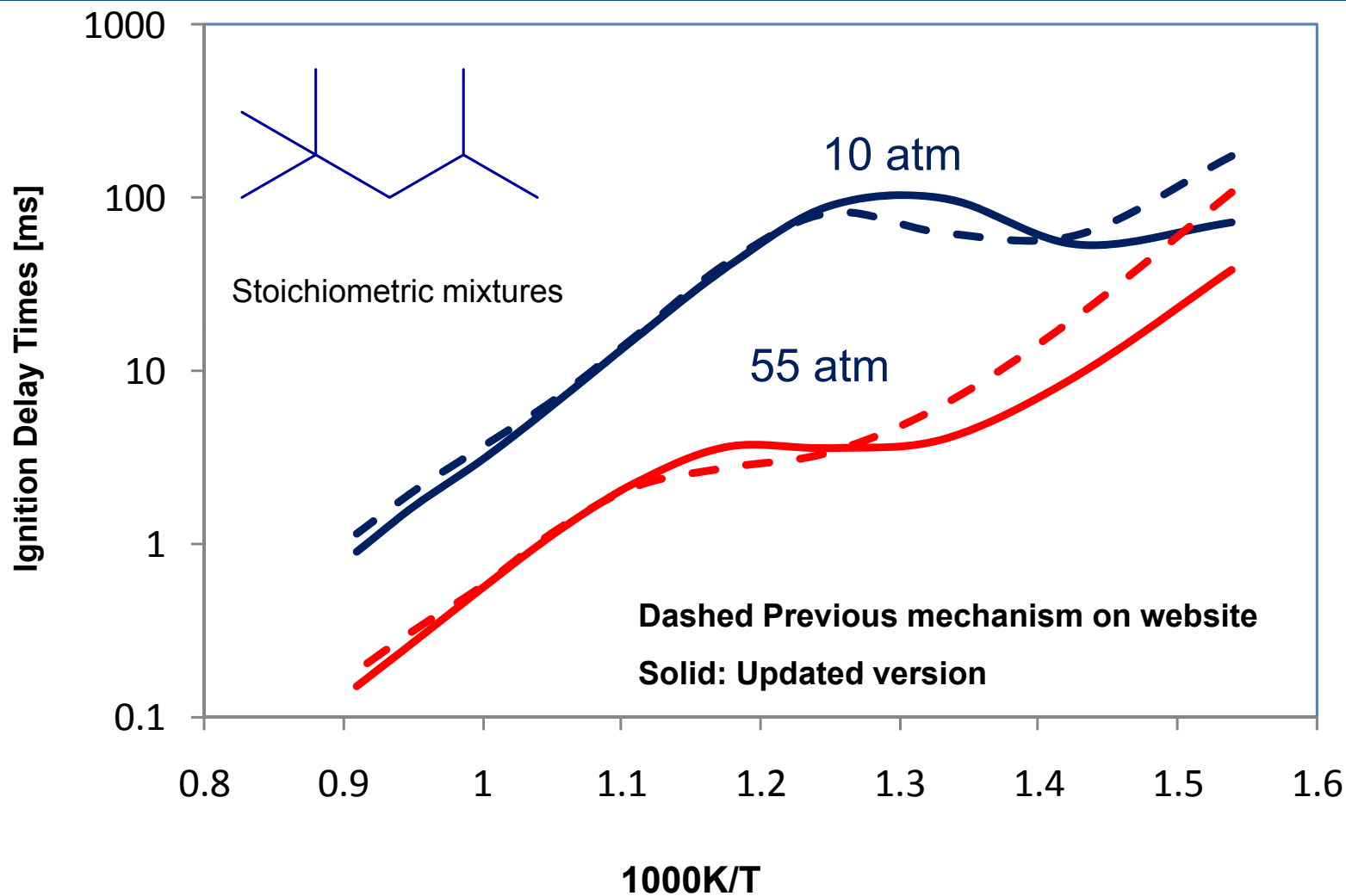


# Class 3: alkyl radical decomposition.

## Improvements for iso-octane



Class 3







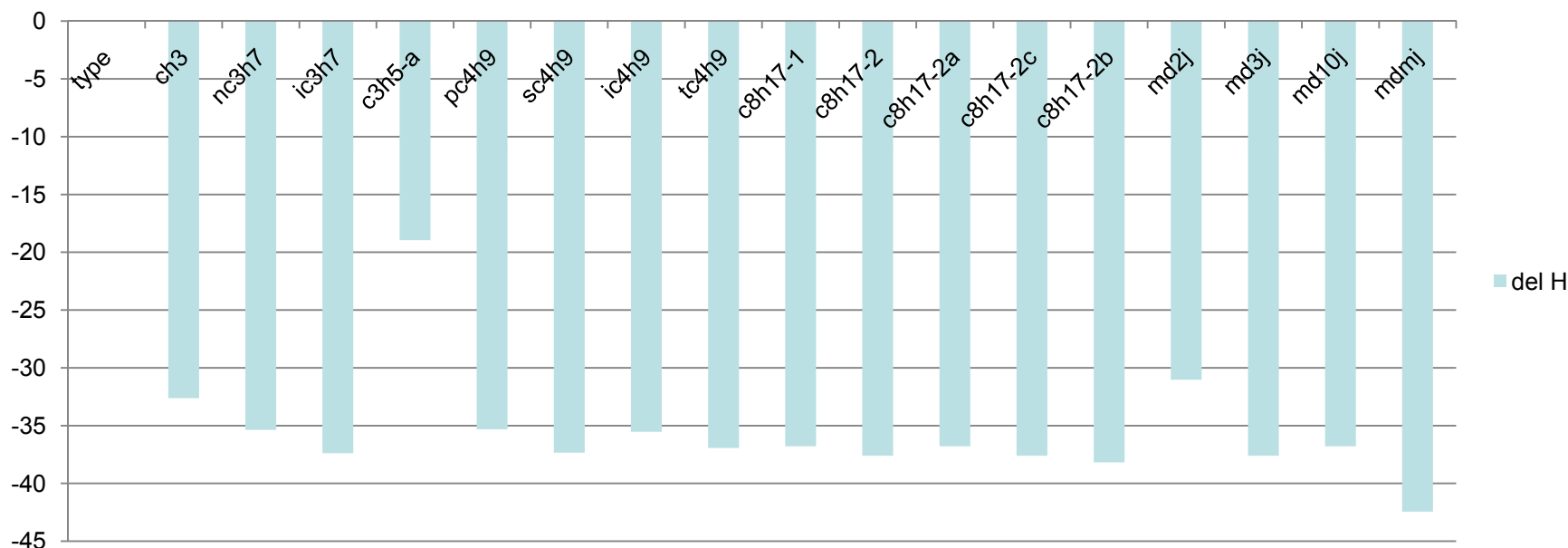
## Low temperature reactions:

Effect of R-O2 bond strength varies with bond type and controls amount of low temperature chemistry

Class 10  
R+O2 ⇌ RO2

Values used in LLNL models

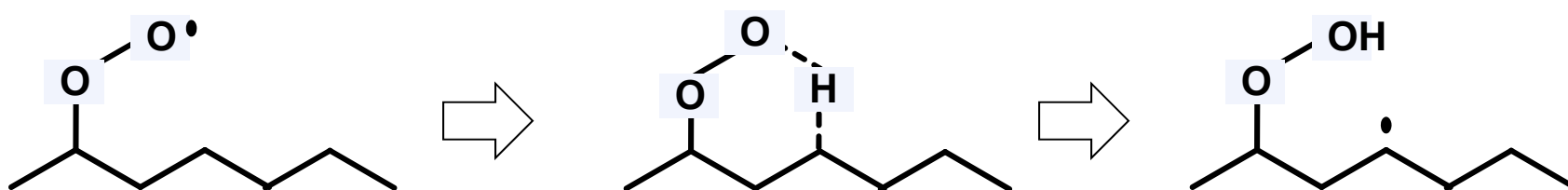
### Bond dissociation energy ( $\Delta H_{298}$ ) : R-OO => R + O2



# Low temperature chemistry: ROO → QOOH isomerizations

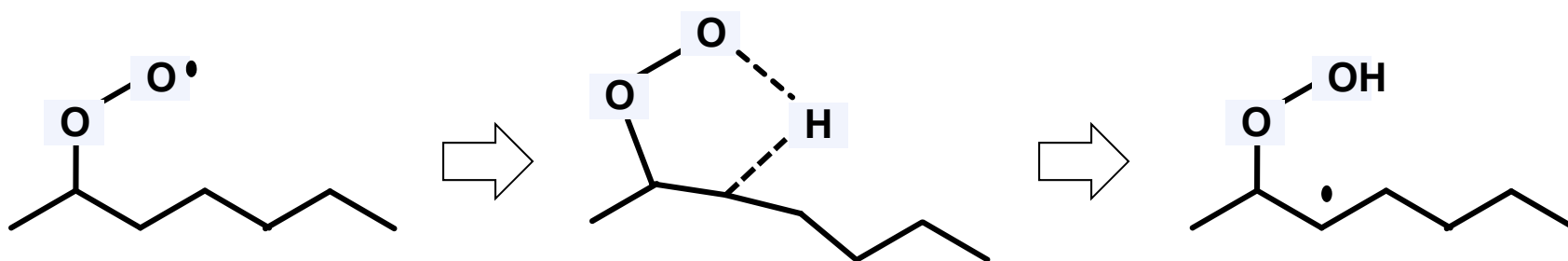
Class 12

## 6 Member ring isomerization



$$K_6 = 2.5E+10 \cdot \exp(-20450/RT)$$

## 5 Member ring isomerization

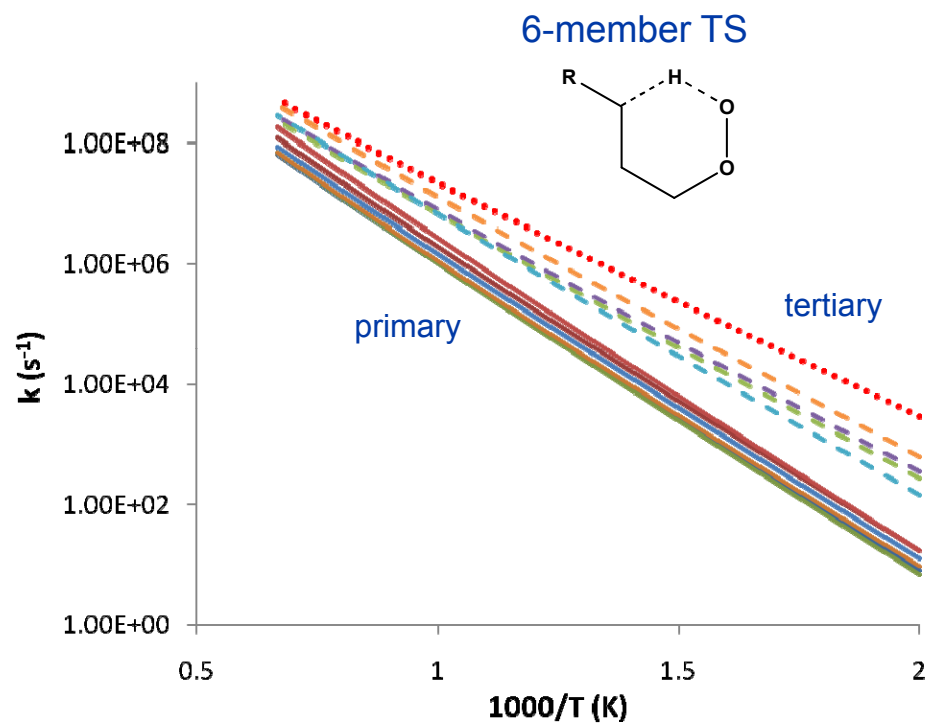
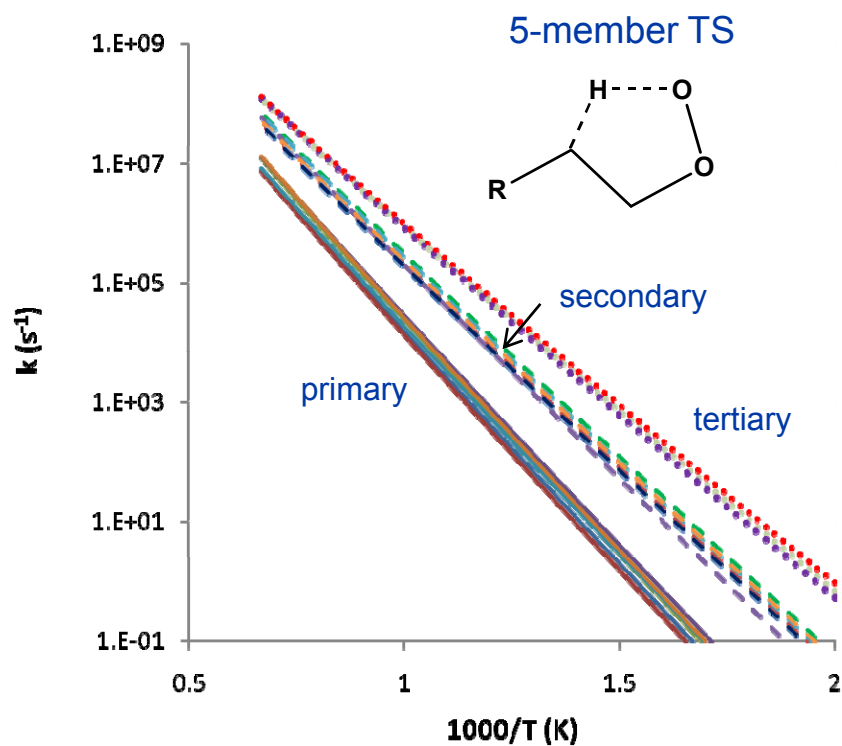


$$K_5 = 2.0E+11 \cdot \exp(-26450/RT)$$



# RO<sub>2</sub> isomerizations: Rate constants from computational chemistry (Dean, Carstensen et al. Colorado School of Mines)

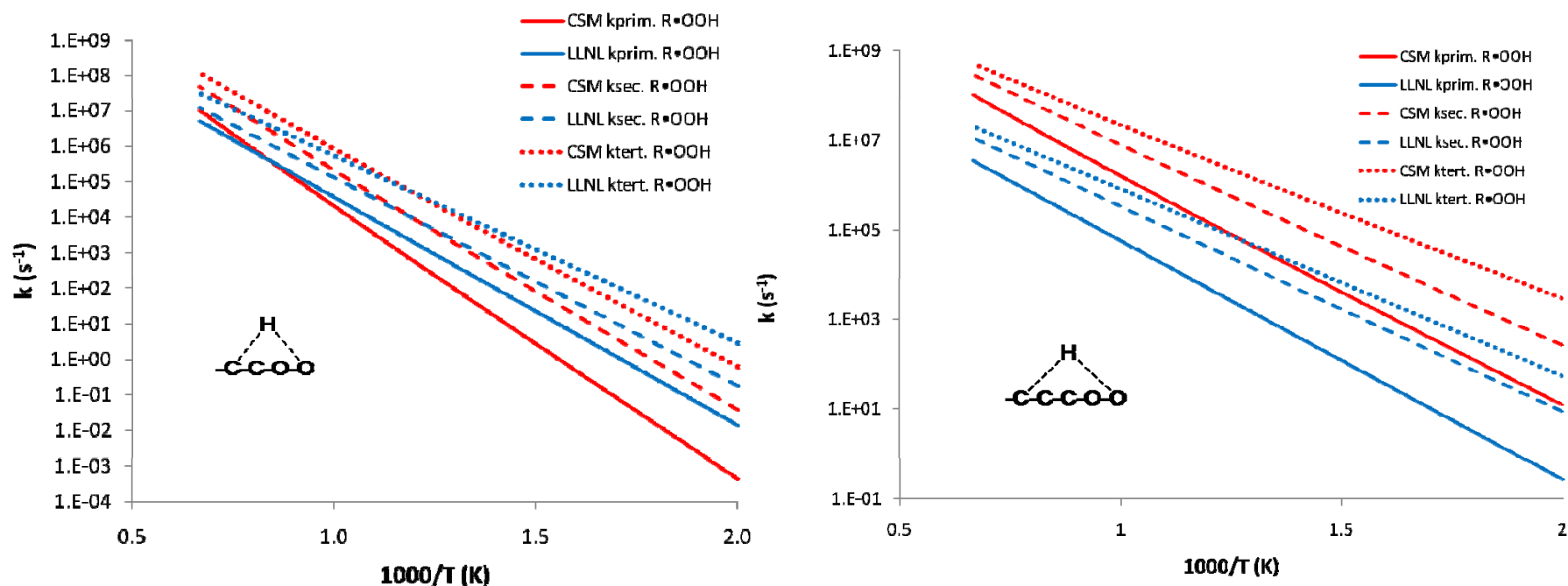
Class 12



- Activation energy depends on ring size *and* overall thermochemistry
- Amenable to rule generation

# Significant differences in CSM vs. LLNL rate constants: RO2 isomerization

Class 12

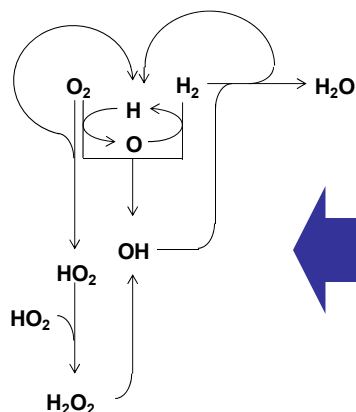


- CBS-QB3 results generally lower than LLNL values for 5-member TS
- CBS-QB3 results much higher than LLNL values for 6-member TS
  - Mainly due to higher A-factors (much higher than alkyl isomerizations)
- Differences lead to significantly different reaction pathways

# Mechanisms for fuels are built in a hierarchical manner and increase rapidly in size with fuel size

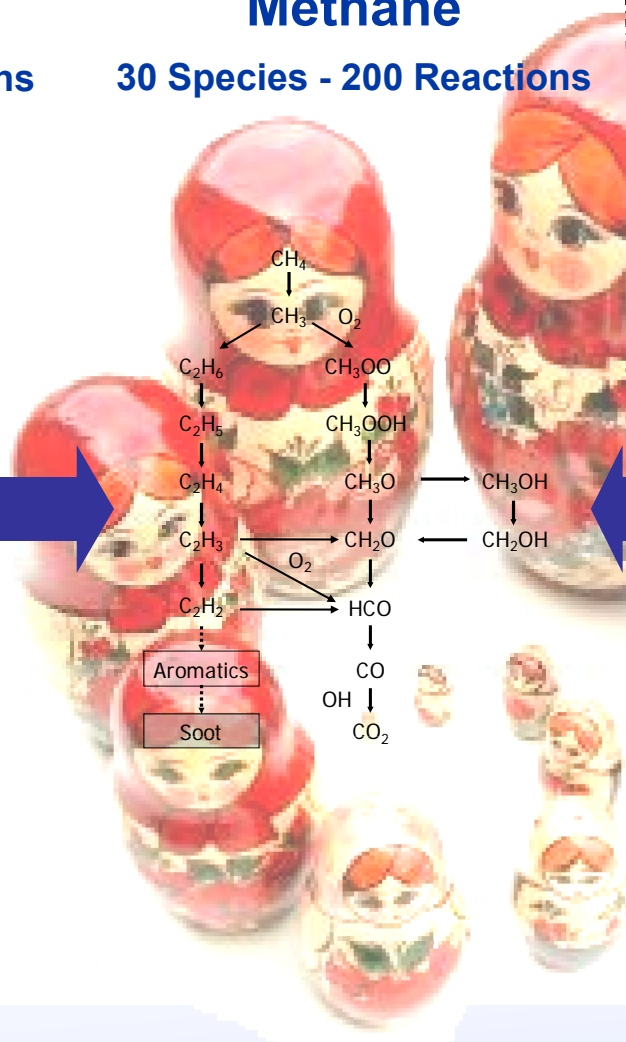
## Hydrogen

8 Species - 20 Reactions



## Methane

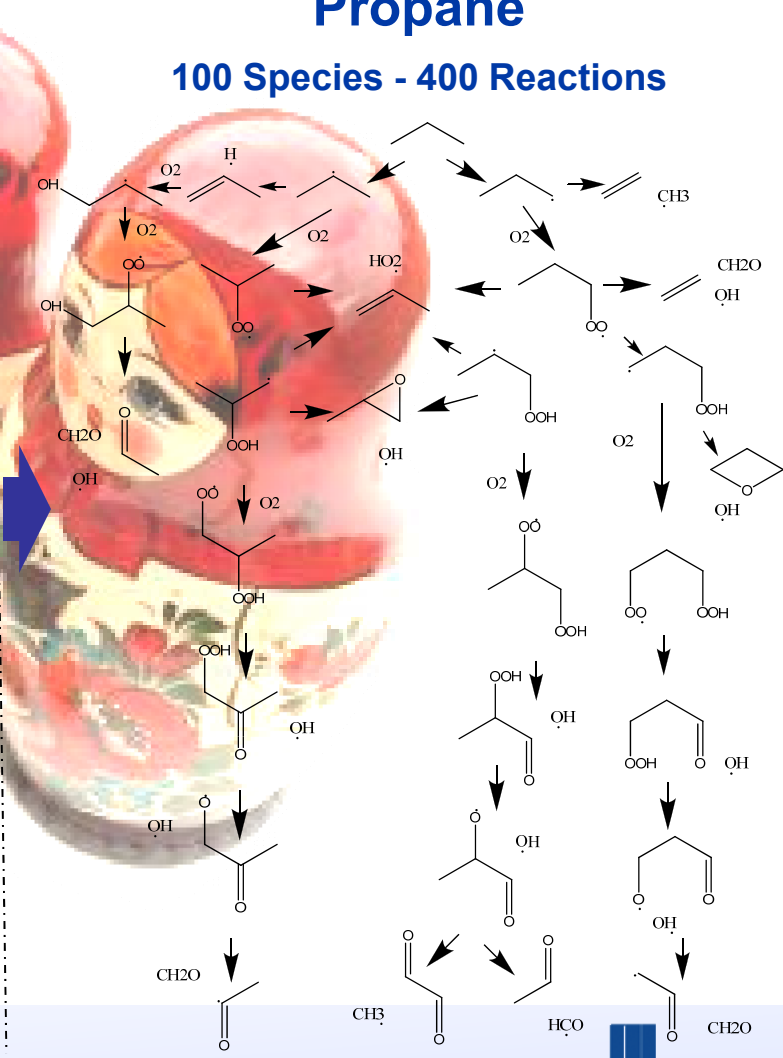
30 Species - 200 Reactions



C2 Chemistry

## Propane

100 Species - 400 Reactions



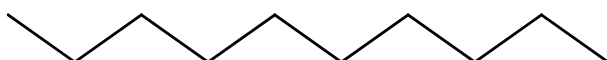
# Fuels Size and Mechanism Size

**n-Alkane**

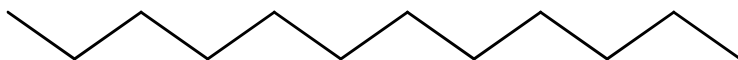
**C<sub>8</sub>H<sub>18</sub>**



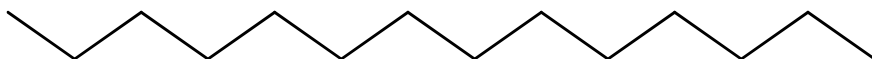
**C<sub>10</sub>H<sub>22</sub>**



**C<sub>12</sub>H<sub>26</sub>**



**C<sub>14</sub>H<sub>30</sub>**



**C<sub>16</sub>H<sub>34</sub>**



**Mechanism Size  
(Detailed Mechanism)**

**700 Species**

**3150 Reactions**

**950 Species**

**4050 Reactions**

**1250 Species**

**5150 Reactions**

**1650 Species**

**5150 Reactions**

**2100 Species**

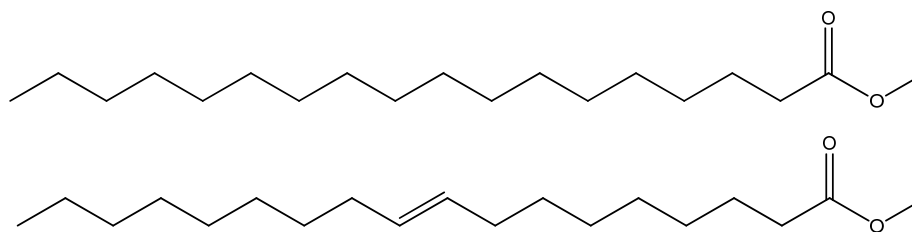
**8150 Reactions**



# Application of rules to biofuels

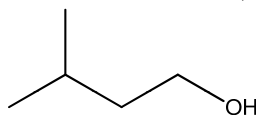
- Biodiesel

- Large methyl esters

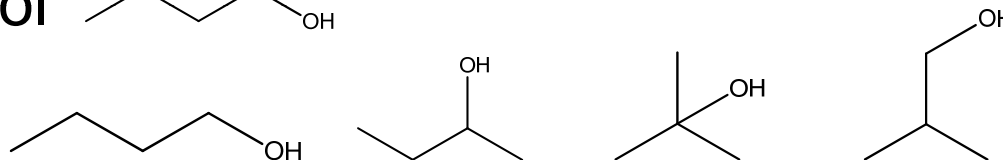


- Alcohols

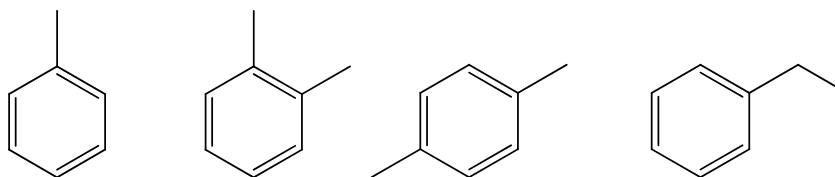
- Iso-pentanol



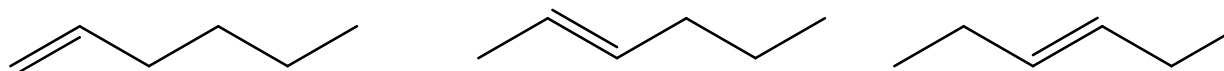
- Butanol



- Aromatics



- Olefins



# Biofuels

- Biodiesel
- New types of biofuels
  - Biomass
  - derived from algae and other single cell organisms



rapeseed



Algal pilot scale  
bioreactor in  
Lawrence, Kansas

From: Smith, Sturm, deNoyelles and Billings, Trends Ecol. Evol. (2010)





# Algal oil-derived fuels contain additional esters

Approximate weight percent of fatty acids in various vegetable and algal oil feedstocks [15,19, present work]. The nomenclature C<sub>x</sub>:<sub>y</sub> denotes the length of the hydrocarbon chain (x) and the number of double bonds in the hydrocarbon chain (y) of the fatty acid.

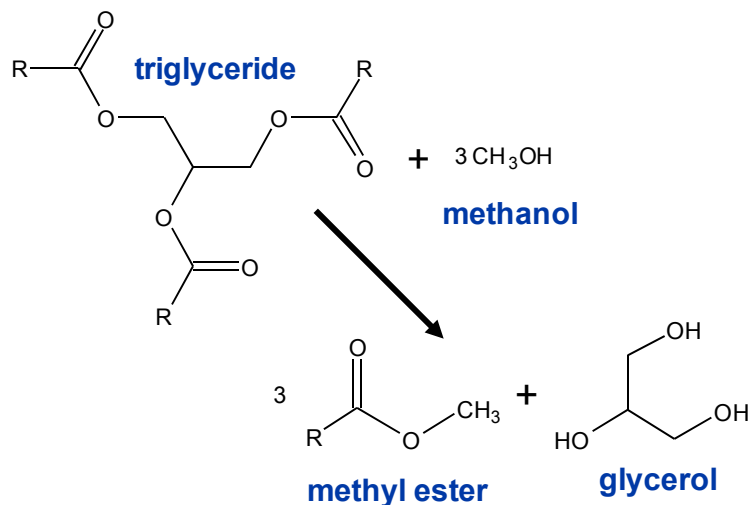
Feedstock	C8:0	C10:0	C12:0	C14:0	C16:0	C16:1	C18:0	C18:1	C18:2	C18:3	C20:0	C20:4	C20:5	C22:6
Soy					10		4	24	54	8				
Canola					5		2	64	20	8				
Coconut	9	6	49	17	8		2	5	2					
Palm				1	42		5	41	10					
Jatropha					11		17	13	47		5			
<i>Nannoch. Oculata</i>				4	29	24	9	4	1	1		5	22	
<i>Iso. Galbana</i>				13	36	32	1	4	4				7	3

Table 1 also includes the fatty acid composition for two algal oils: *Nannochloropsis Oculata* and *Isochrysis Galbana 3*. The former algae species is currently under consideration for wide scale production and its fatty acid composition was measured from algal oil samples provided by Solix Biofuels [18].

From: Marchese and B. Fisher, "Measurement of Gaseous and Particulate Emissions from Algae-Based Fatty Acid Methyl Esters," SAE 2010-01-1523.

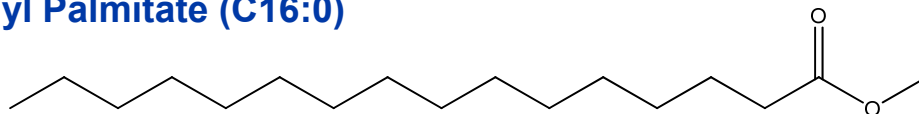


# Soybean and rapeseed derived biodiesels have only 5 principal components

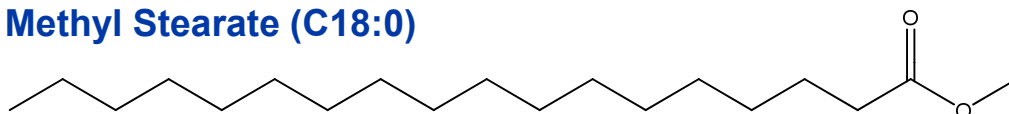


## Fatty acid methyl esters (FAMES):

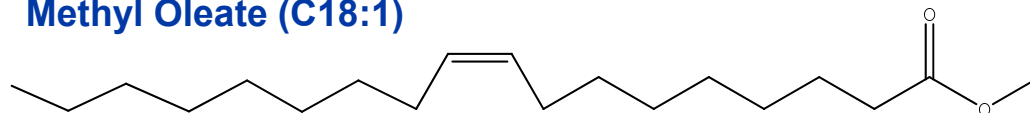
### Methyl Palmitate (C16:0)



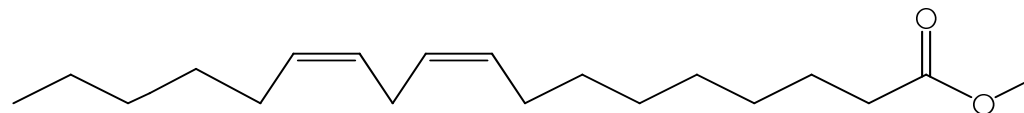
### Methyl Stearate (C18:0)



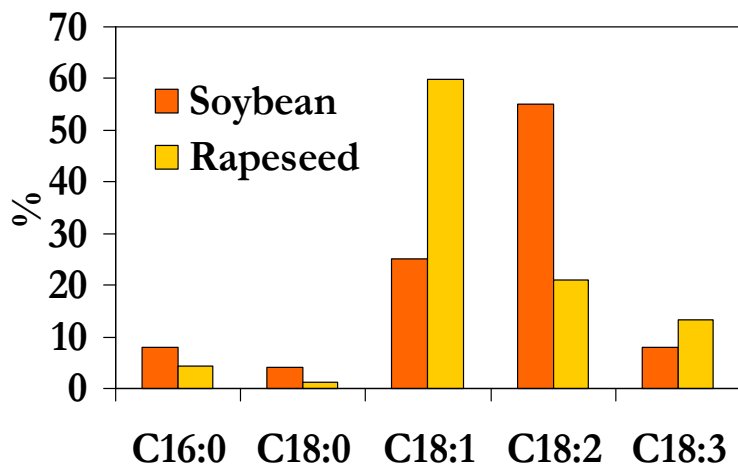
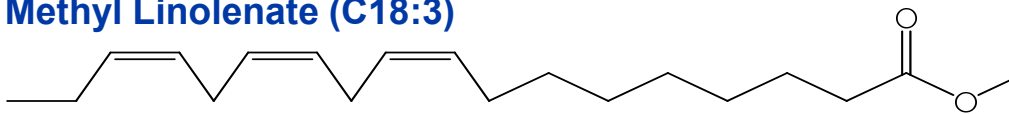
### Methyl Oleate (C18:1)



### Methyl Linoleate (C18:2)

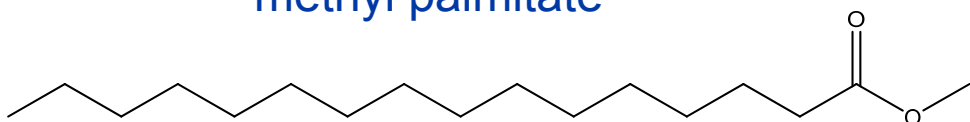


### Methyl Linolenate (C18:3)

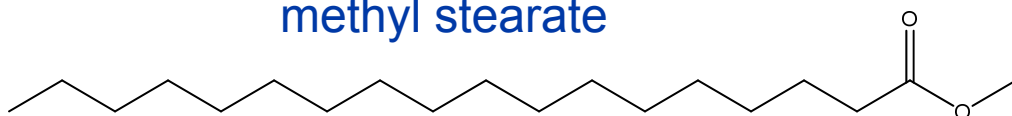


# Assembled chemical kinetic model for all of the five main components in biodiesel derived from soybeans or rapeseed oil

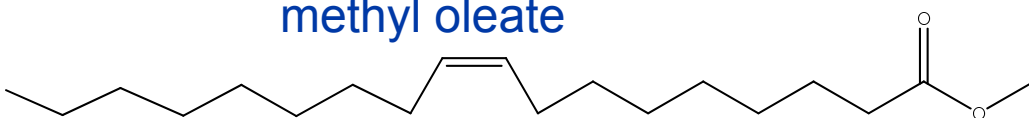
methyl palmitate



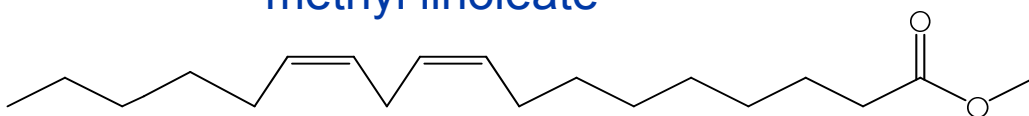
methyl stearate



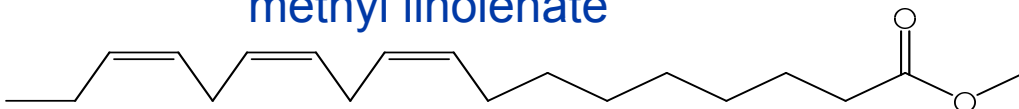
methyl oleate



methyl linoleate



methyl linolenate



Built with the same reaction rate rules as our successful methyl decanoate and methyl decenoate mechanism

5 component mechanism, approximately

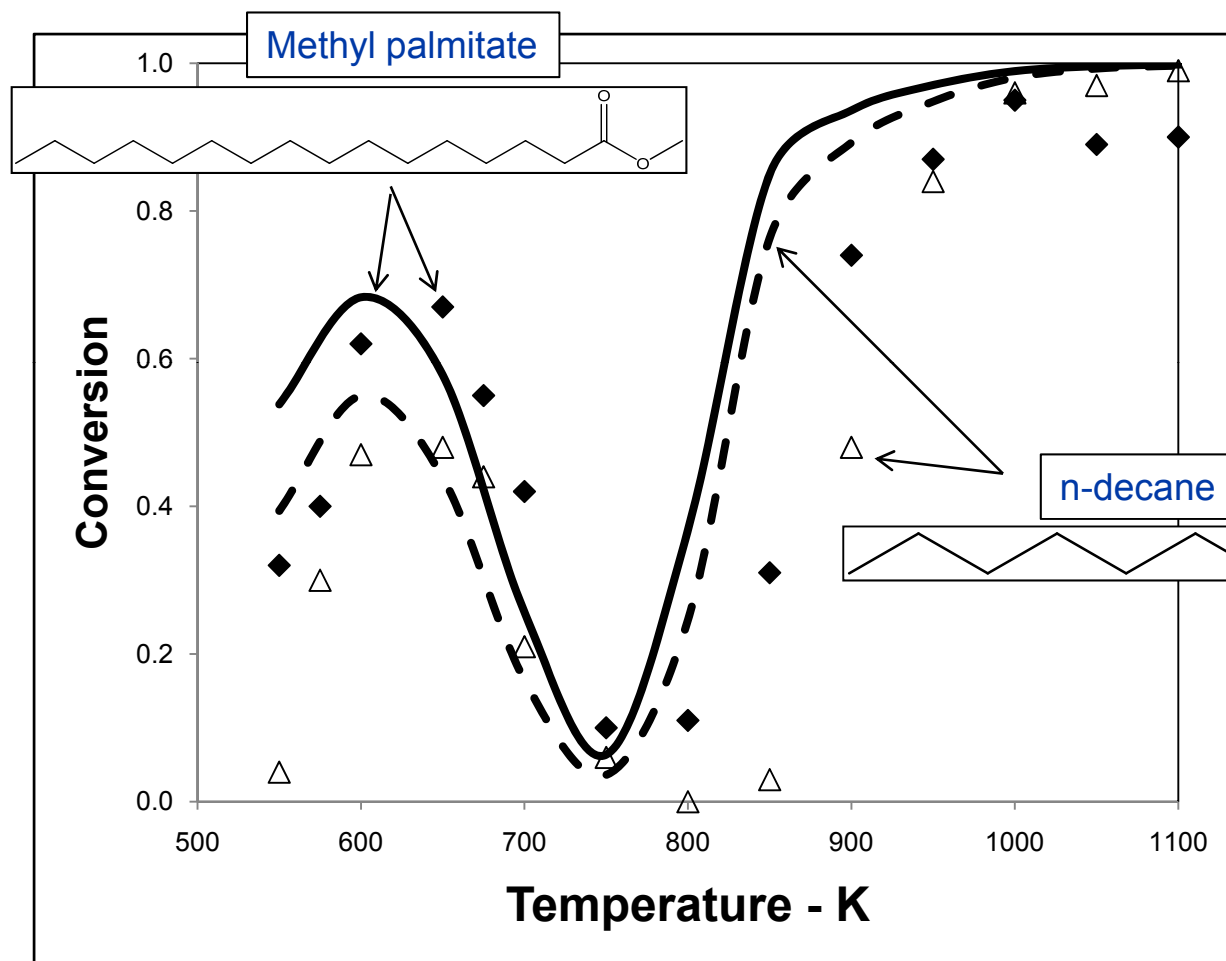
5,000 species  
20,000 reactions

Model with all 5 components now published and available:

Westbrook, Naik, Herbinet, Pitz, Mehl, Sarathy and Curran, "Detailed chemical kinetic reaction mechanisms for soy and rapeseed biodiesel fuels," Combustion and Flame, 2011.



# Experimental validation: New biodiesel model reproduces oxidation of n-decane/methyl palmitate mixture in jet stirred reactor

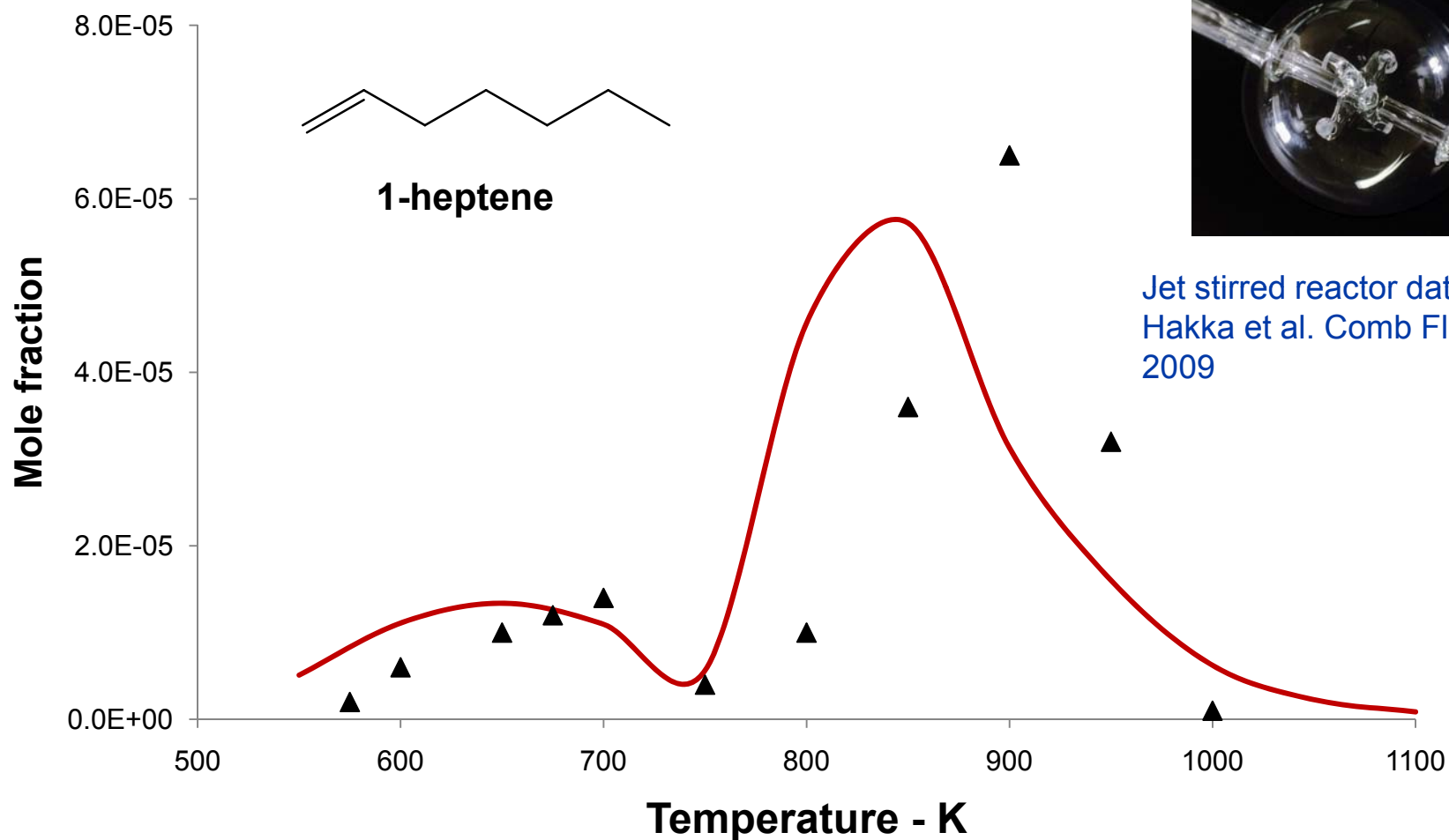


Stoichiometric fuel/O<sub>2</sub>/He mixtures  
1 atm  
1.5 s residence time

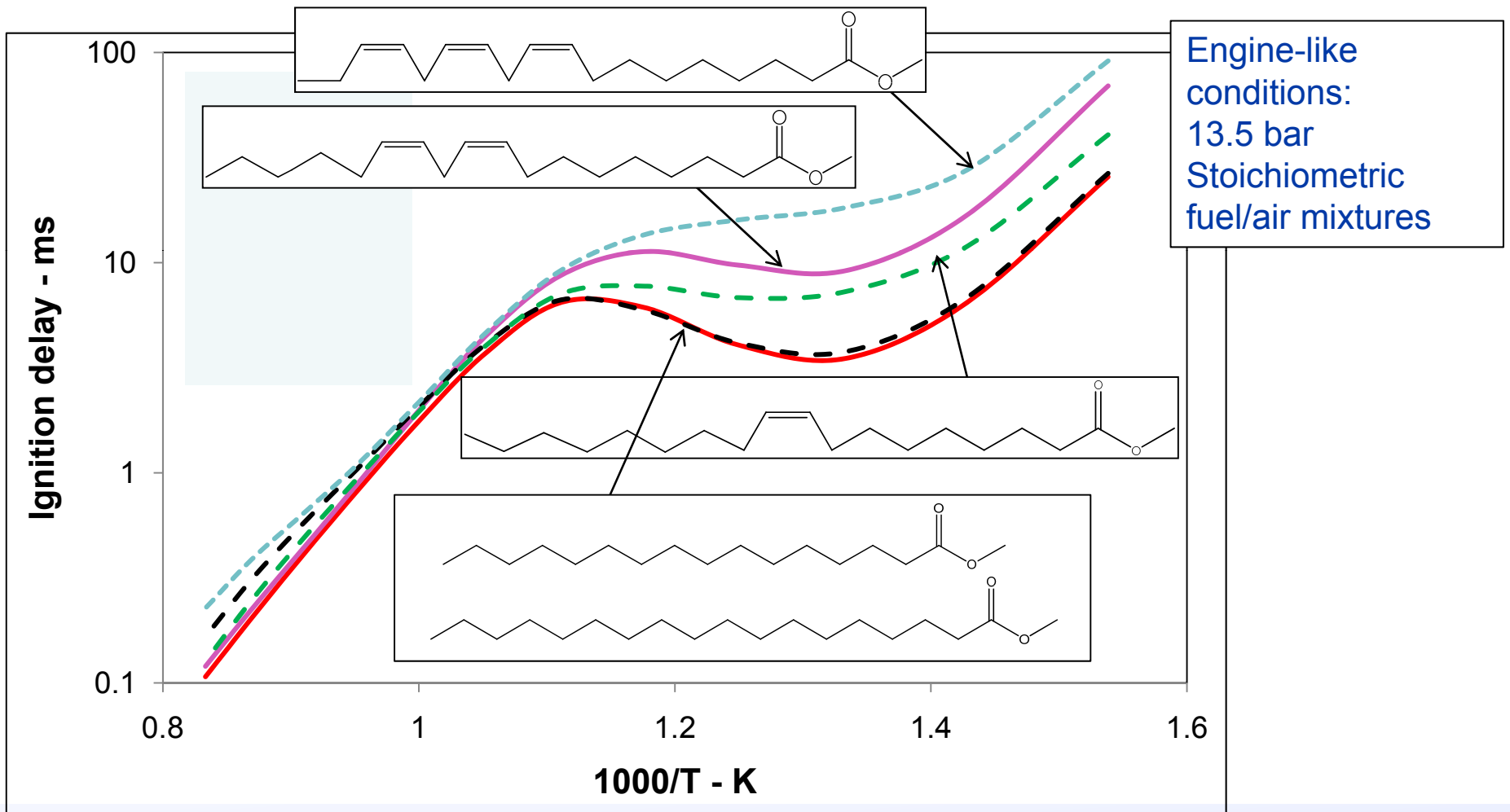
Jet stirred reactor data:  
Hakka et al. Comb Flame  
2009



# Many of the predicted species profiles compare well with experiments: e.g. 1-heptene

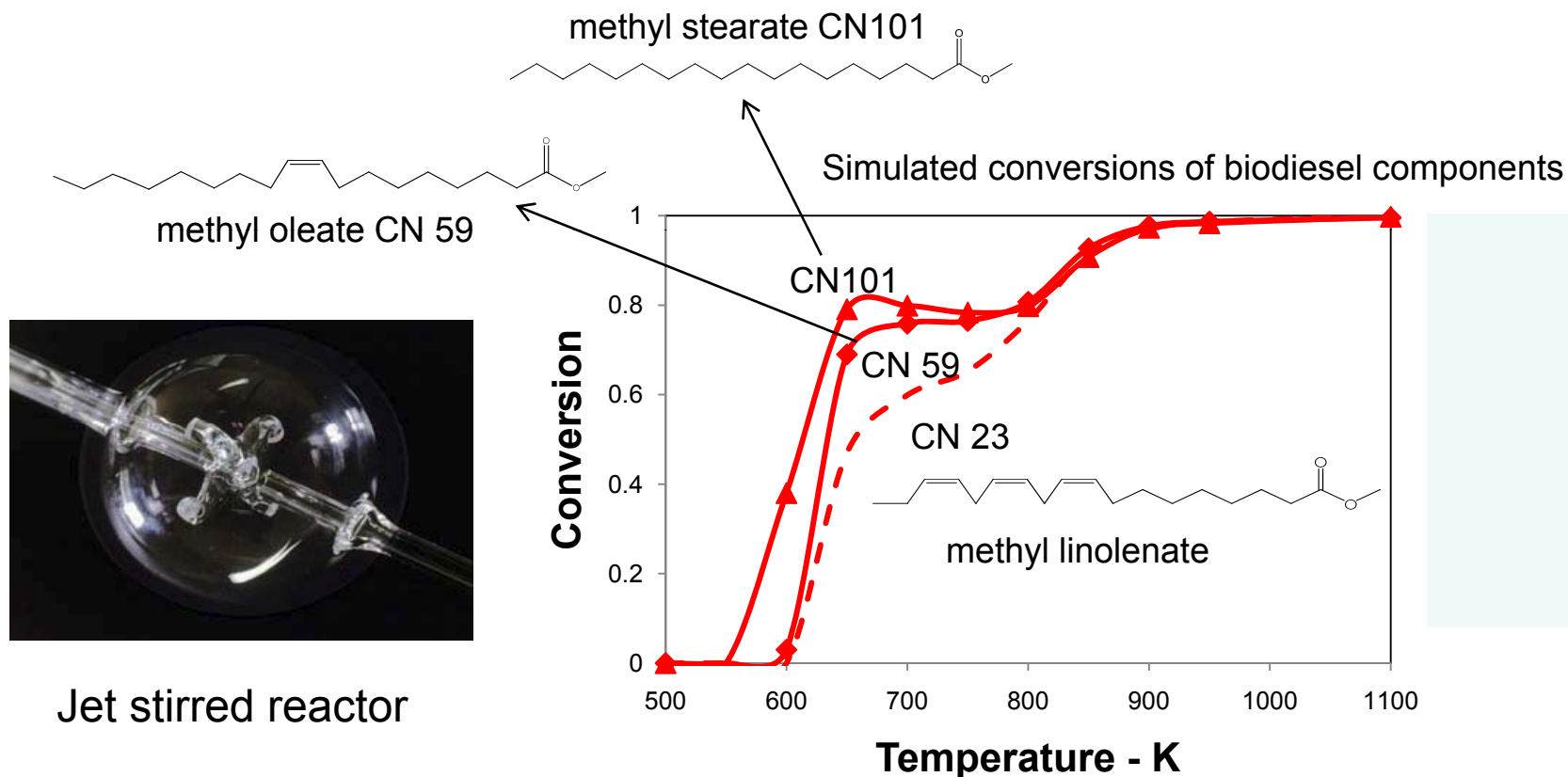


# Biodiesel components ignite in order of number of double bonds



# Increased number of double bonds reduces low T reactivity of individual components in stirred reactor at diesel conditions

Diesel engine conditions of high pressure and fuel-rich mixtures:  
50 bar,  $\Phi=2$  (Fuel: 200 ppm, residence time = 0.05 s)



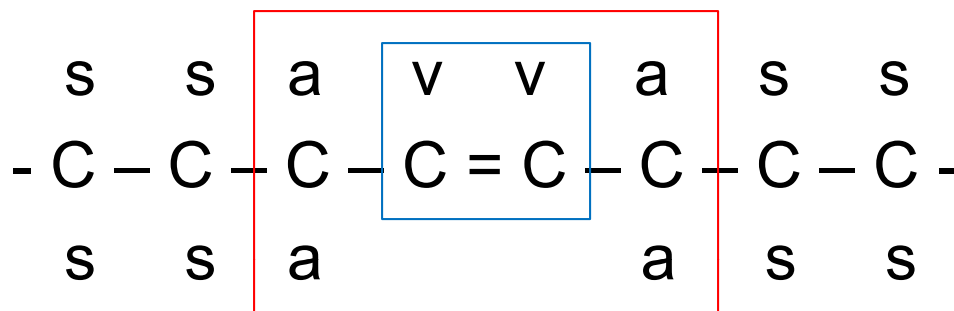
Jet stirred reactor

Derived cetane numbers from Knothe (2010)



# C = C double bonds reduce low T reactivity

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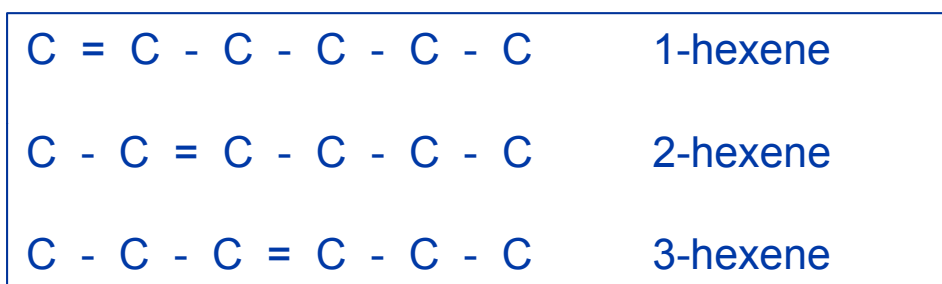


- Inserting one C=C double bonds changes the reactivity of 4 carbons atoms in the C chain
- Allylic C – H bond sites are weaker than most others
- Therefore they are preferentially abstracted by radicals
- O<sub>2</sub> is also very weakly bound at allylic sites and falls off rapidly, inhibiting low T reactivity





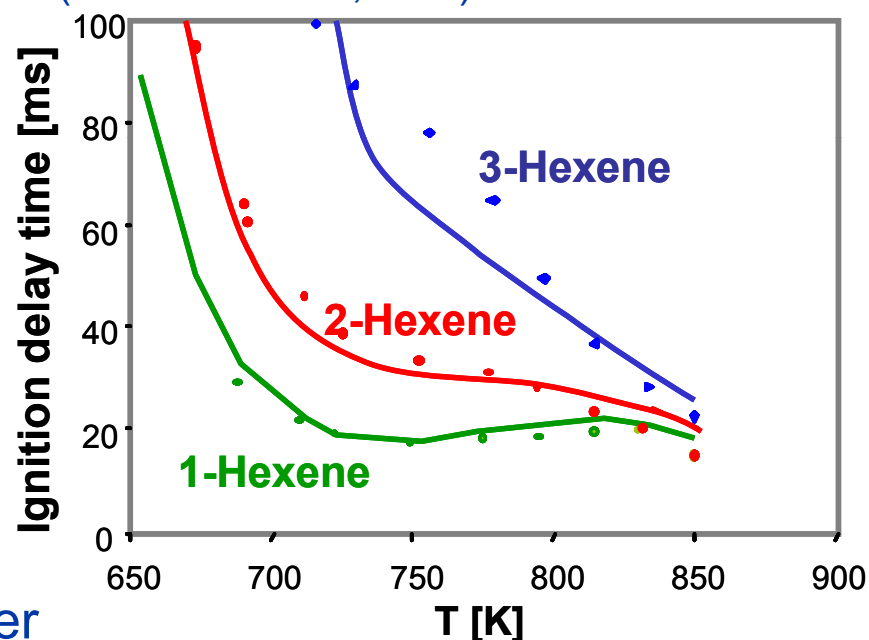
# We have seen the same effect in hydrocarbon fuels: hexenes



RO2 isomerization initiates low temperature reactivity

Moving the double bond towards the center of the molecule “blocks” more RO2 kinetics

Ignition delay times in a rapid compression machine of hexene isomers (0.86-1.09 MPa,  $\Phi=1$ ):



Experimental data: Vanhove et al. PCI2005  
Simulations: Mehl, Vanhove, Pitz, Ranzi Combustion and Flame 2008



# Plant and animal fat oils have different fatty acid profiles that affect reactivity in a diesel engine

	Sunflower	Safflower	Linseed	Jatropha	Cottonseed	Corn	Olive	beef tallow	Palm	Peanut	Soy	rapeseed
palmitate	7	7	7	4	23	10	13	28	46	11	8	4
stearate	5	2	1	8	3	4	4	21	4	8	4	1
oleate	19	13	19	49	20	38	72	47	40	49	25	60
linoleate	68	78	19	38	53	48	10	3	10	32	55	21
linolenate	1	0	54	1	1	0	1	1	0	0	8	14
CN	49	50	39	58	51	49	55	58	62	54	47	54

With models for all 5 major components, we can now model all these types of biodiesel:

- Not a surrogate model, but a real biodiesel (B100) model !



# Use Diesel PRF as a scale to compare reactivity of biodiesel compounds

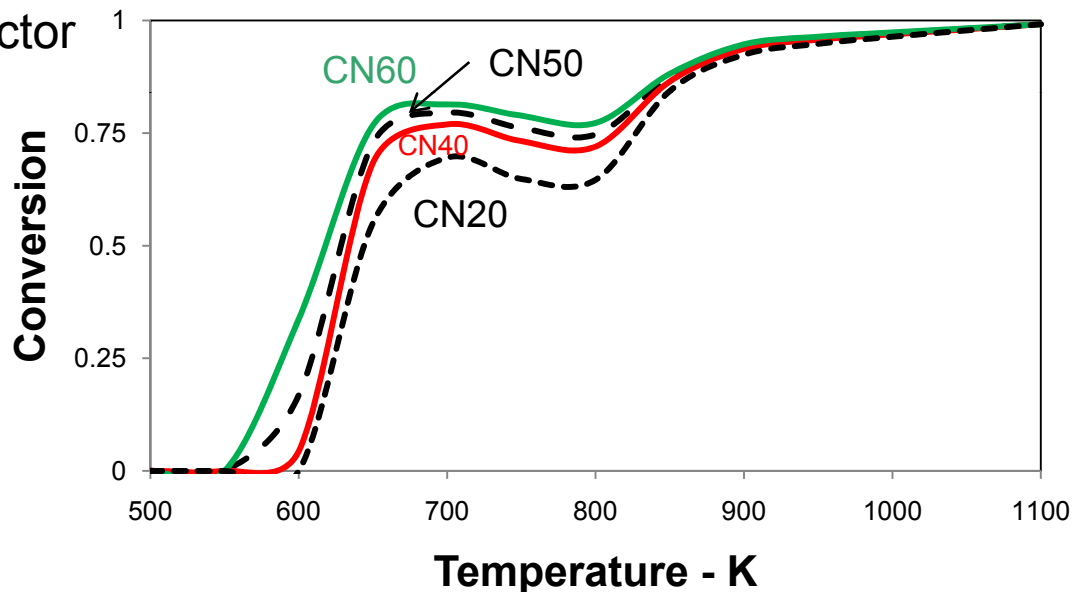


Jet stirred reactor

## Simulated Diesel PRF scale in a PSR

(n-hexadecane and 2,2,4,4,6,8,8-heptamethylnonane)

50 bar  
 $\Phi=2$   
fuel: 200 ppm  
 $\tau=0.05s$

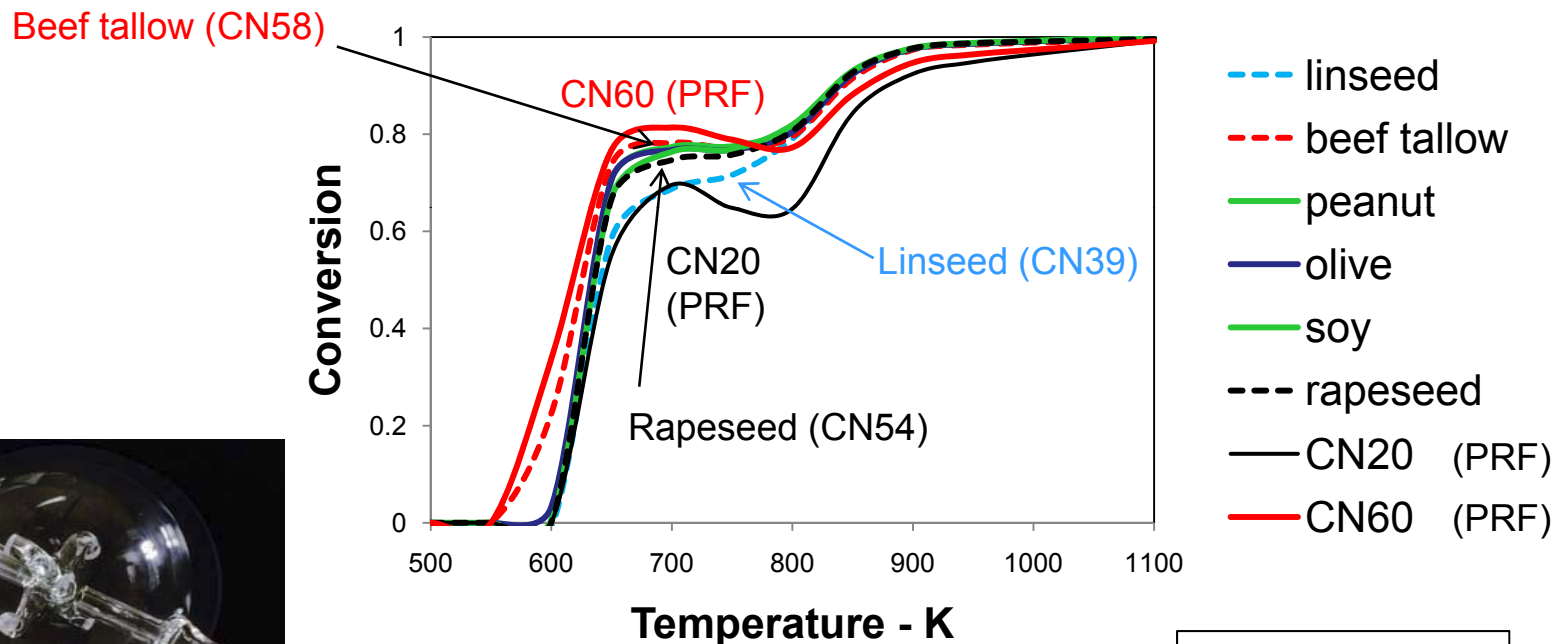


As CN increases, reaction in PSR starts at lower temperatures and has a greater extent of low T combustion



# Diesel PRF scale allows assessment of the reactivity of biodiesel from different sources

Simulated reactivity profiles for biodiesel fuels



Jet stirred reactor

50 bar  
 $\Phi=2$   
fuel: 200 ppm  
 $\tau=0.05s$



# Observations on reactivity of biodiesel fuels from different oils

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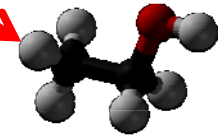
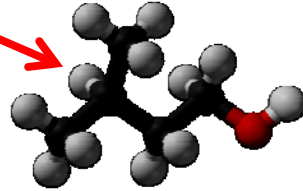
- Methyl ester fuels from different plant and animal fats and oils have different reactivity
- Detailed composition of these biodiesel fuels determine their reactivity
- Biggest factor for reactivity variability of biodiesel, large methyl ester fuels is the number of C=C double bonds
- We can model kinetics of most of these biodiesel fuels using the new biodiesel kinetic mechanism
- The mechanisms still need refinements and testing, and careful laboratory experiments would be very valuable



# What & Why Isopentanol ?

## A Next Generation BioFuel:

- Isopentanol (3-Methyl-1-Butanol or 3 Methylbutane-1-ol) is one of biomass derived alcoholic fuel, like Ethanol

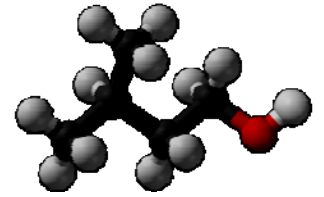


- The challenge of **JBEI**: To convert all monomer sugars (hexoses and pentoses) released from depolymerization of lignocellulosic biomass into transportation fuels and other chemicals. And the **initial targets of JBEI** is ethanol, butanol, isopentanol, hexadecane, and geranyl decanoate ester.
- Higher alcohols such as isopentanol has **higher energy density** and **lower hygroscopicity** compared to ethanol.
- Volatility is **moderate** like gasoline, “Not” too high

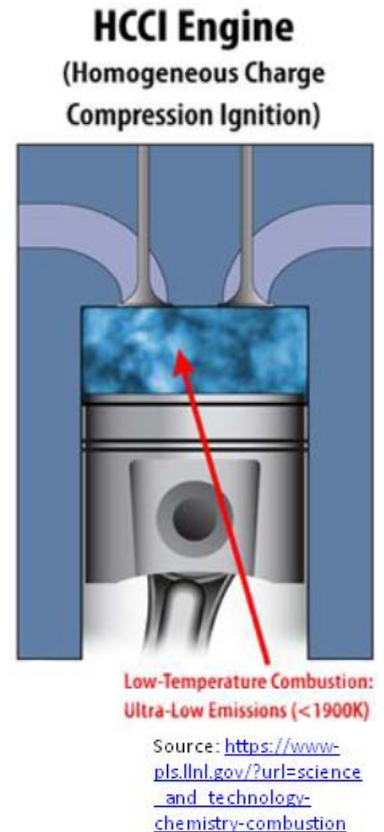
Lawrence Livermore National Laboratory



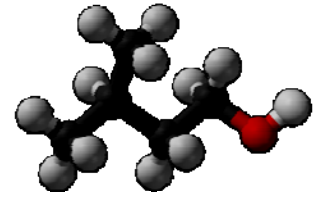
# Approach



- **Development of Isopentanol reaction mechanism**
- **Single-zone Simulations → Validation**
- **Study of the kinetics involved in the auto-ignition process**
- **Simulate an HCCI Engine Combustion**
- **Compare with representative experimental results**

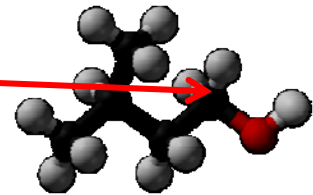


# Development of Reaction Mechanism



## High temperature chemistry:

- Unimolecular decomposition and H atom abstraction from fuel by activated radicals mainly occur
- Alcohols have weak C-H bonds at  $\alpha$  site

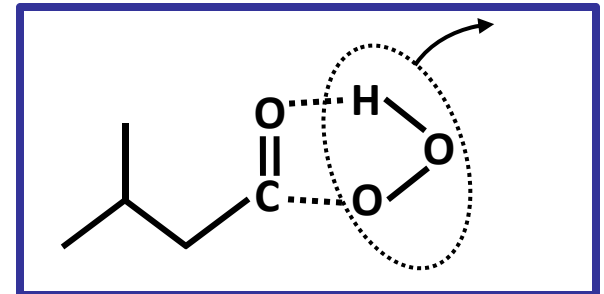


## Low temperature chemistry:

- Based on low temp. chemistry of isooctane because isooctane has some similar structures to isopentanol
- ➔ Results showed “Too Short Ignition Delay & Too Strong NTC”

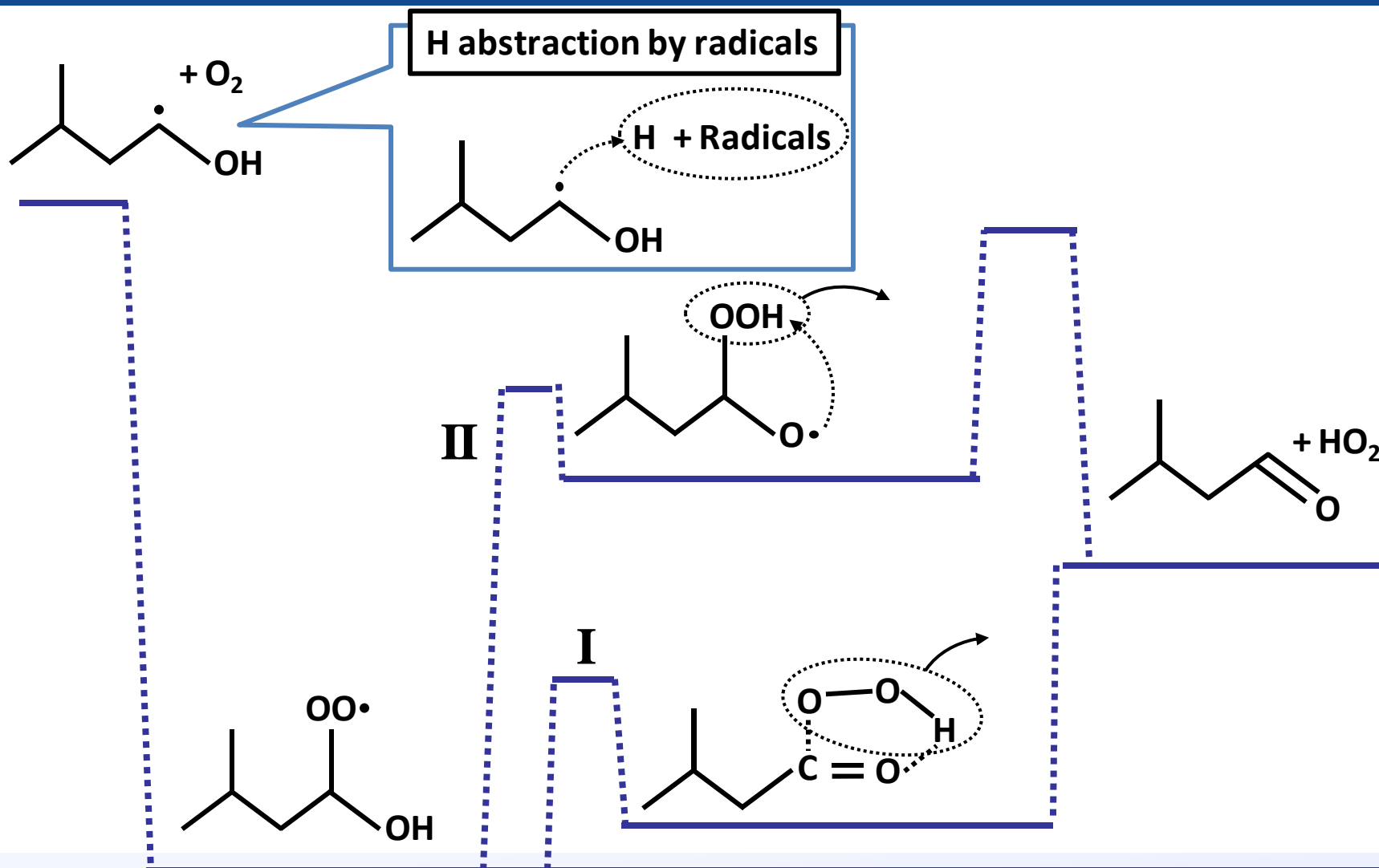
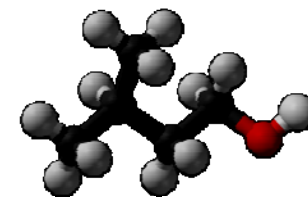
## **Concerted elimination of $HO_2$ :**

- Concerted elimination forming aldehyde and  $HO_2$  from  $RO_2$  is so fast that low temperature reactions would be slowed down

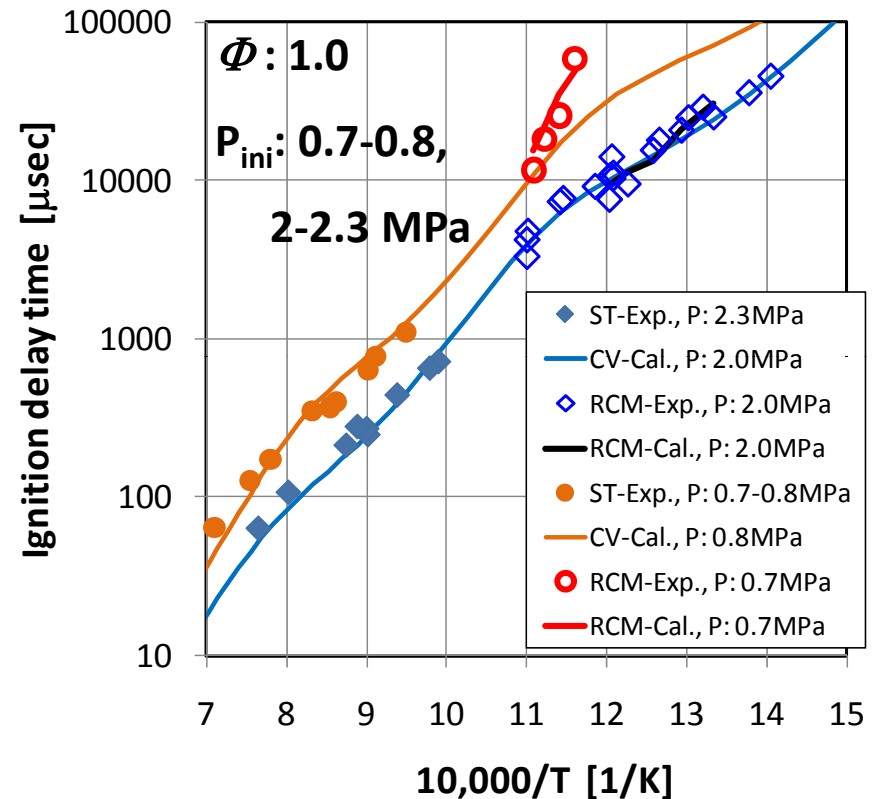
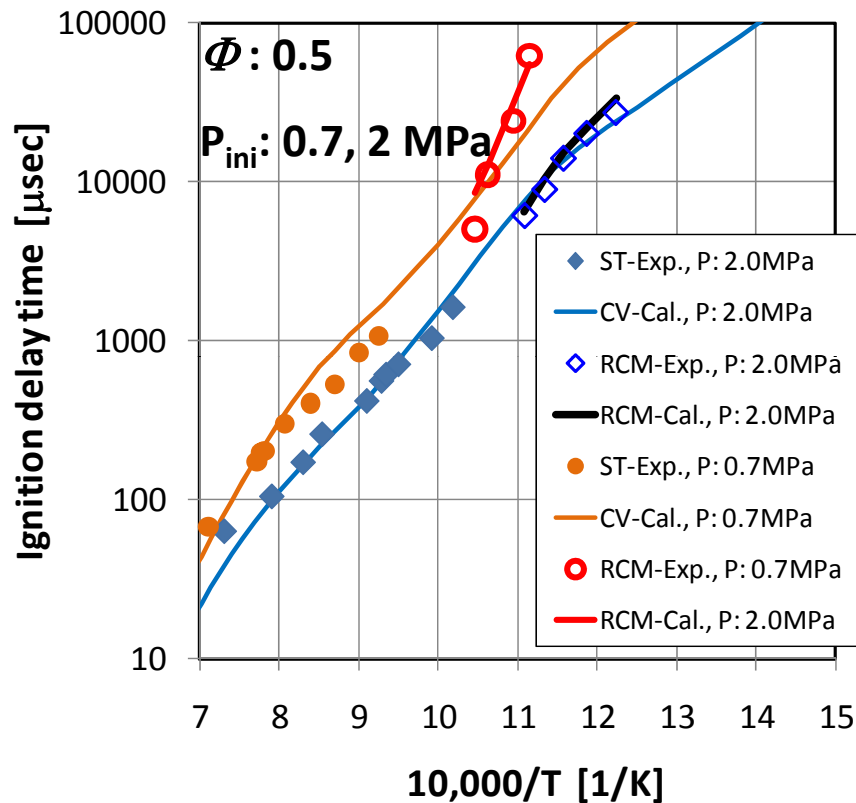
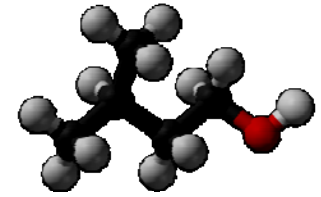




# Schematic Energy Diagram for the Concerted Elimination of HO<sub>2</sub>



# Validations of Reaction Mechanism



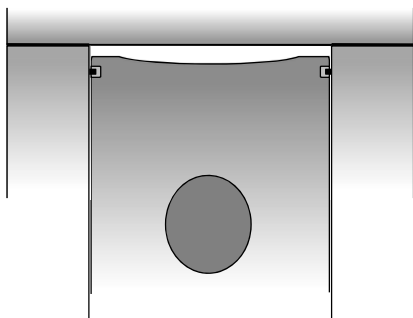
- Isopentanol model developed in this study can reproduce the experimental data which were acquired under various  $\Phi$ , T, and P conditions with a shock tube and an RCM

**Shock tube experiments:** Kenji Yasunaga, Fiona Gillespie, and Henry Curran (NUI Galway - Ireland)  
**Rapid compression machine (RCM) experiments:** Bryan Weber, Yu Zhang and Chih-Jen Sung (UConn.)

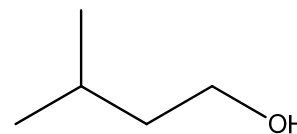


# Developed chemical kinetic model for new biofuel iso-pentanol and compared it to experiments in Sandia HCCI engine

HCCI engine experiments:  
Yang and Dec, Sandia, SAE 2010



Iso-pentanol mechanism



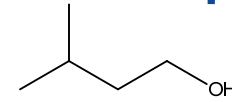
New generation biofuel proposed by  
DOE Joint BioEnergy Institute (JBEI)

Reaction rate rules on successful iso-  
octane because it has some similar  
structures

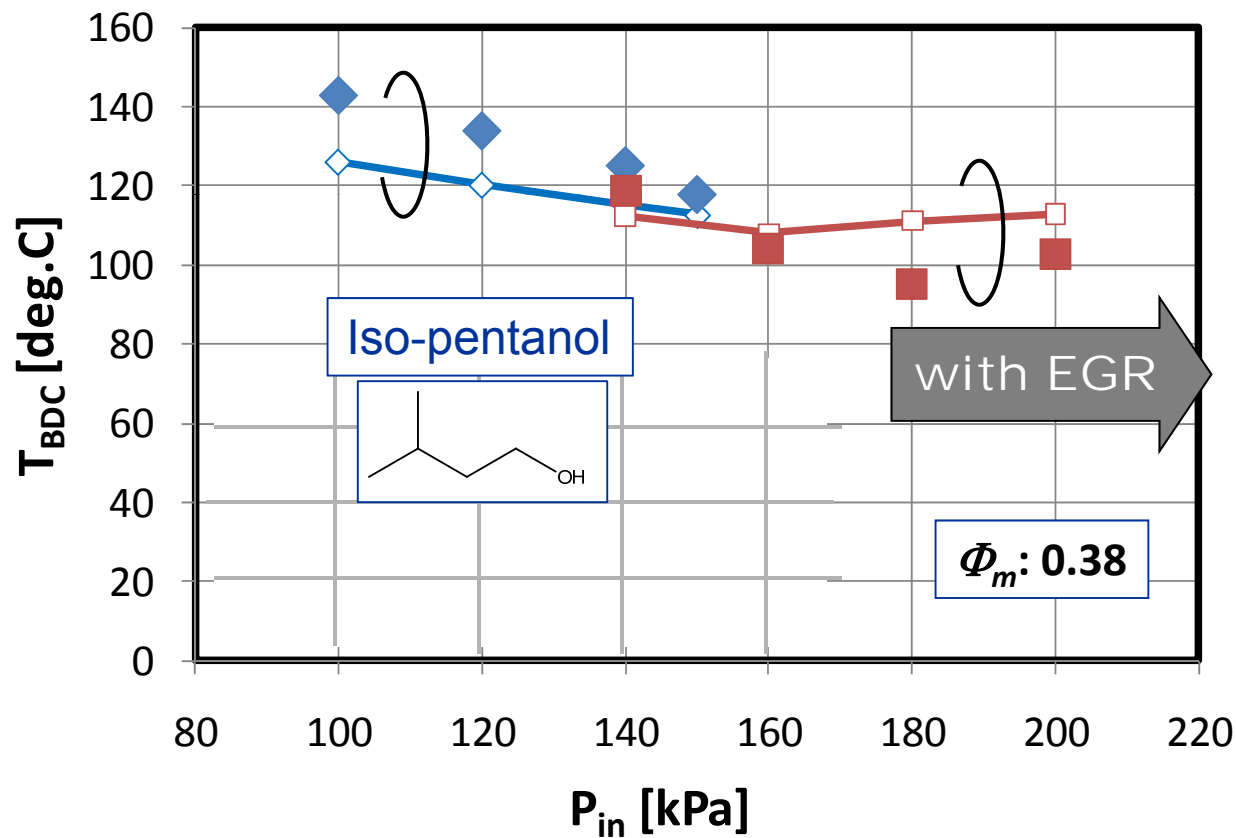
Model development and application:  
LLNL visiting scientist  
Dr. Taku Tsujimura  
National Institute of Advanced  
Industrial Science and Technology, Japan



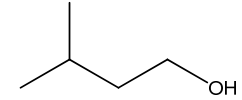
# Iso-pentanol model predicts correct combustion phasing as load is increased in Sandia HCCI engine



Experiments and Calculations:  
Required  $T_{BDC}$  for constant combustion phasing

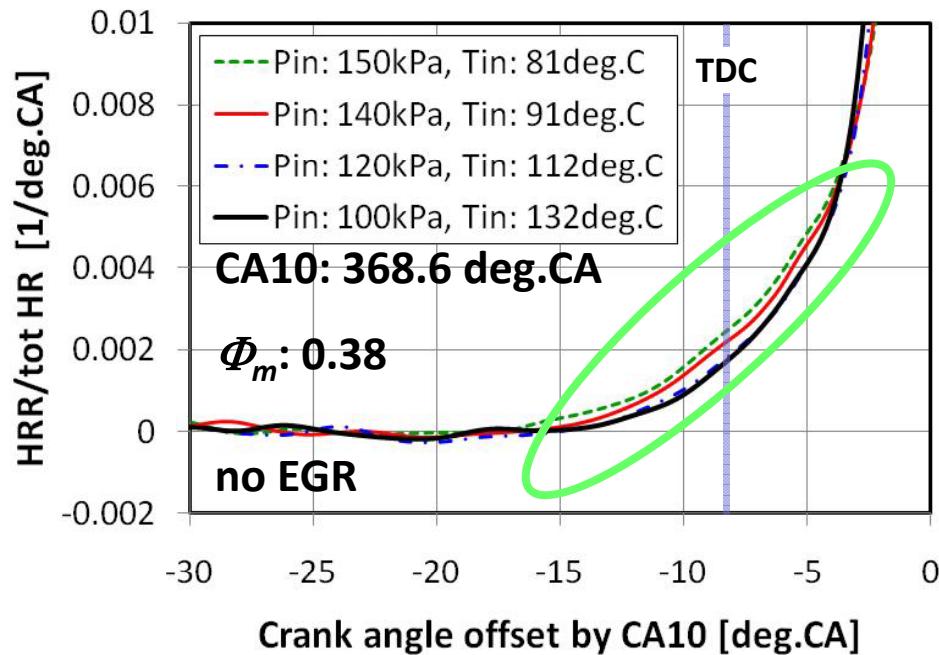


# Iso-pentanol model predicts intermediate heat release that allows high load operation for HCCI

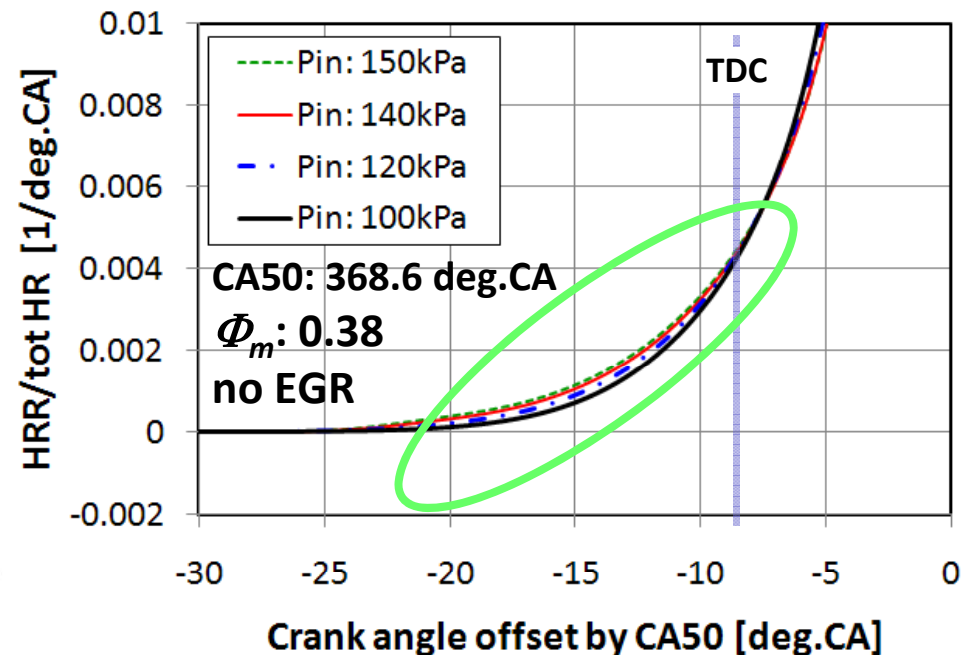


## Iso-pentanol

### Experiments



### Calculations



HCCI engine experiments:  
Yang and Dec, Sandia, SAE 2010



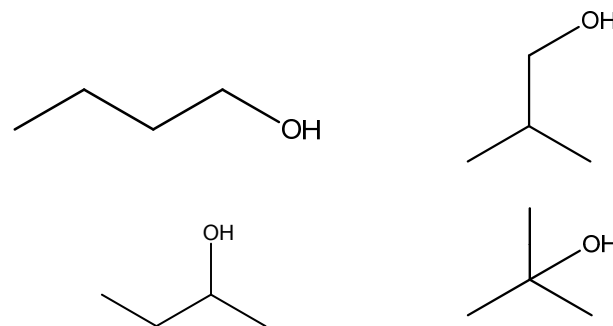
# Developed model for 4 isomers of butanol and compared model predictions to flame experiments at USC

Flame speed measurements:  
Egolfopoulos et al. USC



Twin premixed counterflow  
flames

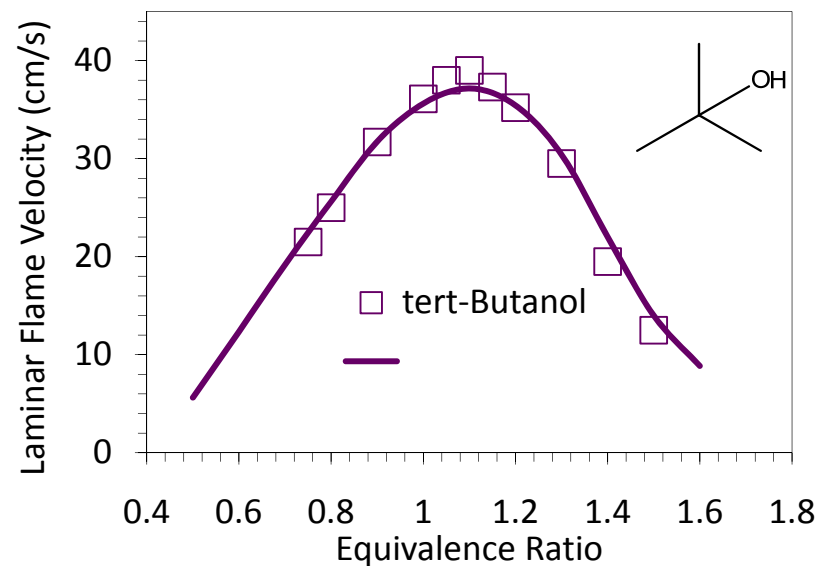
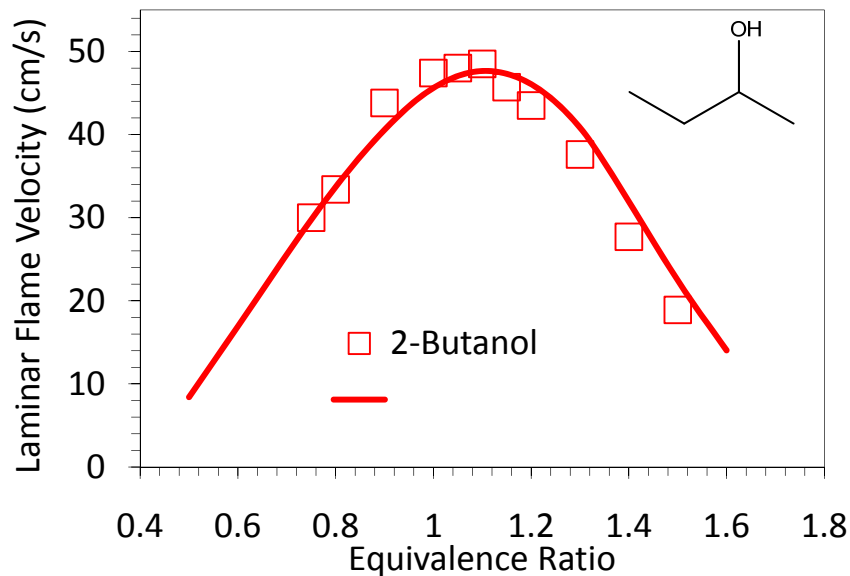
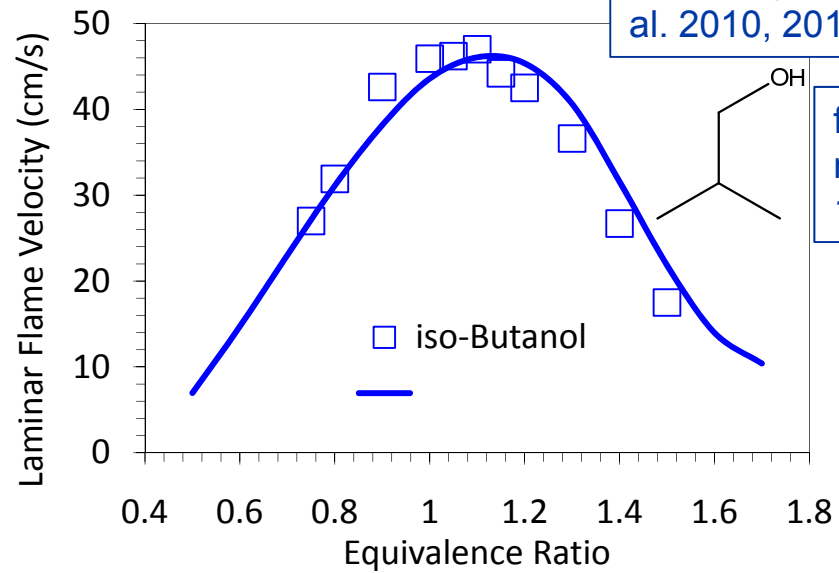
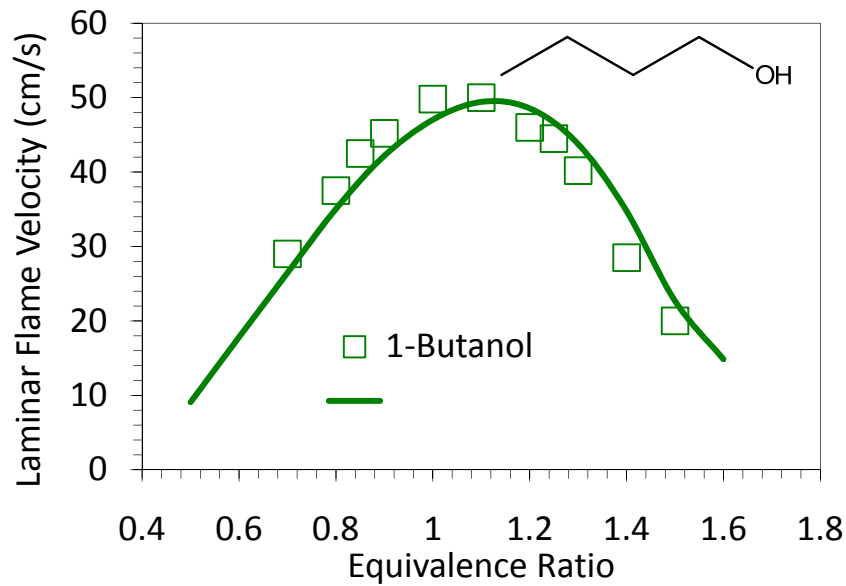
butanol mechanism: 4 isomers



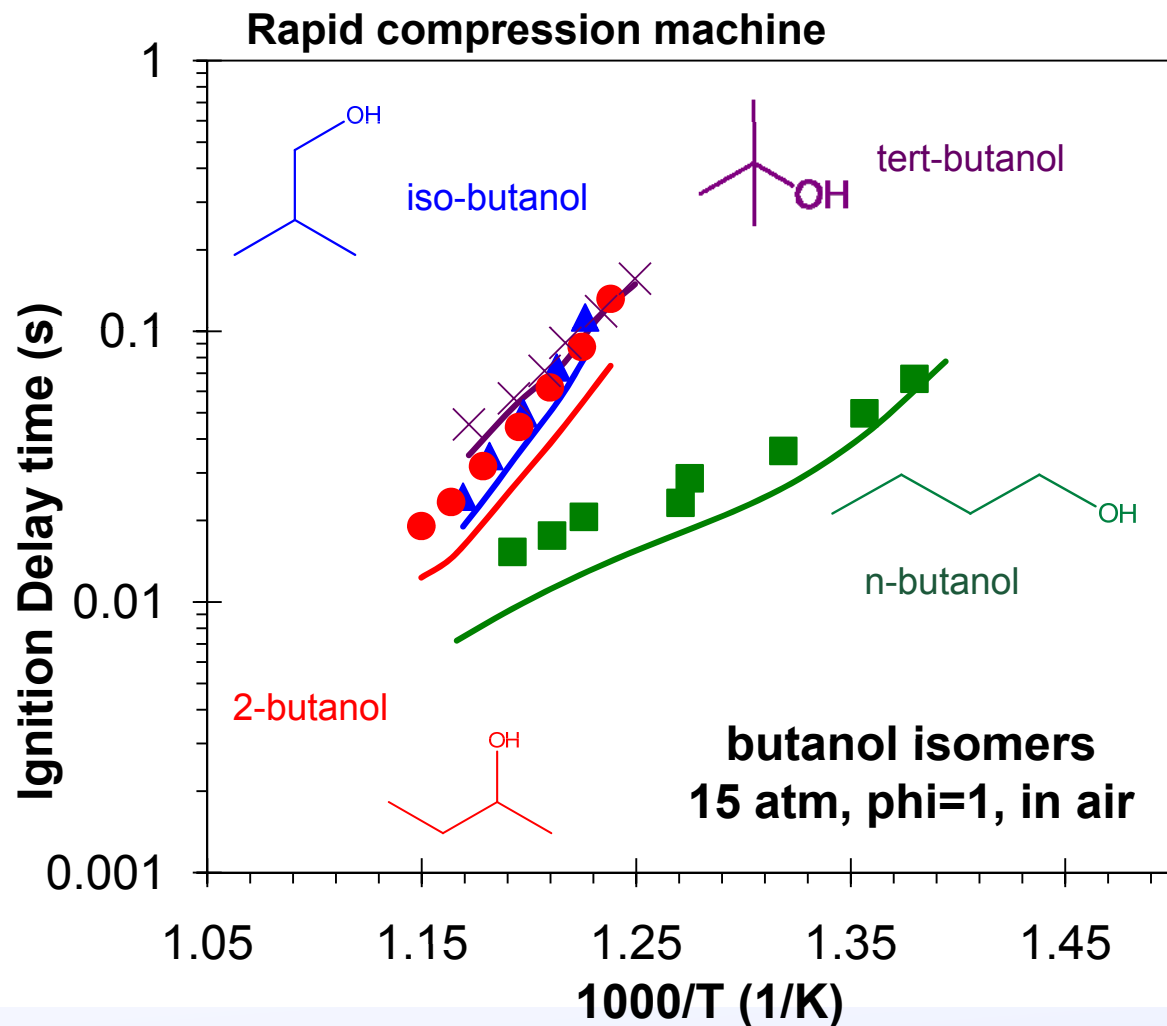
Iso-butanol is a  
new type of  
biofuel that can  
be made directly  
from cellulose  
using bacteria



# Butanol mechanism accurately simulates flame speeds important for predicting spark ignition engine combustion



# Butanol model well predicts ignition delay times at pressures and temperatures found in IC engines



Symbols:  
experimental data  
Sung et al.,  
AIAA paper, 2011

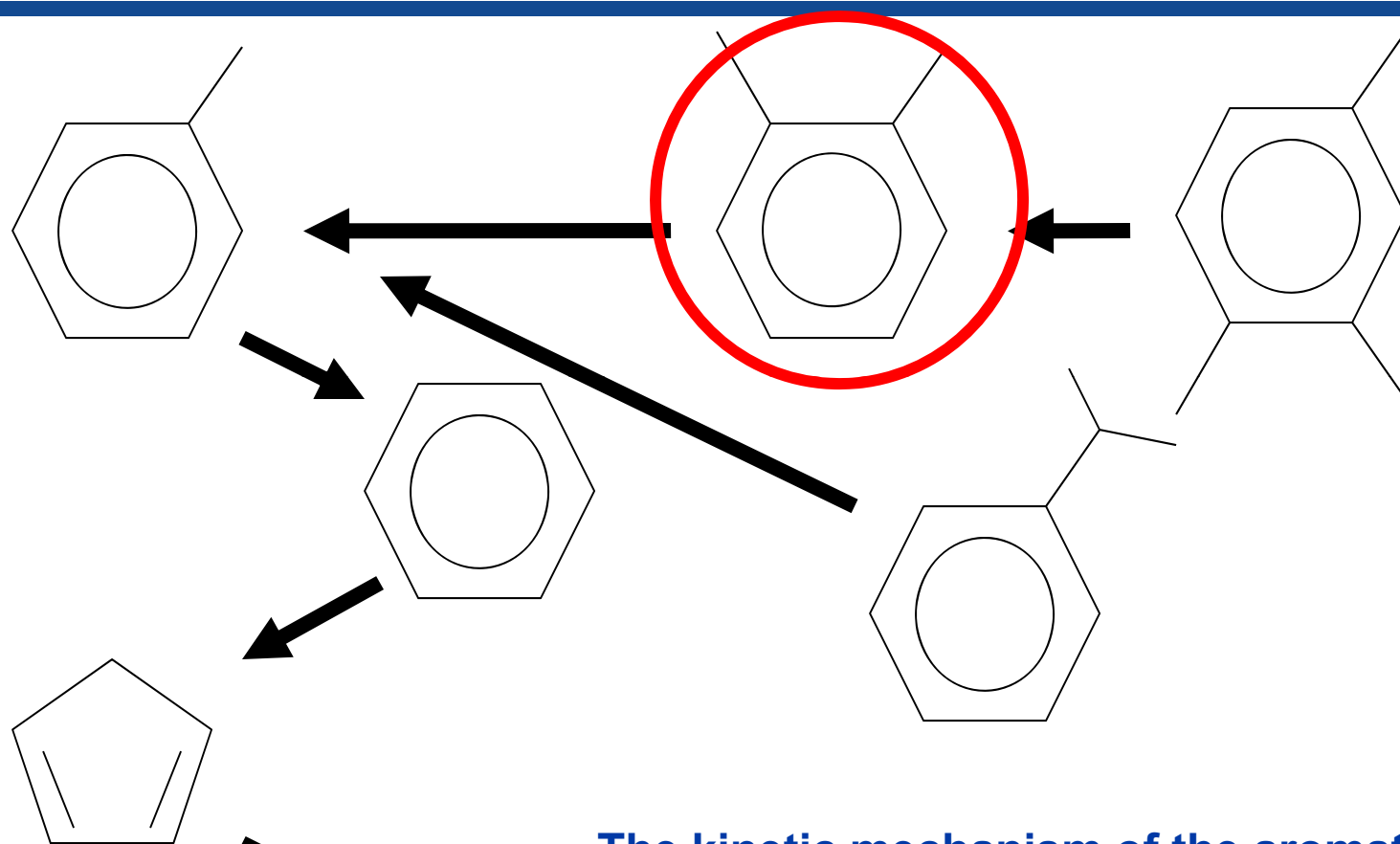


Rapid compression machine  
University of Connecticut





# Chemical kinetic mechanism for larger aromatics

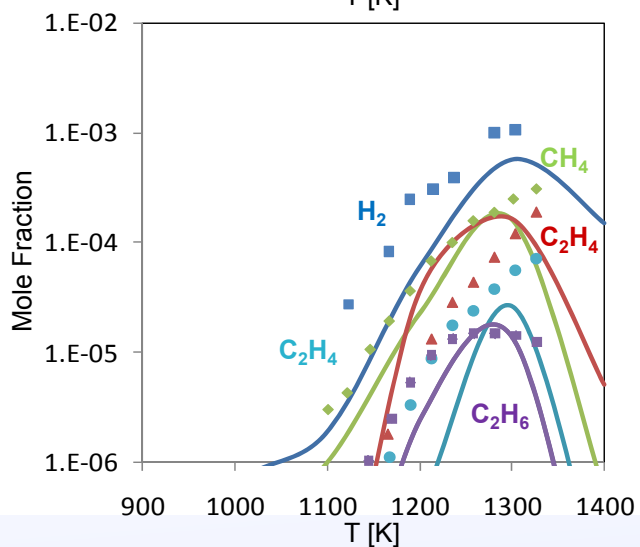
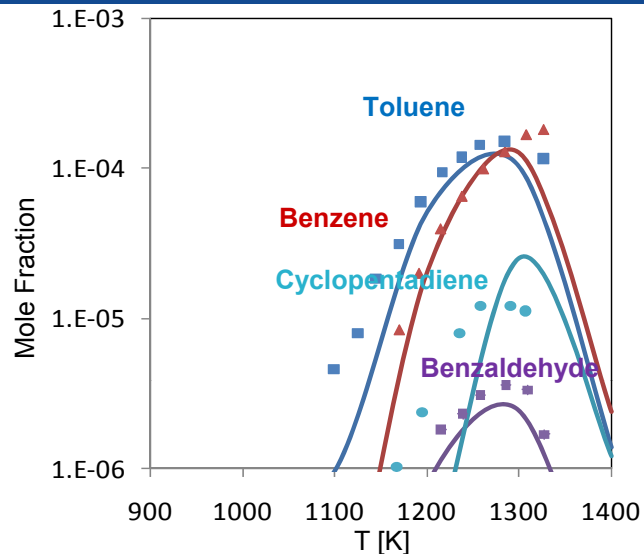
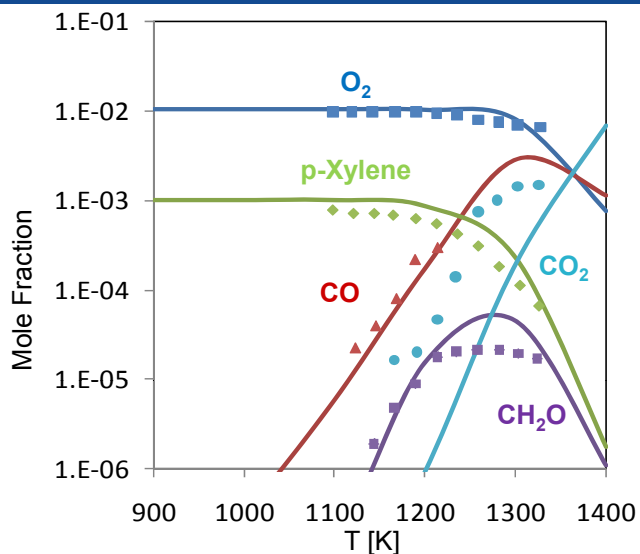
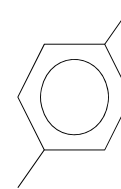


**The kinetic mechanism of the aromatics has an intrinsic hierarchical structure**

**A new module specific to C8 alkyl aromatics is now under development**



# p-Xylene mechanism well reproduces species profiles in jet stirred reactor



Jet stirred reactor

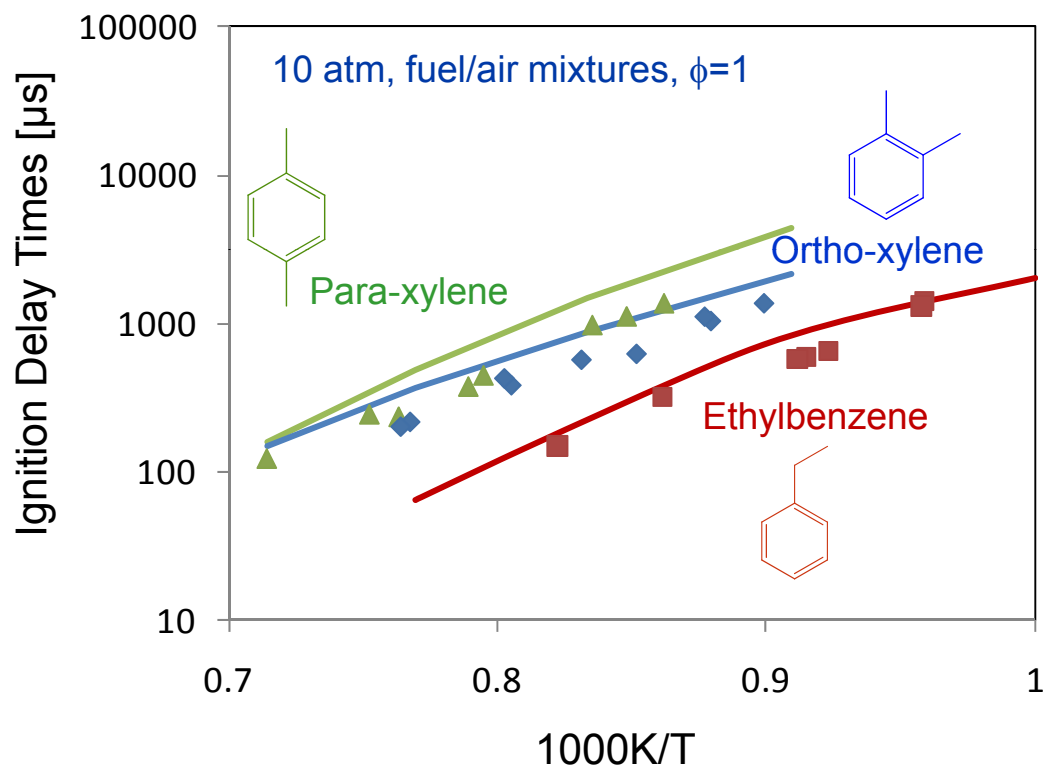
$P = 1 \text{ atm}, \Phi = 1, \tau = 0.1 \text{ s}$

Experiments: Gail and Dagaut  
Combustion and Flame 2005



# Ortho-, para- and ethyl-benzene models compare well to ignition delay times measured at pressure and temperatures relevant to engines

Ignition delay times in a shock tube for aromatics



Shock tube experimental data:  
Shen and Oehlschlaeger,  
Combustion and Flame 2009



# Mechanisms are available on LLNL website and by email

[http://www-pls.llnl.gov/?url=science\\_and\\_technology-chemistry-combustion](http://www-pls.llnl.gov/?url=science_and_technology-chemistry-combustion)

Ethanol

Dimethyl Ether

CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, C<sub>3</sub>H<sub>8</sub>,  
and nC<sub>4</sub>H<sub>10</sub>

CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, C<sub>3</sub>H<sub>6</sub>,  
C<sub>3</sub>H<sub>8</sub>, and NO<sub>x</sub>

C<sub>8</sub>-C<sub>16</sub> n-Alkanes

Cyclohexane

Methylcyclohexane

Methyl Butanoate and  
Methyl Formate

Methyl Decanoate

Methyl Decanoates

Biodiesel Surrogates

Dimethyl Carbonate

Heptane, Detailed  
Mechanism

Heptane, Reduced  
Mechanism

iso-Octane

Primary Reference Fuels:  
iso-Octane / n-Heptane  
Mixtures

2,2,4,4,6,8,8-  
Heptamethylnonane

Organophosphorus  
Compounds under  
Incineration Conditions

Organophosphorus  
Compounds in Propane  
Flames

Organophosphorus

## Combustion Chemistry

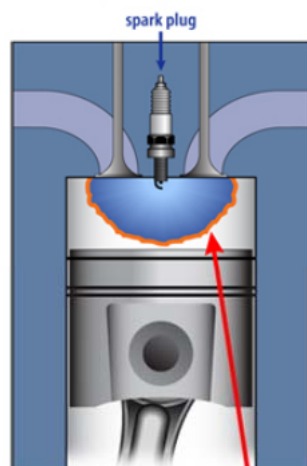
### [Go Directly to Mechanisms...](#)

The central feature of the Combustion Chemistry project at LLNL is our development, validation, and application of detailed chemical kinetic reaction mechanisms for the combustion of hydrocarbon and other types of chemical fuels. For the past 30 years, our group has built hydrocarbon mechanisms from hydrogen and methane through much larger fuels including heptanes and octanes. Other classes of fuels for which models have been developed include flame suppressants such as halons, organophosphates, and air pollutants such as soot and oxides of nitrogen and sulfur.

Reaction mechanisms have been tested and validated extensively through comparisons between computed results and measured data from laboratory experiments (e.g., shock tubes, laminar flames, rapid compression machines, flow reactors, stirred reactors) and from practical systems (e.g., diesel engines, spark-ignition engines, homogeneous charge, compression ignition (HCCI) engines). We have used these kinetic models to examine a wide range of combustion systems.

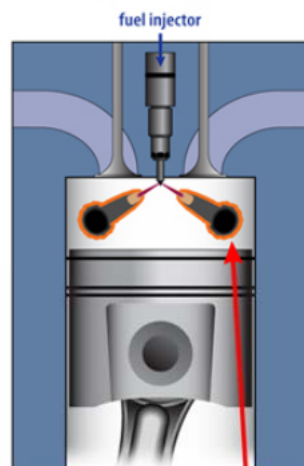
Biodiesel Surrogates

**Gasoline Engine**  
(Spark Ignition)



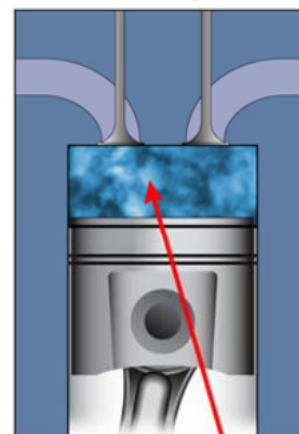
Hot-Flame Region:  
NO<sub>x</sub>

**Diesel Engine**  
(Compression Ignition)



Hot-Flame Region:  
NO<sub>x</sub> & Soot

**HCCI Engine**  
(Homogeneous Charge  
Compression Ignition)



Low-Temperature Combustion:  
Ultra-Low Emissions (<1900K)



# Summary

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- Reaction classes and reaction rate rules greatly simplify the task of developing chemical kinetic models and assigning rate constants
- Continually updating reaction rate rules and adding new rules for new moieties such as those from new biofuels
- Made a lot of progress in chemical kinetic modeling new classes of compounds like esters and alcohols and difficult compounds to model like aromatics



# Acknowledgements

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- Fokion Egolfopoulos, butanol
- Jackie Sung, iso-pentanol
- John Dec and Yi Yang, iso-pentanol



# Acknowledge support from:

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- DOE Office of Vehicle Technologies
  - Gurpreet Singh
  - Kevin Stork
- DOE Office of Basic Energy Sciences
  - Wade Sisk
- DOD Office of Naval Research

